

BIOLOGICAL PHOSPHORUS REMOVAL PLUS CHEMICAL POLISHING FOR LOW LEVEL COMPLIANCE

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Lake Michigan District Regional Operators Meeting

May 21, 2015



Presentation Outline

- Background
 - BPR + Coagulants
- Janesville Pilot Studies
- BPR + Supplemental Carbon
- Take-away points

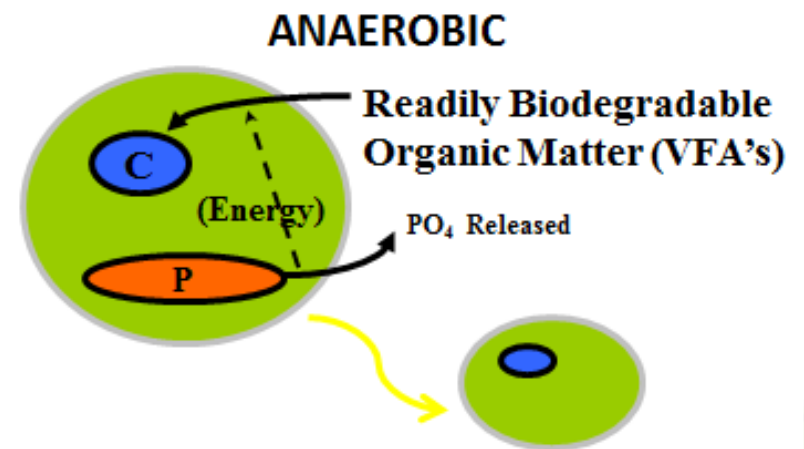
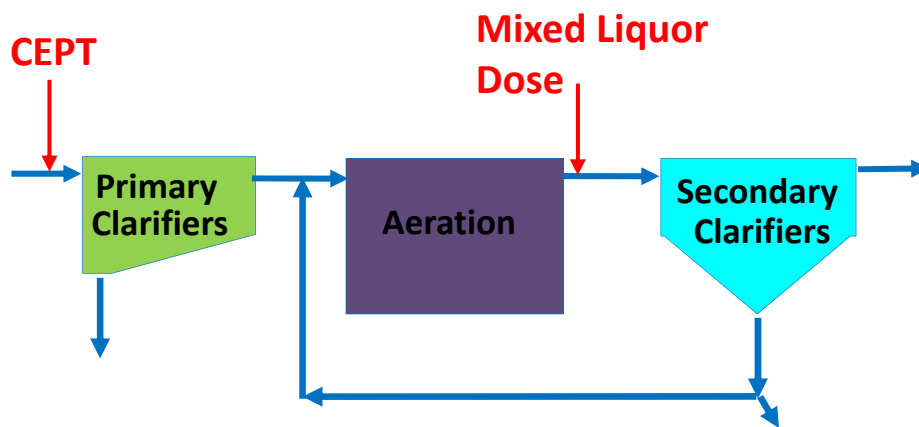


Background

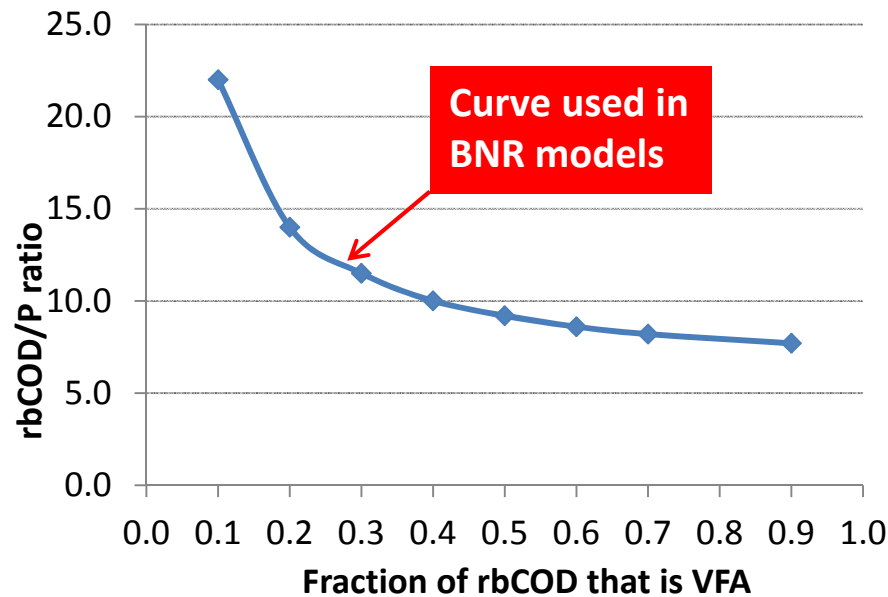
Background

➤ Focus of discussion:

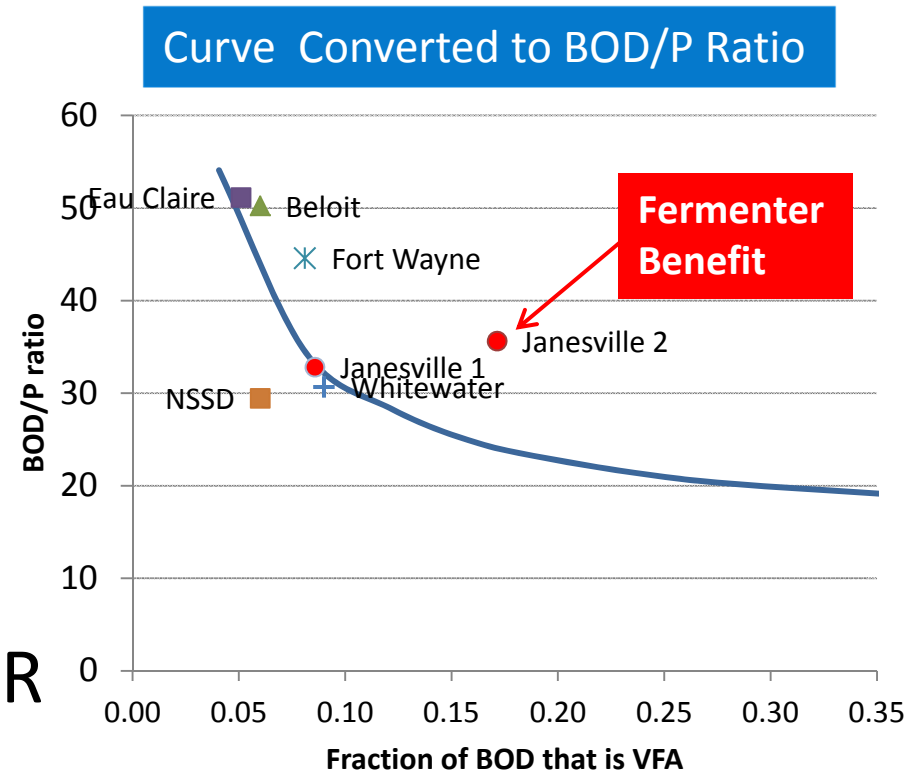
- BOD:P ratio
 - Importance to BPR
- Chemical dosing ratio
 - Interactions / interrelationships when chemicals are added to a BPR process



Background



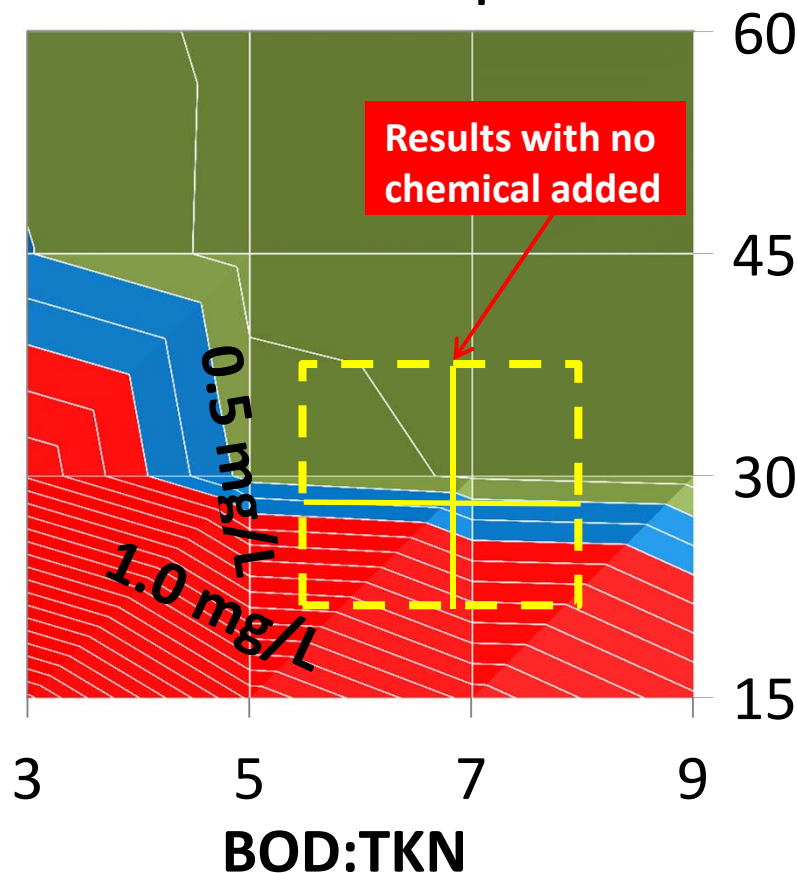
EBPR Curve (Barnard et al, WEFTEC 2005)



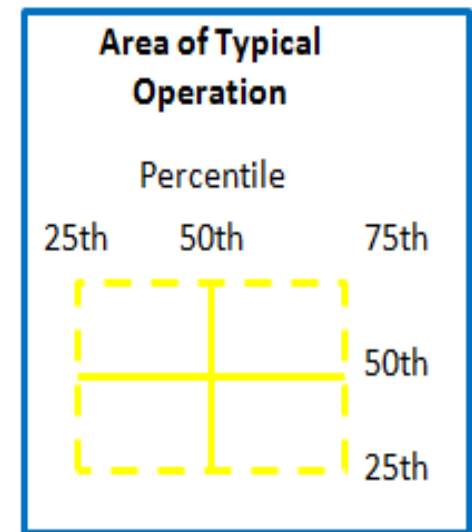
- BOD:P provides simple BPR performance gauge

Background

- Surface plot of BioWin modeling results provides “performance map”

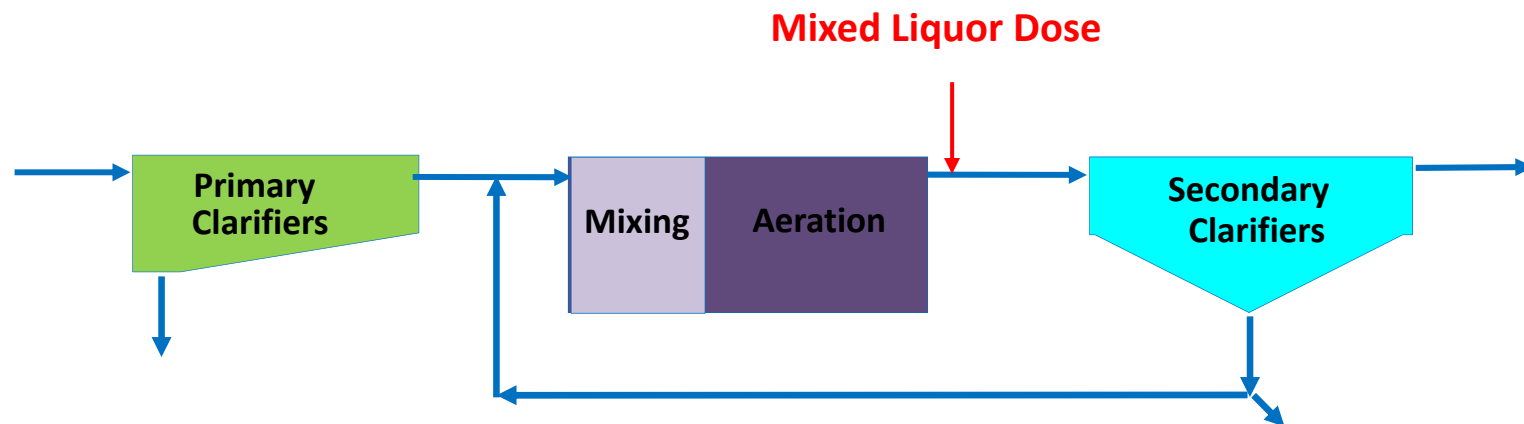


BioWin shows performance is highly dependent on BOD:P



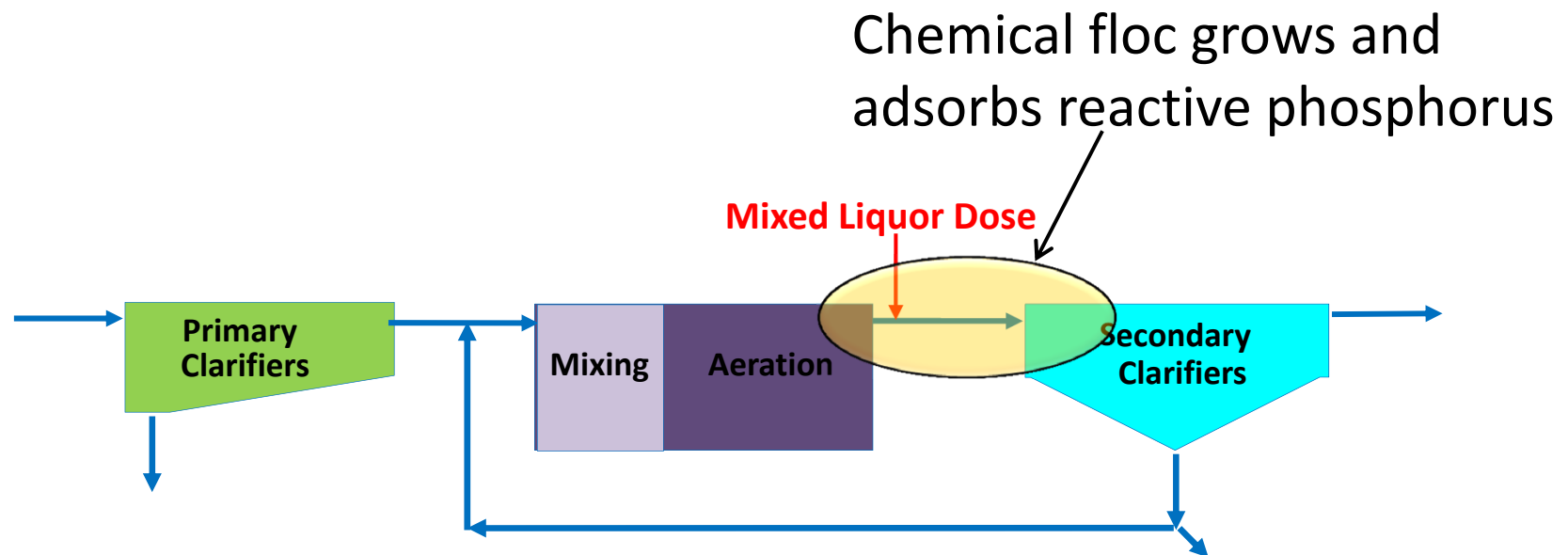
Background

- Chemical addition for polishing
 - BPR + chemical working together
 - How does this affect BOD:P ratio?
 - Focus on two areas of chemical interaction



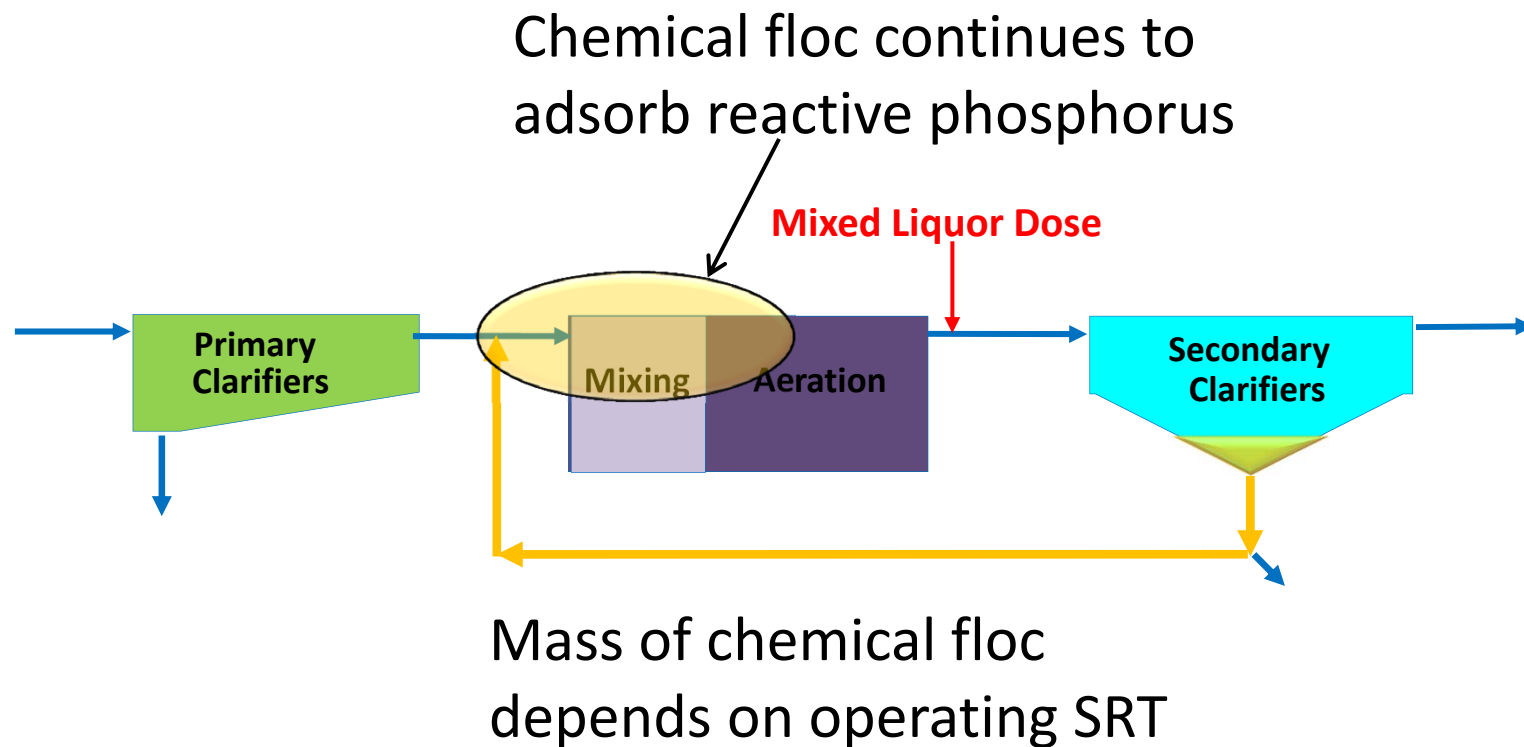
Background

➤ Dose point interaction



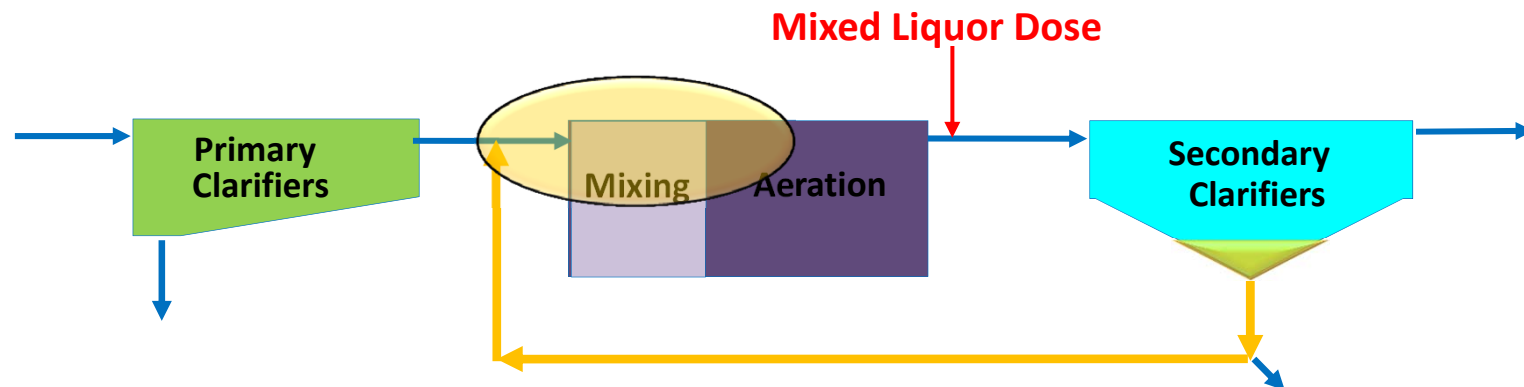
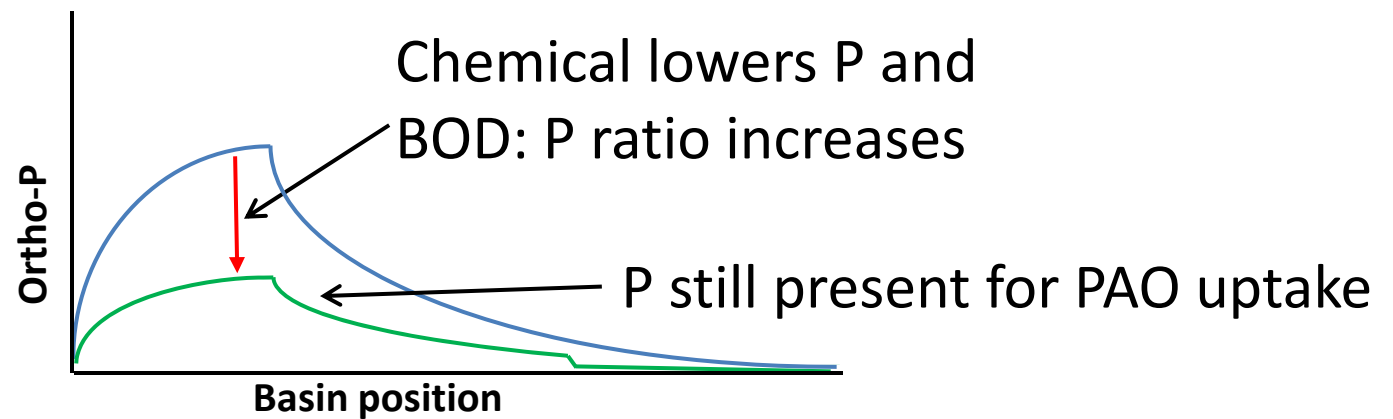
Background

➤ In-basin interaction



Background

➤ BPR interaction



PAOs continue to have an advantage – BPR stays healthy

Background

➤ Chemical addition for polishing

- Chemical interaction

Low level treatment
requires high dosing
ratios

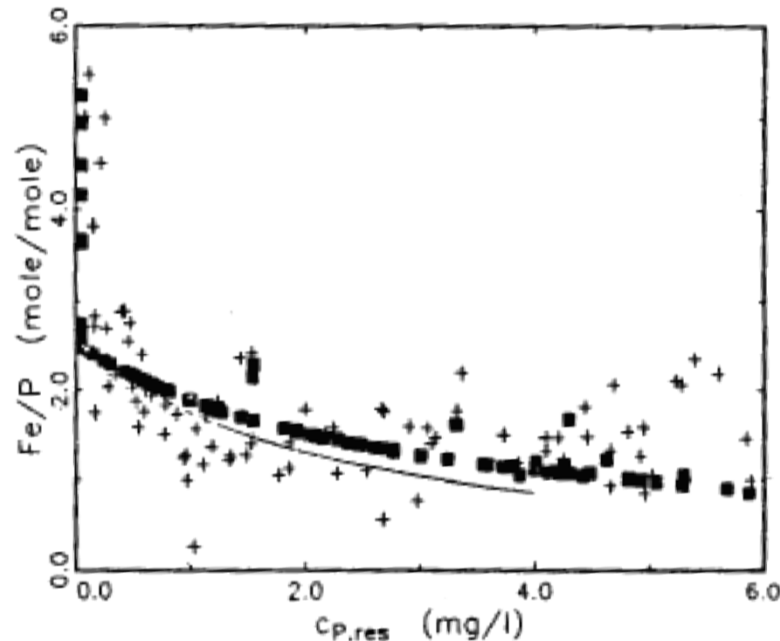
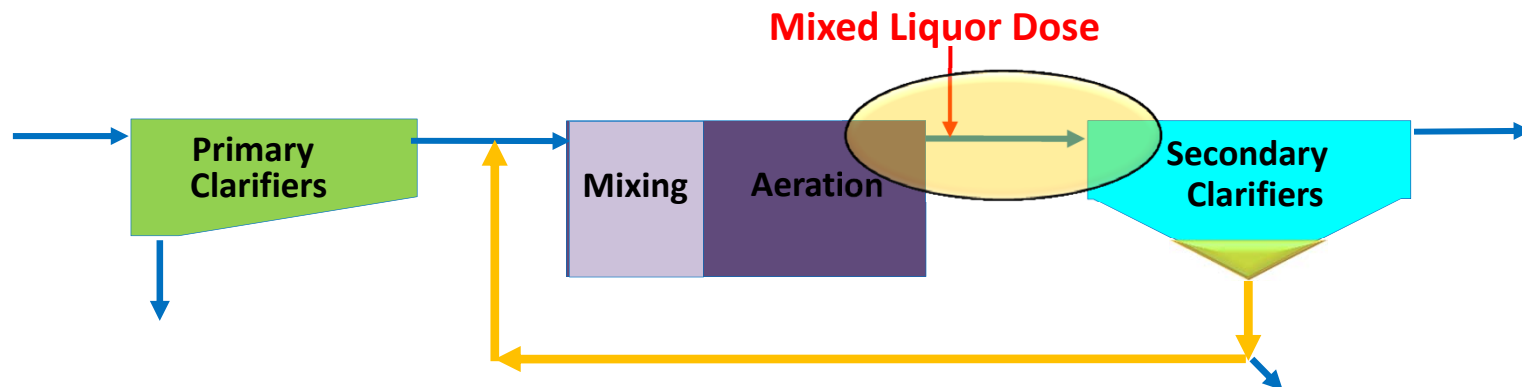
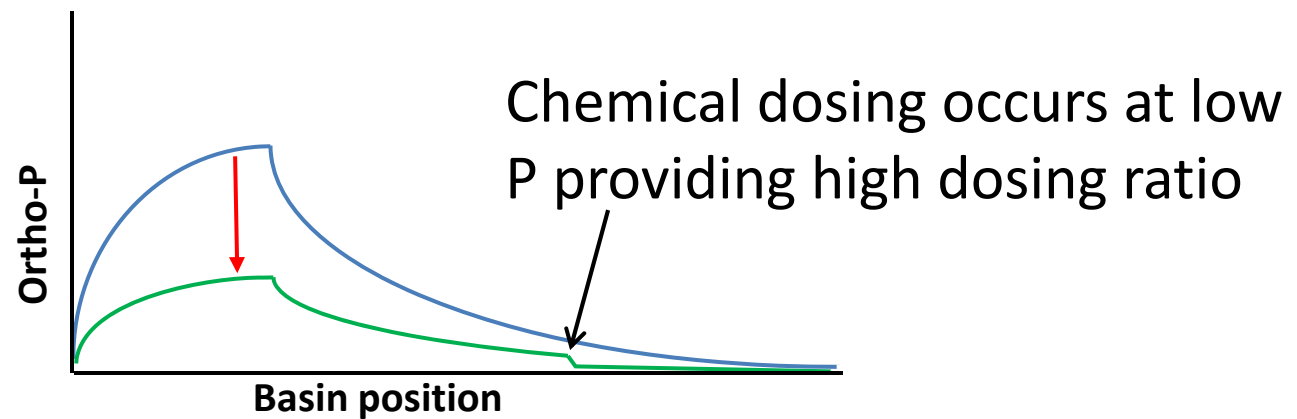


Fig. 6. Observed and calculated values of Fe/P ratios for pH=7.2
(+ observed, * calculated, solid and broken lines: estimation of r_1)

“Precipitation of Ferric Phosphate in Activated Sludge: A Chemical Model and Its Verification,” Luedicke et al, Water Science and Technology, Vol. 21, pp 325-337, 1989.

Background

➤ Chemical interaction

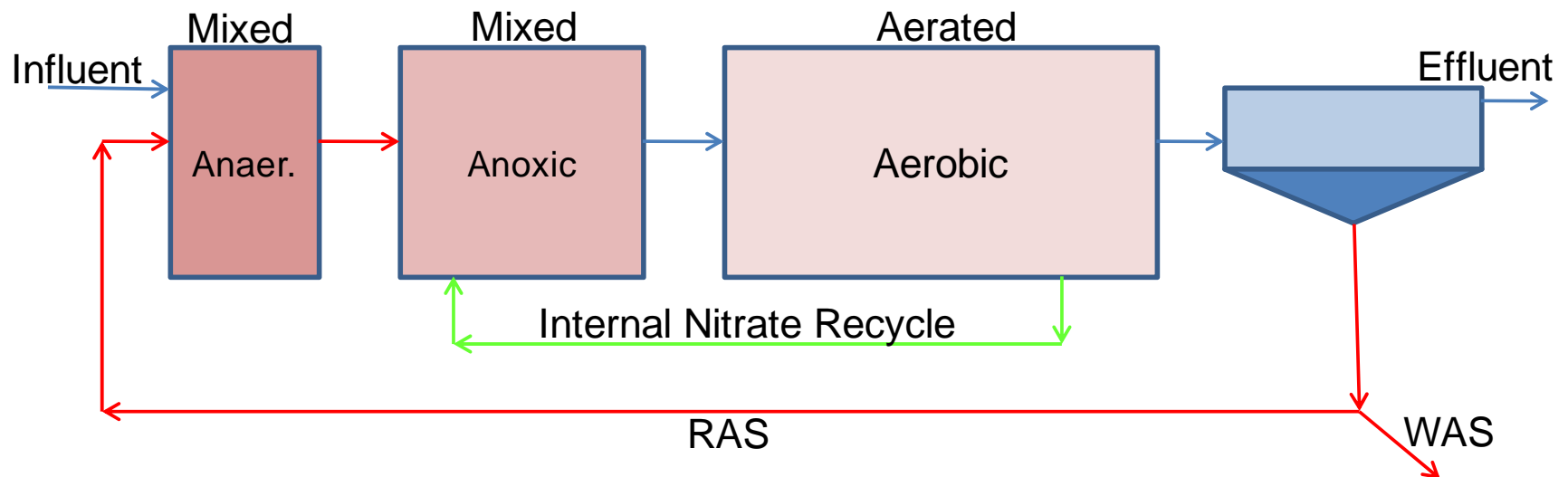


Chemical dose point provides best opportunity for low level treatment

Janesville Case Study

Janesville Background

- Current flow of 14 mgd
- A²O process configuration
- Effluent P goal between 0.3 mg/L and 0.5 mg/L



Janesville Background

- TMDL Implementation for Rock River
 - Janesville has new TMDL permit
 - Monthly mass allocations necessitate effluent P concentrations at or below 0.1 mg/L
 - Compliance schedule of 9 years



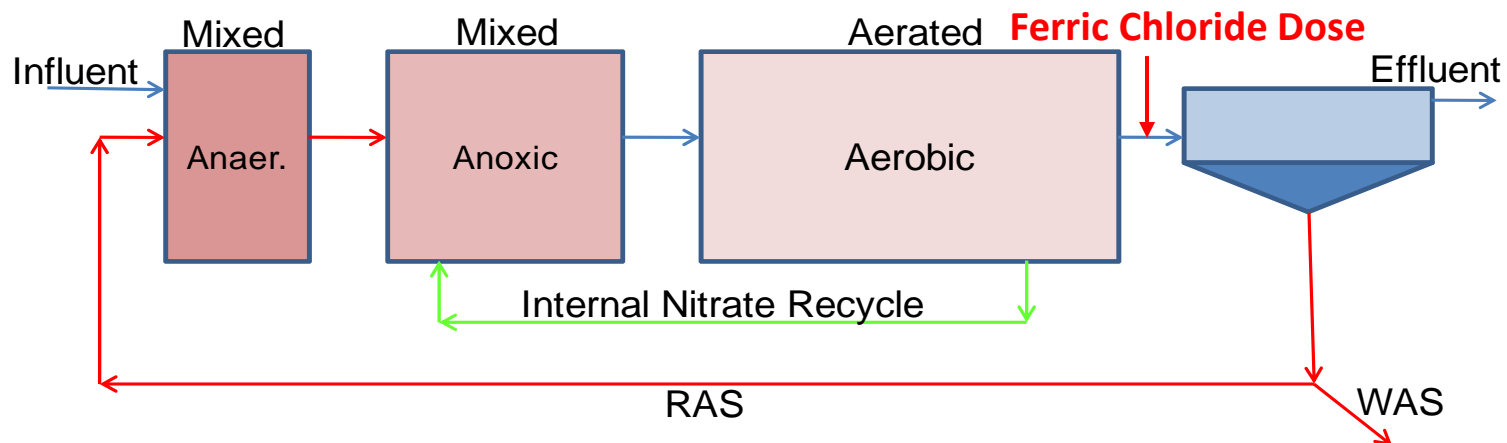
Ferric Dosing Pilot

➤ First pilot testing period

- September 3 to October 5, 2013 (5 weeks)
 - Low flow period
 - 35 mg/L ferric dose (300 gpd ferric, Q = 12 MGD)

This dose is likely too high to be considered polishing

Fe : P molar dosage of 7:1

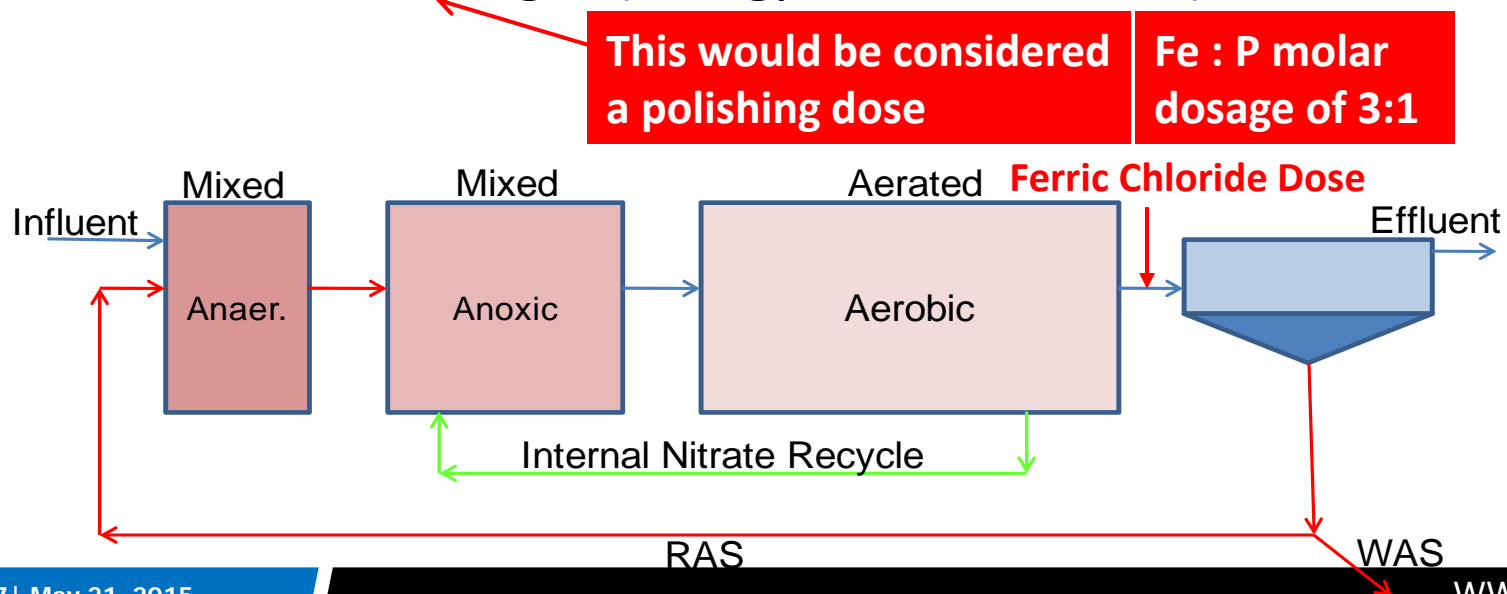


Ferric Dosing Pilot

➤ Second pilot testing period

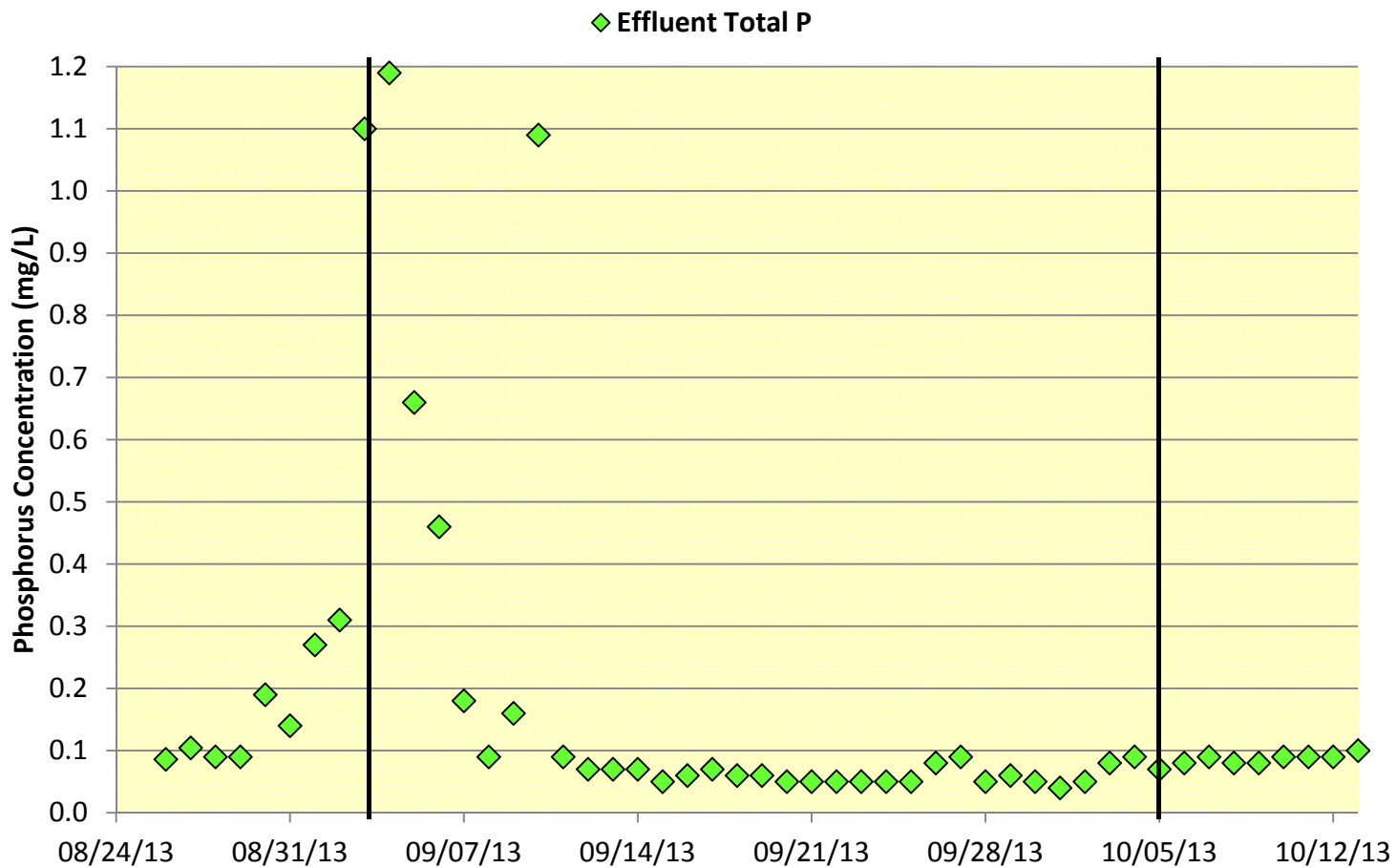
■ June 2 to August 10, 2014 (10 weeks)

- High flow period
- Initial ferric dose of 19 mg/L (200 gpd ferric, Q = 15 MGD)
- Ended at 11.5 mg/L (130 gpd, Q = 16 MGD)



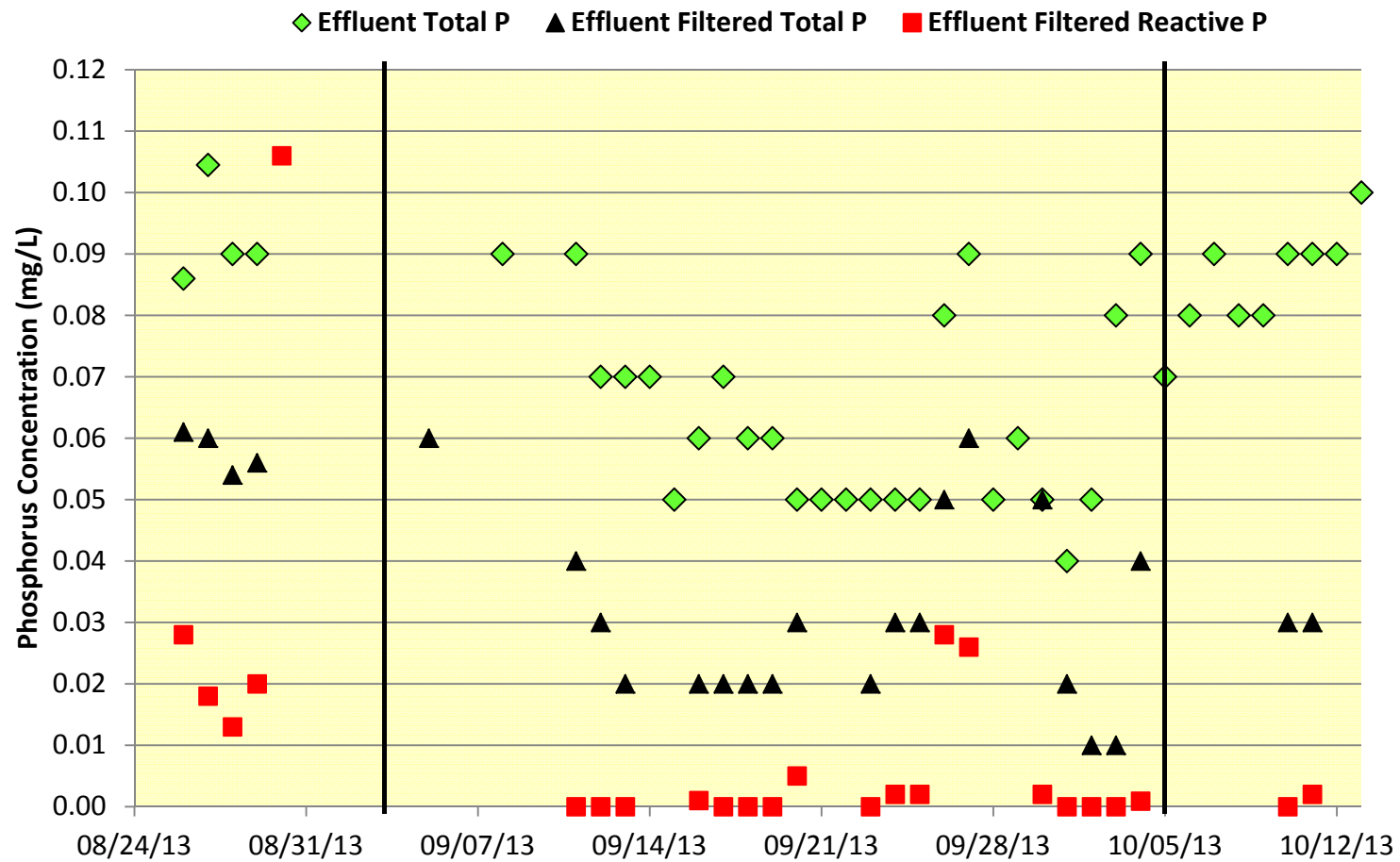
2013 Pilot Results

➤ Effluent total P



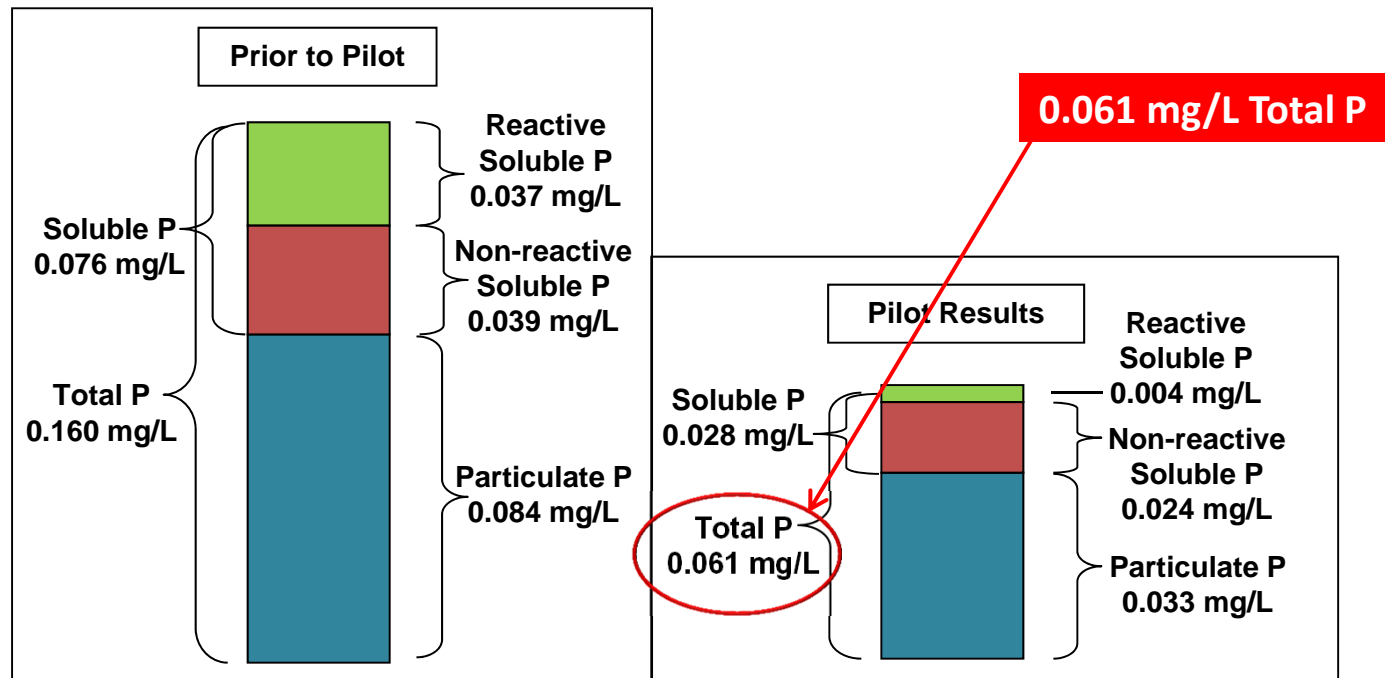
2013 Pilot Results

➤ Effluent P speciation data



2013 Pilot Results

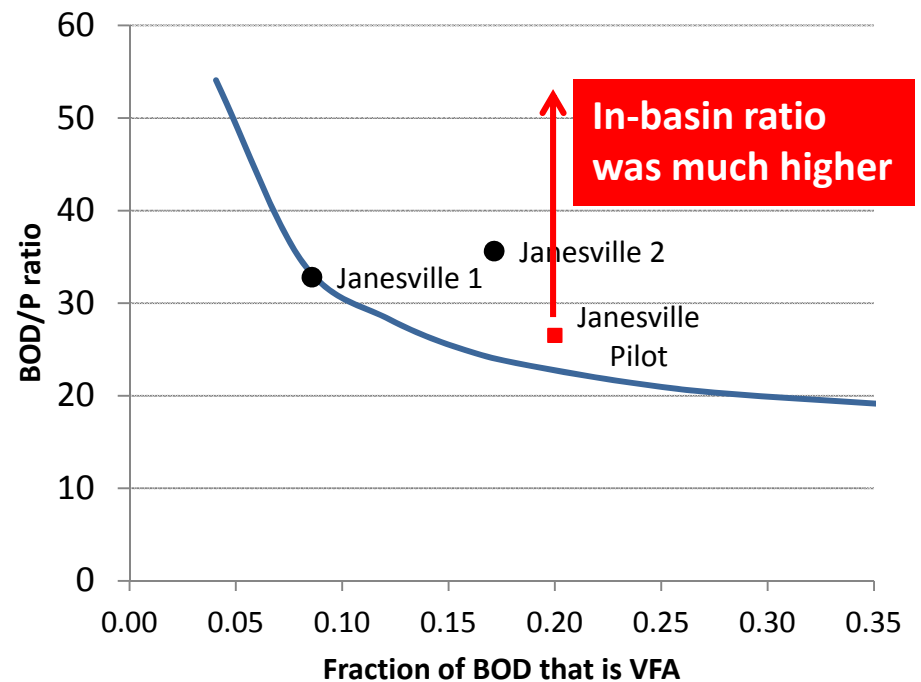
- Effluent phosphorus speciation – average values
 - Note: Ortho P is part of reactive P



2013 Pilot Results

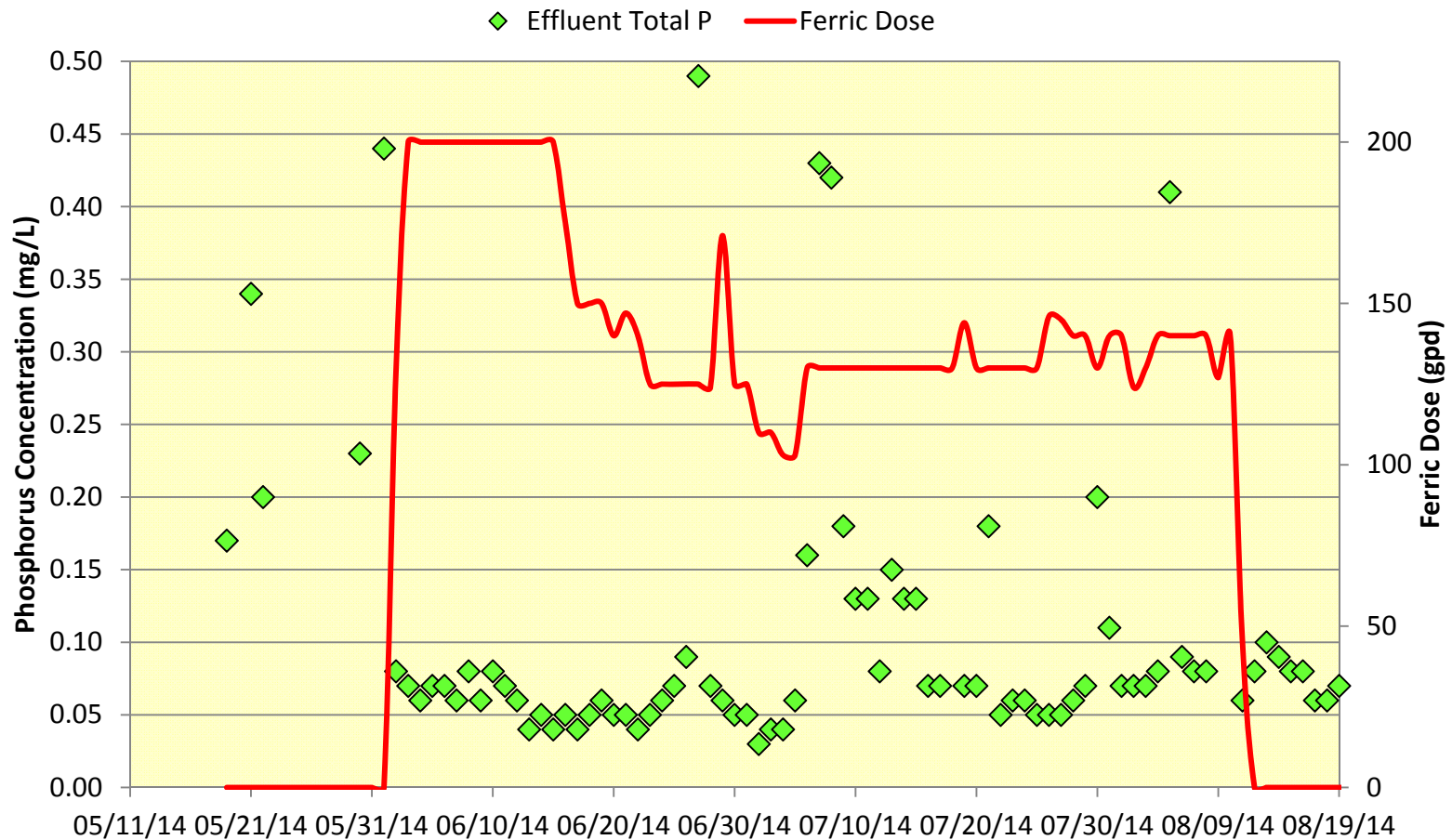
➤ Observations

- BOD:P ratio 26.5
- Target P was 0.1 mg/L
- 0.06 mg/L result suggested over-dose
- BPR was not affected
 - Following month P of 0.10 mg/L



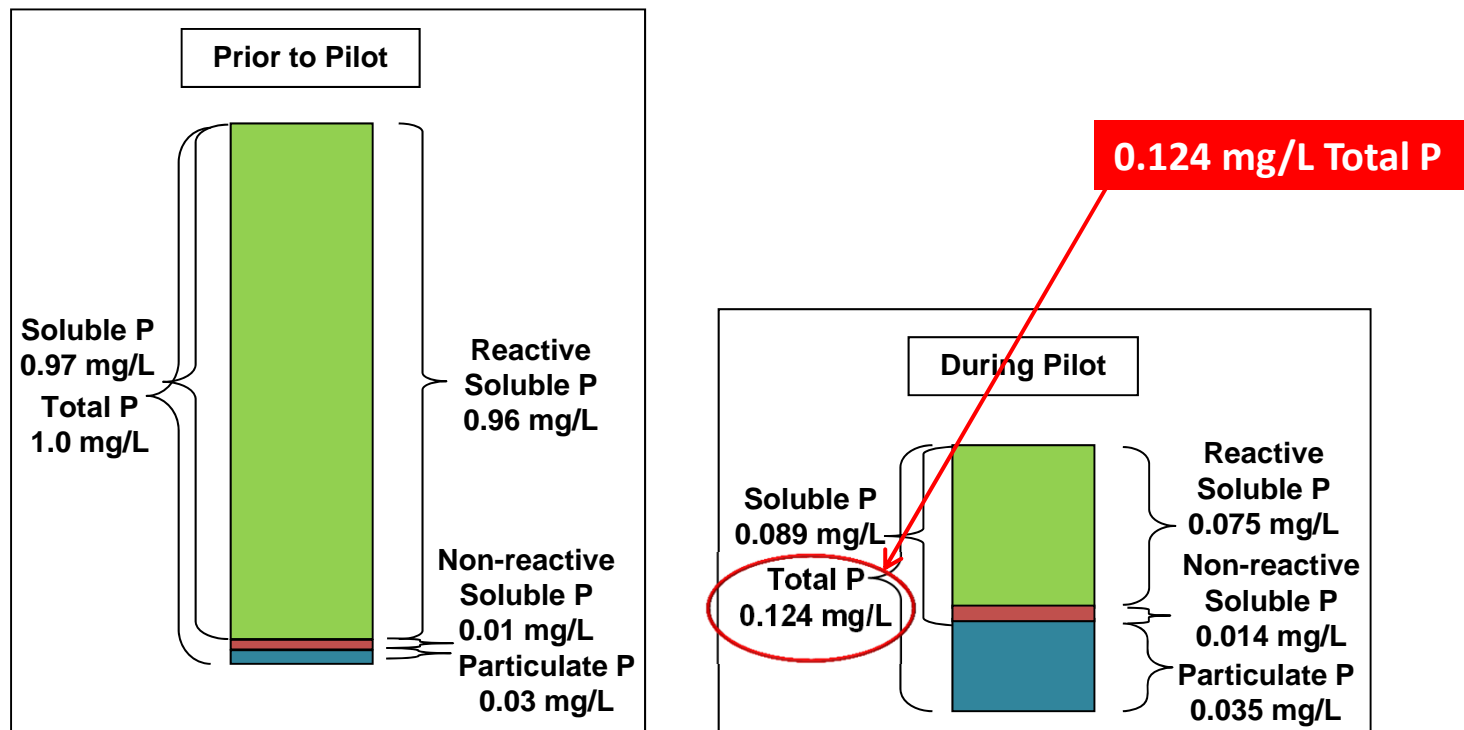
2014 Pilot Results

➤ Effluent total P versus ferric dose



2014 Pilot Results

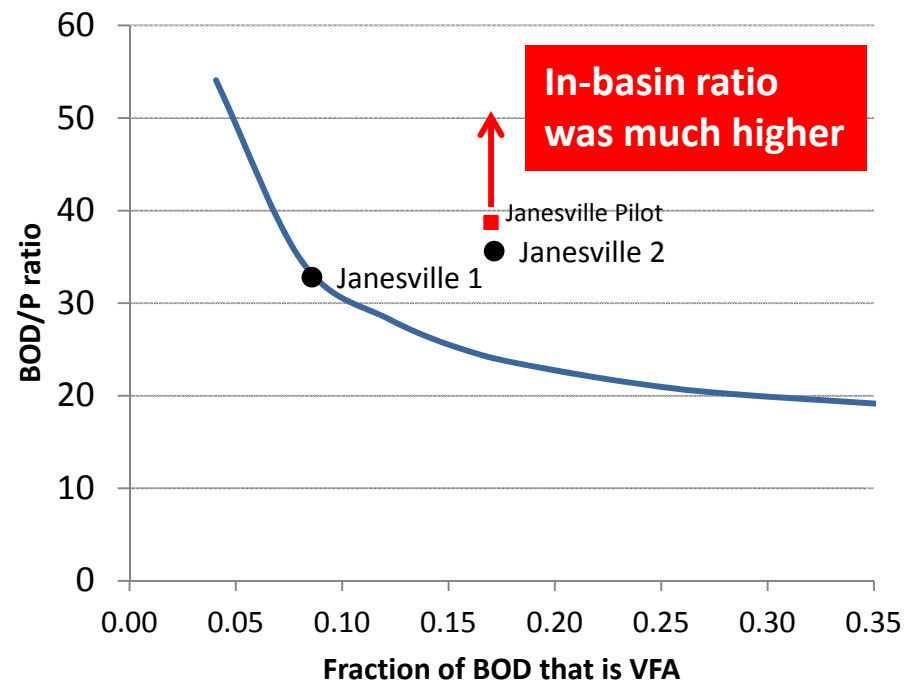
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2014 Pilot Results

➤ Observations

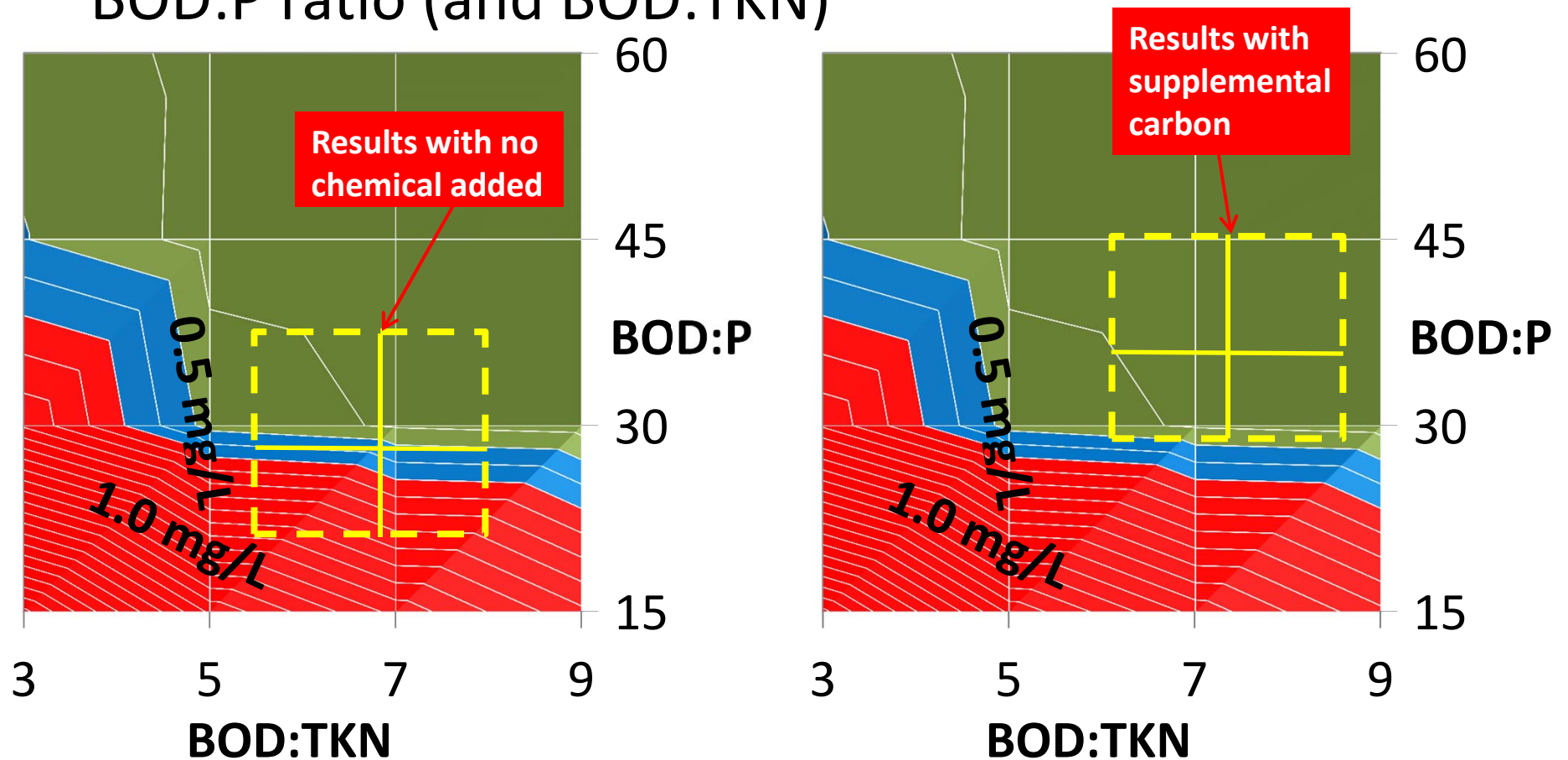
- BOD:P ratio 38.7
- Target P was 0.1 mg/L
- 0.12 mg/L result suggested under-dose
- BPR was not affected
 - Following month P of 0.12 mg/L



BPR + Supplemental Carbon

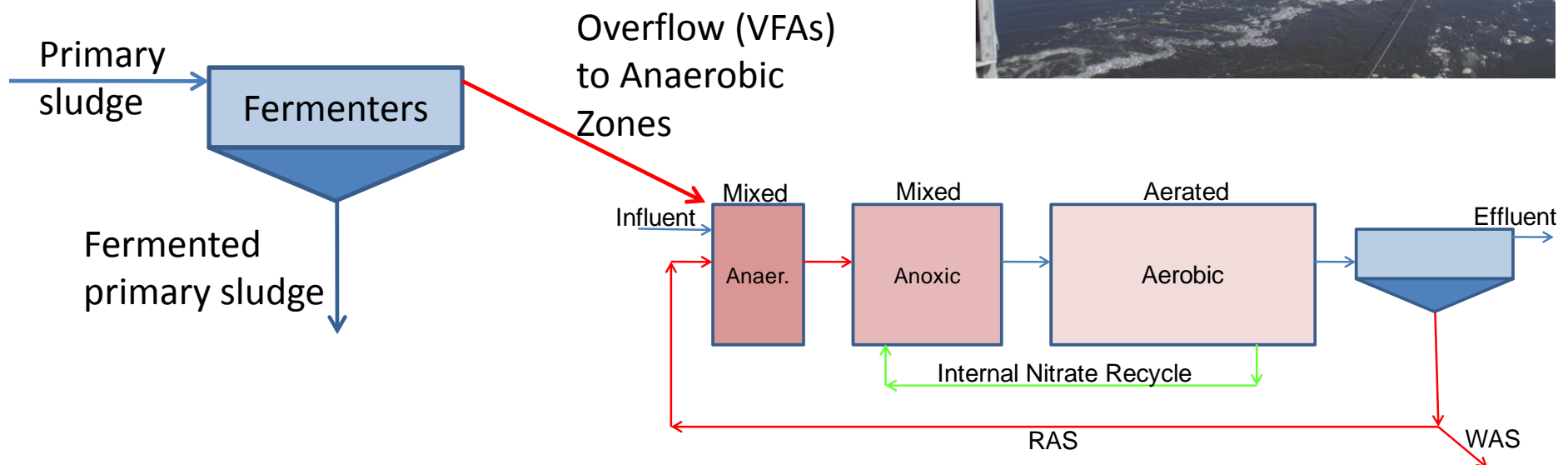
BPR + Supplemental Carbon

- Supplemental carbon can be added to increase BOD:P ratio (and BOD:TKN)



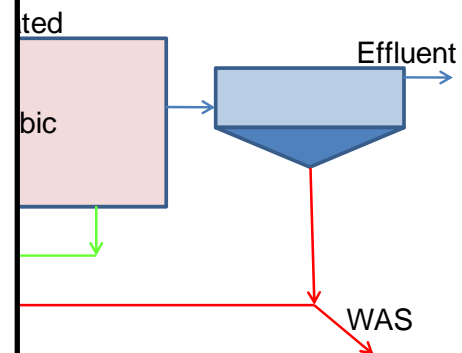
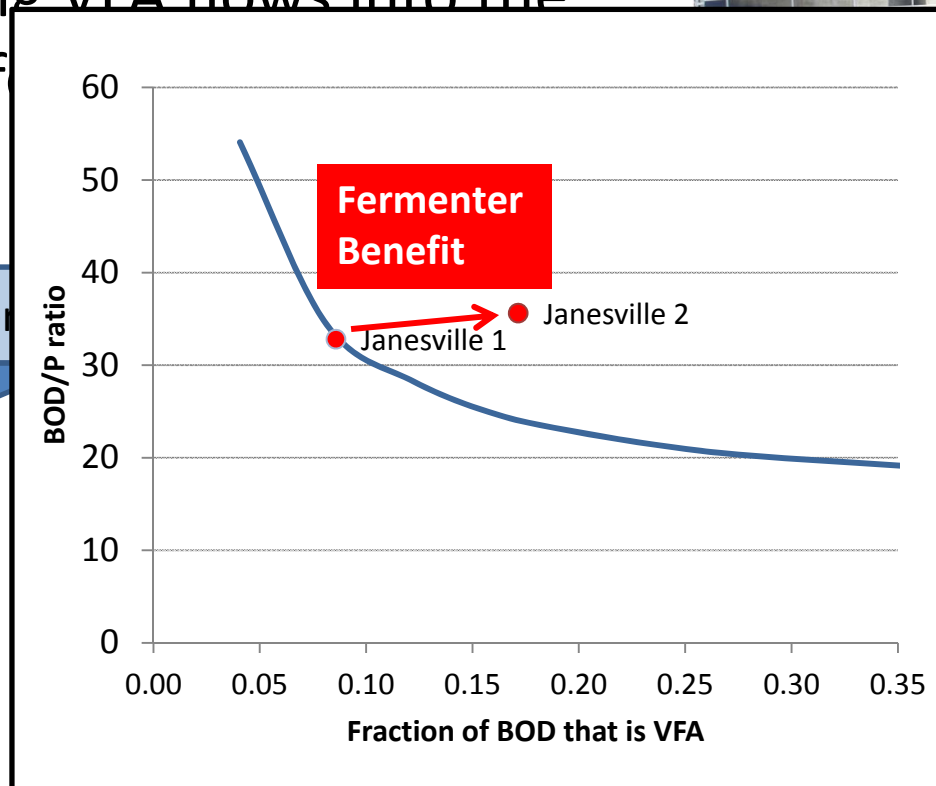
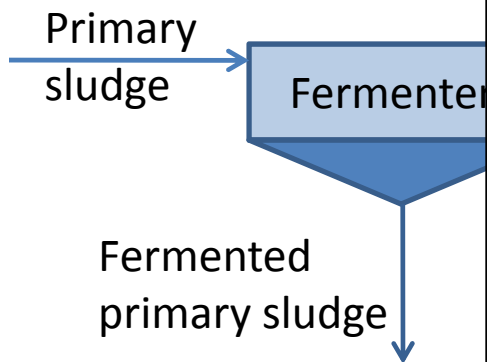
BPR + Supplemental Carbon

- Overflow from fermenters provides additional VFA for BPR
- The remaining VFA flows into the anoxic zone for biological nitrogen removal



BPR + Supplemental Carbon

- Overflow from fermenters provides additional VFA for BPR
- The remaining VFA flows into the anoxic zone for removal



Supplemental Carbon Pilot

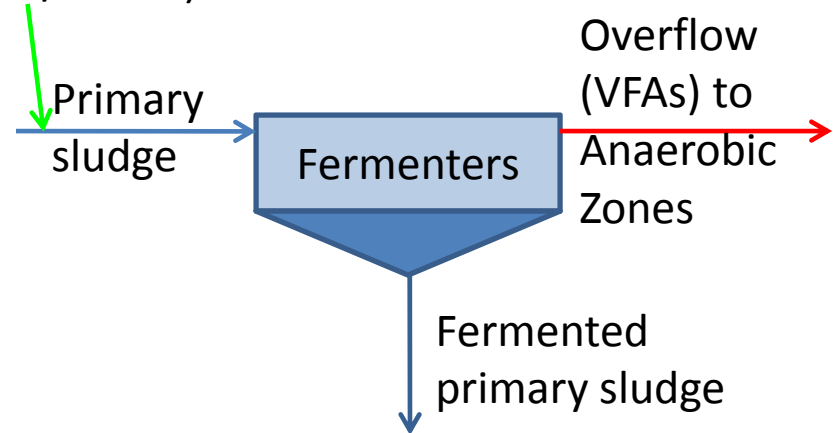
- Evaluate feeding supplemental carbon from QLF Specialty Products
 - Liquid molasses blend product
 - 7.3 lbs COD per gallon (875,000 mg/L)
- Pilot Goal
 - Stabilize BPR performance near 0.10 mg/L effluent total-P (**no filters and no ferric chloride**)

Supplemental Carbon Pilot

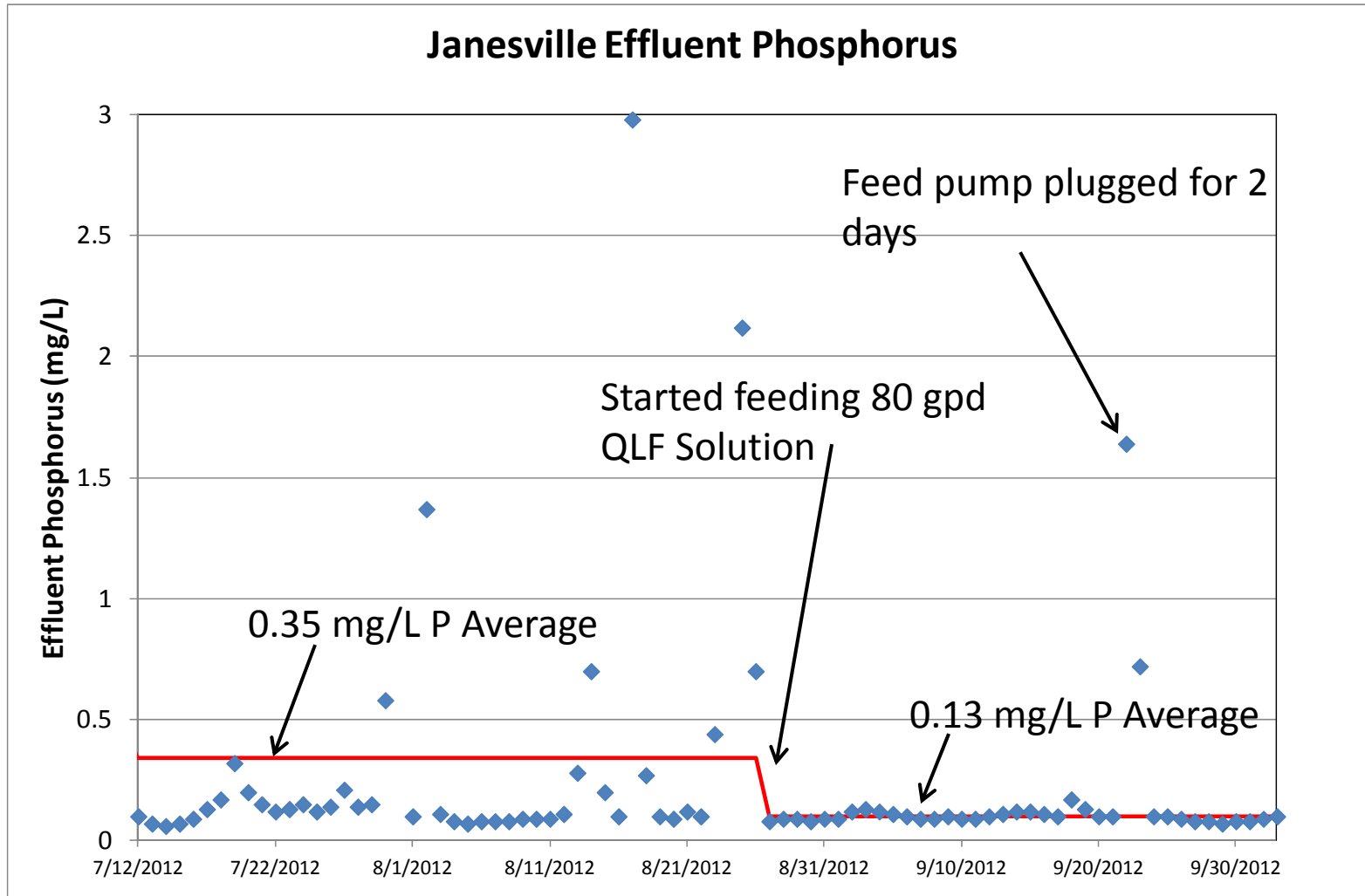
- QLF product fed into fermenters
 - Fermenters convert product to VFA's
 - VFA loading in fermenter overflow increased



80 gpd QLF Feed
(600 lb/d COD)



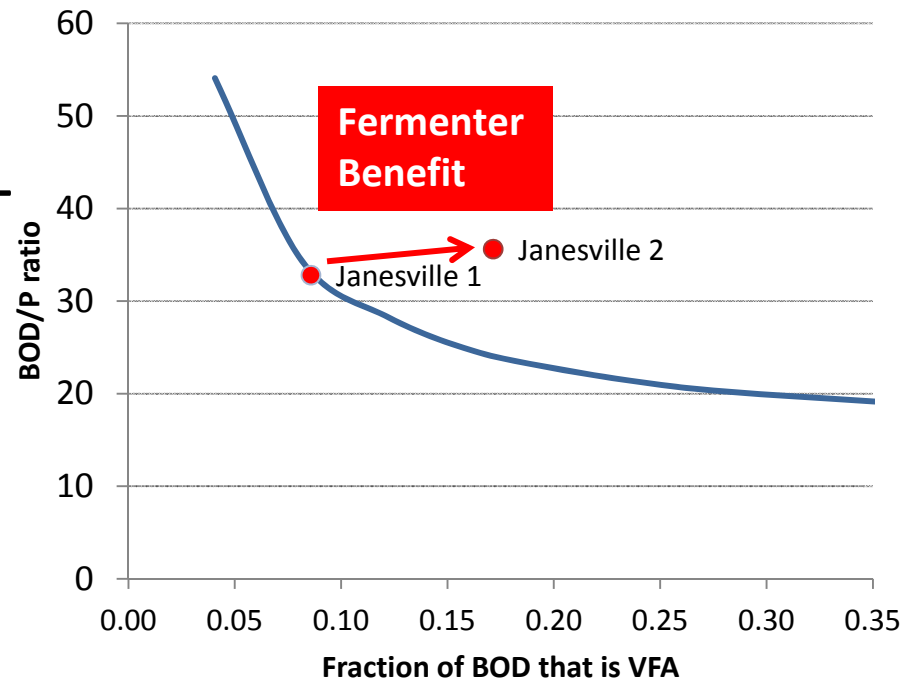
Supplemental Carbon Pilot



Supplemental Carbon Pilot

➤ Observations

- Target P was 0.1 mg/L
- Supplemental carbon dose achieved 0.13 mg/L
- Ortho-P was stable at 0.06 mg/L
 - Limit for BPR?
- Another “tool in the tool box”



Take-Away Points

- Foundation of the process is BPR
 - Focus on keeping BPR happy
- Use of chemicals does not hurt BPR process
- Combination of BPR + chemicals:
 - Can produce low level performance
 - Can improve stability
 - May be more cost effective than chemical alone
- Supplemental carbon is another option
 - Improves both P removal and N removal

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