

Upgrading Lagoons to Remove Ammonia, Nitrogen, and Phosphorus

***nutrient removal in
cold-climate lagoon systems**

October 7, 2015

3:15–4:00pm

Session M

Room Tamboti / Aloes-wood

optAER™ Treatment Processes



Aerated Lagoons
BOD & TSS Removal



SAGR
Nitrification
BOD/TSS Polishing
Partial Disinfection



ANSAGR
and/or Effluent
Recycle
Denitrification



optTPhos
Tertiary Filtration
TP Removal



öPTAER™ Treatment Processes

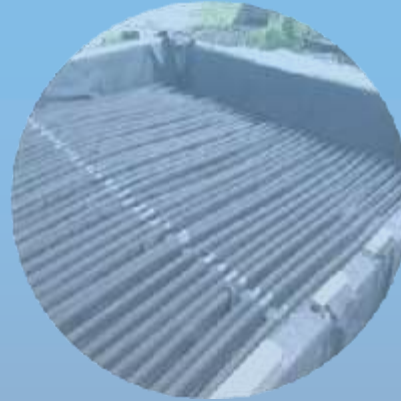


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OptAER™ lagoon aeration components



**Pre-Fabricated
Building**



PD Blowers



**Buried Main
Air Supply**



Floating Laterals



**Self-Tensioning
Assembly**



**Fine & Coarse
Bubble Aeration**



Baffle Curtain

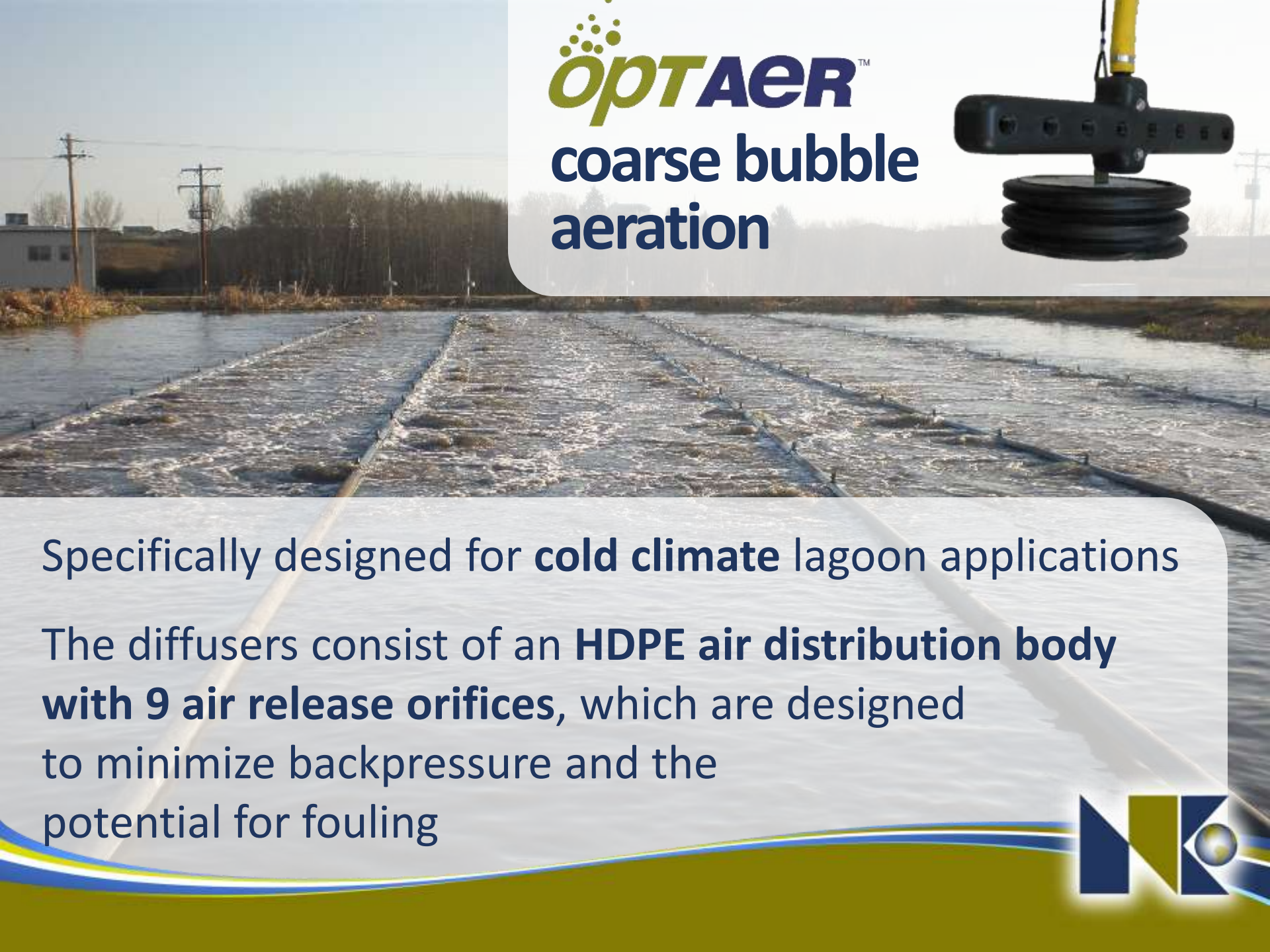


optAER™ fine bubble aeration

Excellent **oxygen transfer** rate at a wide range of airflows

Specifically designed for **cold climate** lagoon applications





öPTAER™ coarse bubble aeration



Specifically designed for **cold climate** lagoon applications

The diffusers consist of an **HDPE air distribution body with 9 air release orifices**, which are designed to minimize backpressure and the potential for fouling





self-tensioning devices

Cables are fastened to **anchors** at the tops of the berm

Allows for **expansion and contraction** of laterals and water level fluctuations



float/sink lateral system



Dry Install



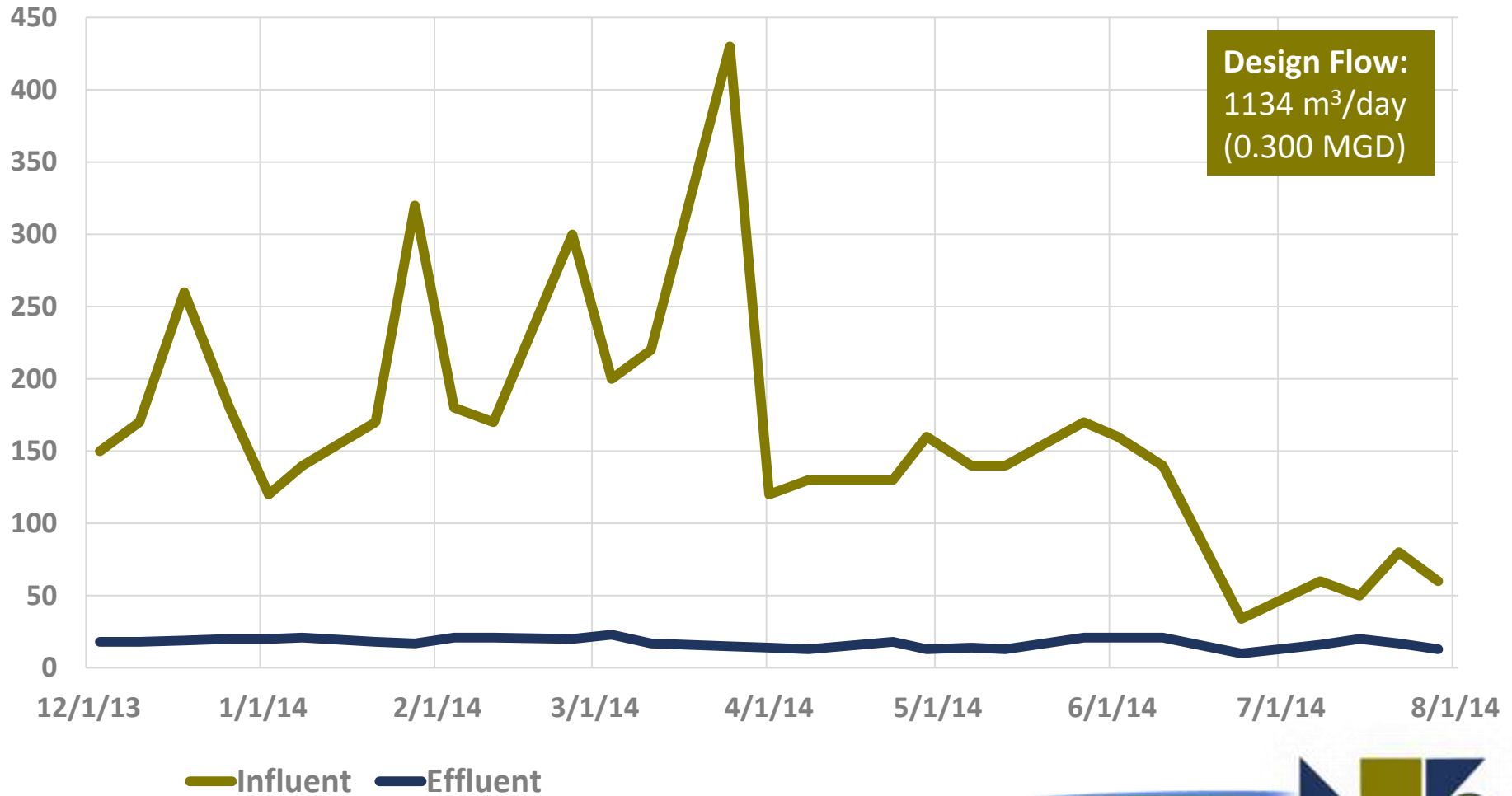
Wet Install

optAER™
Complete Mix Cell



Kingsley, Iowa

Lagoon cBOD₅ (mg/L)



öPTAER™ Treatment Processes

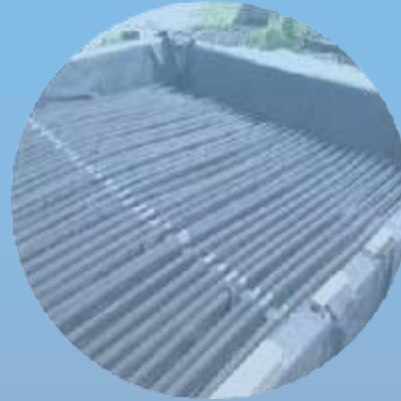


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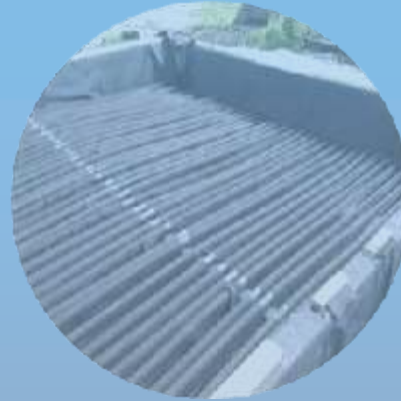
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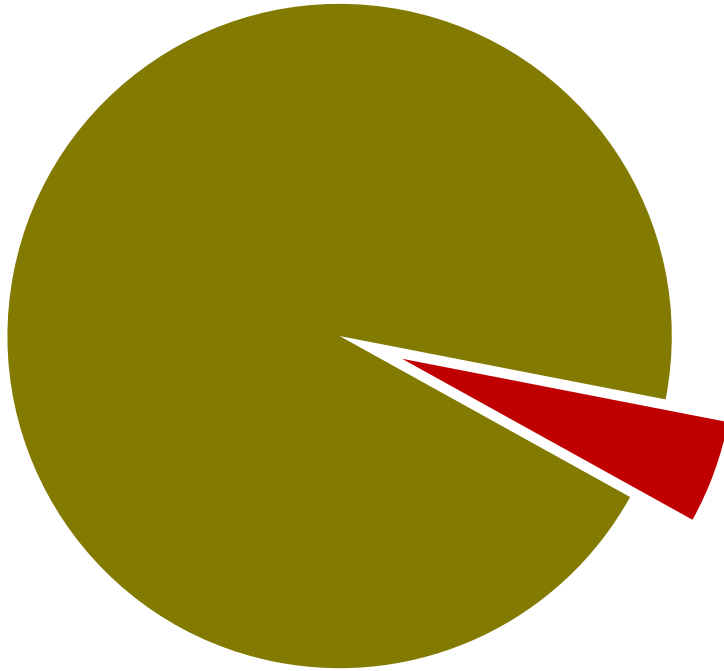


öTPhos
Tertiary Filtration
TP Removal



why is removing ammonia important?

Terminology



NH_4^+ (Ammonium)
+ NH_3 (Ammonia/Un-ionized)

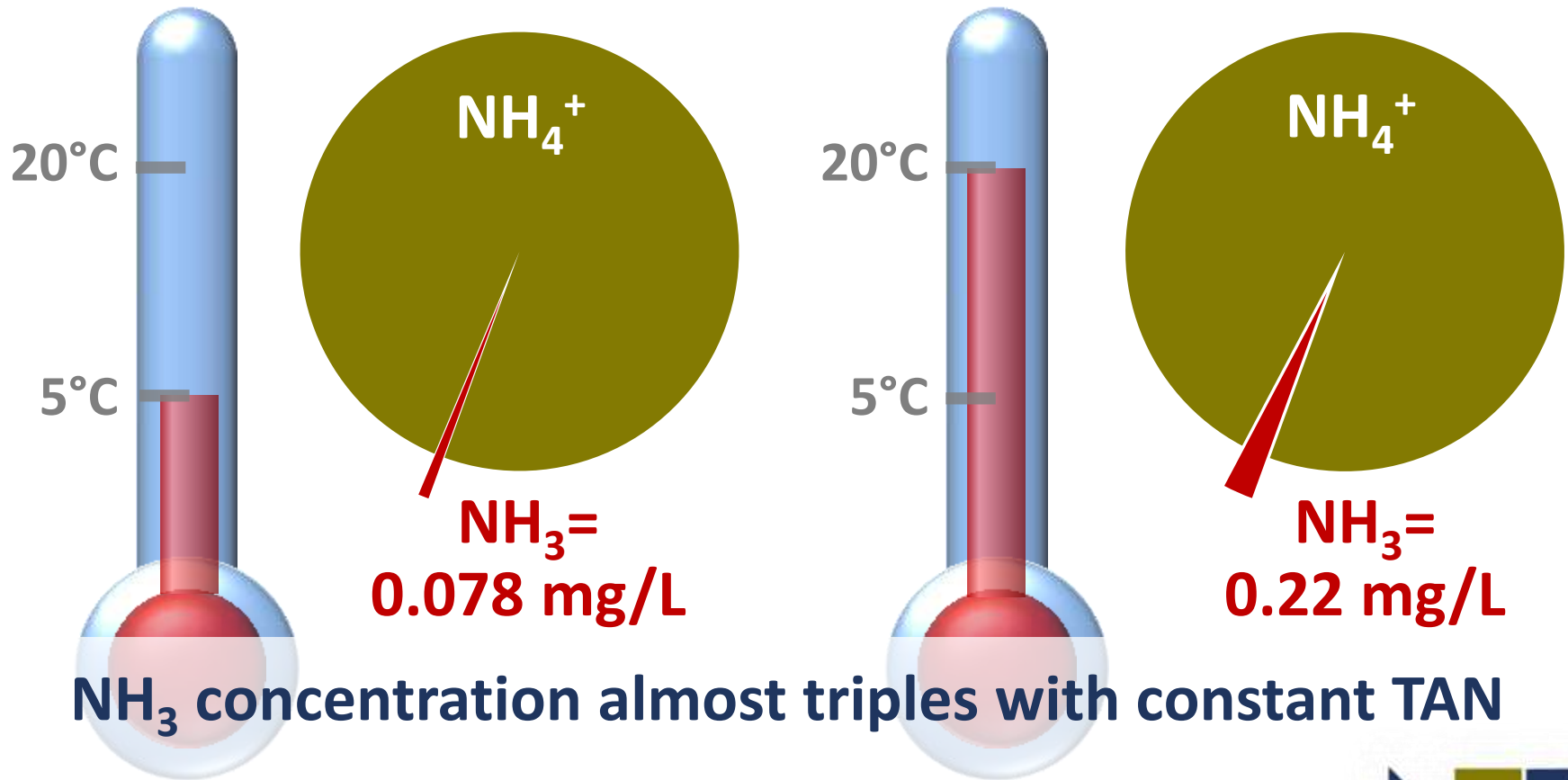
TAN (Total Ammonia)

0.1 mg/L NH_3 is generally
considered “non-toxic”



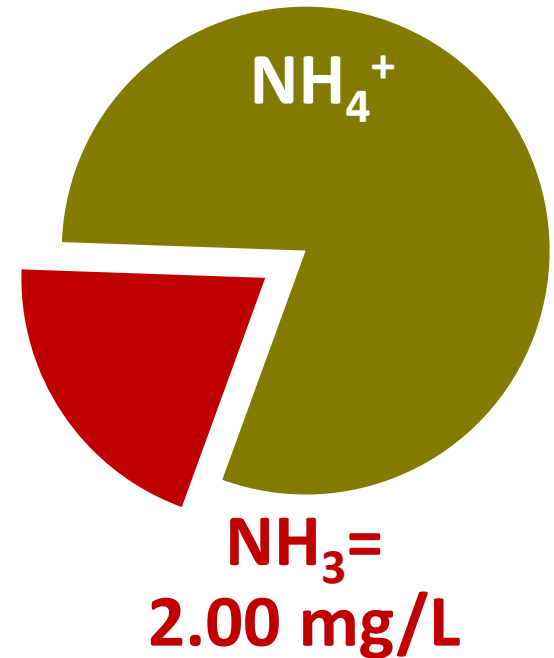
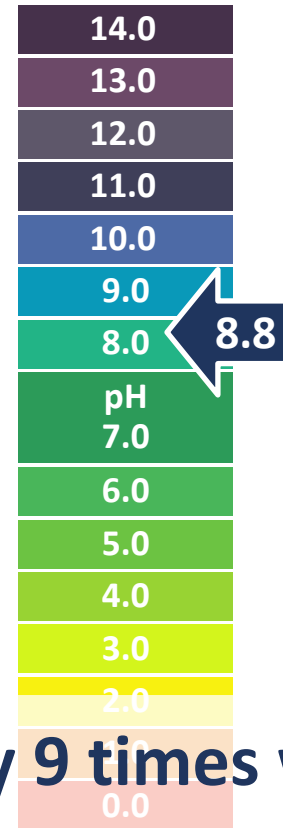
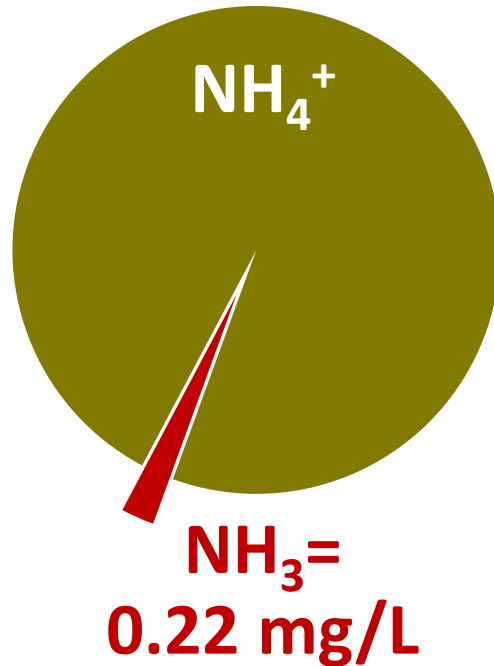
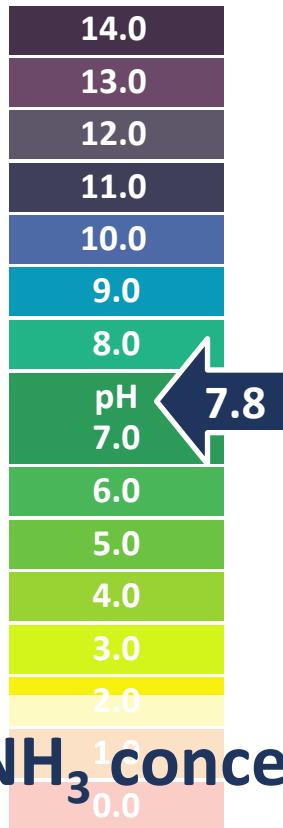
why is removing ammonia important?

Assuming TAN=10 mg/L and pH=7.8



why is removing ammonia important?

Assuming TAN=10 mg/L and water is 20°C



NH_3 concentration increases by 9 times with constant TAN



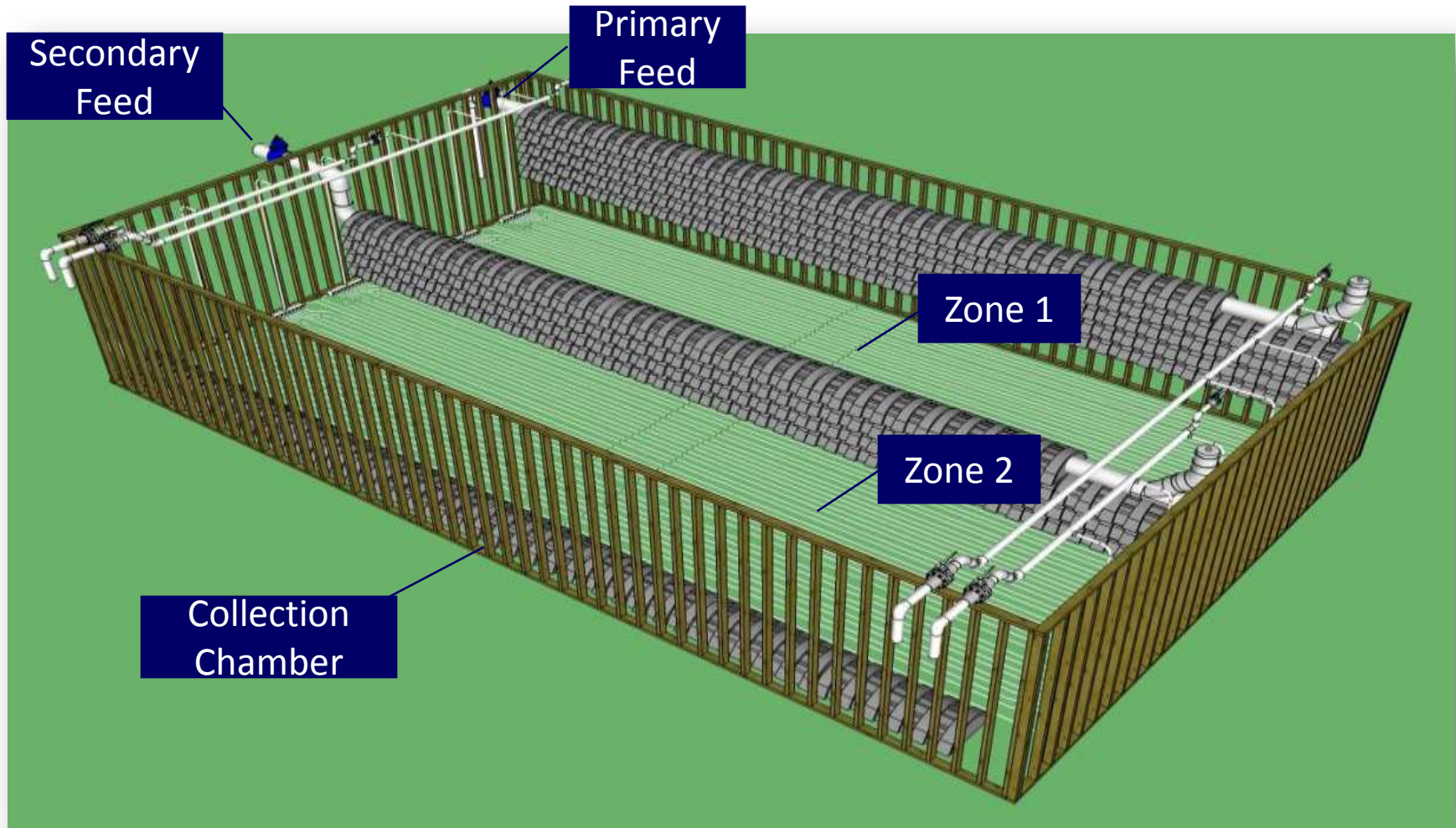
what is a **SAGR**

Fully aerated **coarse gravel** bed reactor

- Water flows through the substrate **horizontally**
- Stable dense rock media which is **not susceptible** to temperature shock
- Designed for **cold water treatment**, the SAGR removes ammonia through nitrification and provides BOD/TSS polishing & partial disinfection



Submerged Attached Growth Reactor



SAGR performance data



University of Manitoba Third Party Winter Operation Verification Data (January 13 – April 21, 2010)

Parameters	SAGR Influent Averages (mg/L)	SAGR Effluent Averages (mg/L)	Removal
cBOD	47	2.1	95.5%
TSS	30	1.3	95.7%
TAN	24.9	0.12	99.5%
TKN	32.5	1.8	94.5%
FC (cfu/100mL)	253,000	13.5	99.99%
Average water temperature (°C)	0.3	1.0	



what makes the **SAGR** so effective?

Built-in temperature buffering: Rock media stabilizes biomass temperature during rapid water cool down

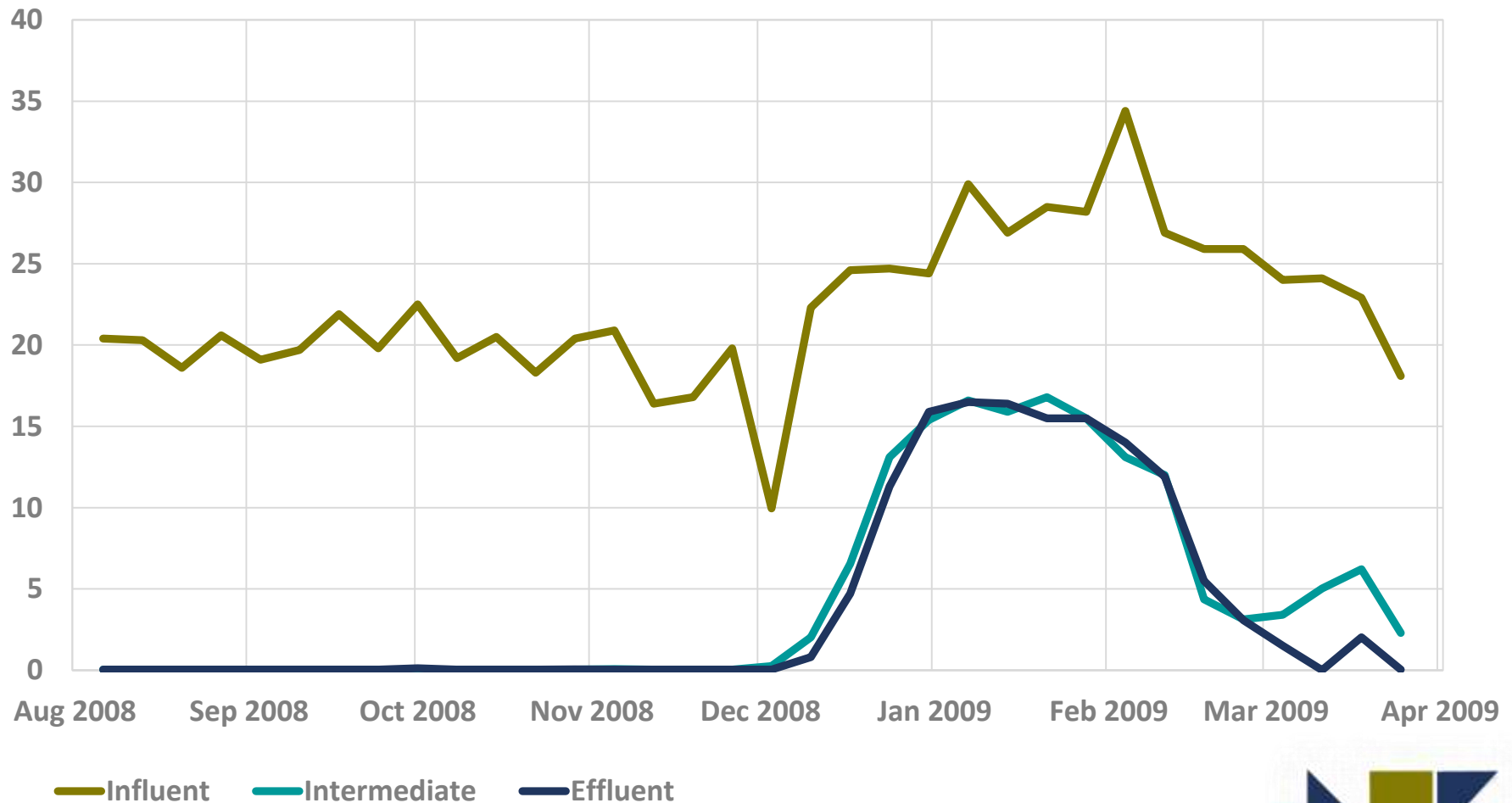
Non-turbulent environment: Allows nitrifier retention throughout the winter which eliminates the need to grow replacement nitrifiers.

Step-Feed: Prebuild and store excessive nitrifiers prior to water temperatures dropping below 1°C. The excess nitrifiers are needed once water temperatures drop and biomass growth slows.

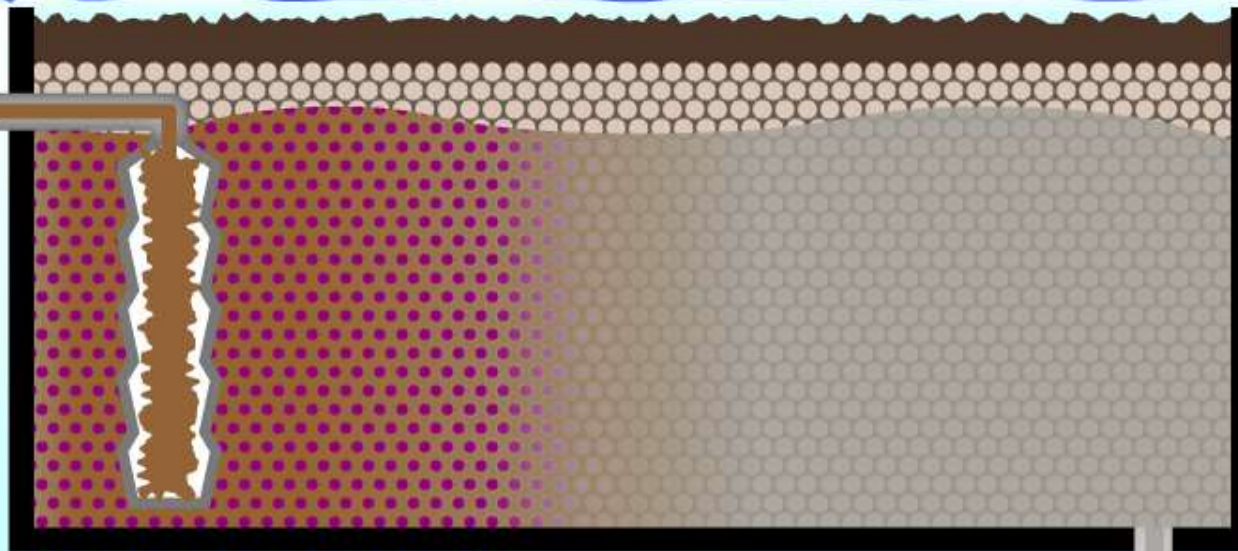


SAGR demonstration site: Steinbach MB

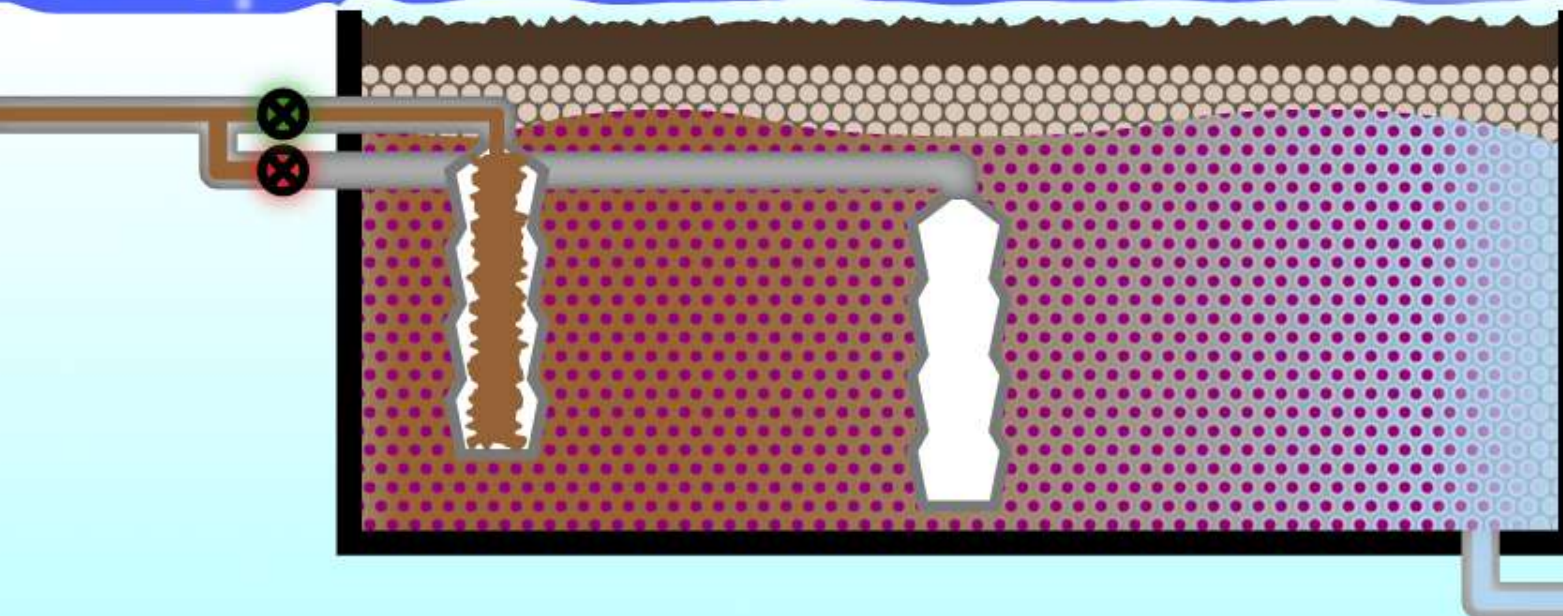
Train 1: TAN (mg/L) with No Step-Feed



SAGR without step-feed: winter



SAGR with step-feed: winter



SAGR projects

Legend

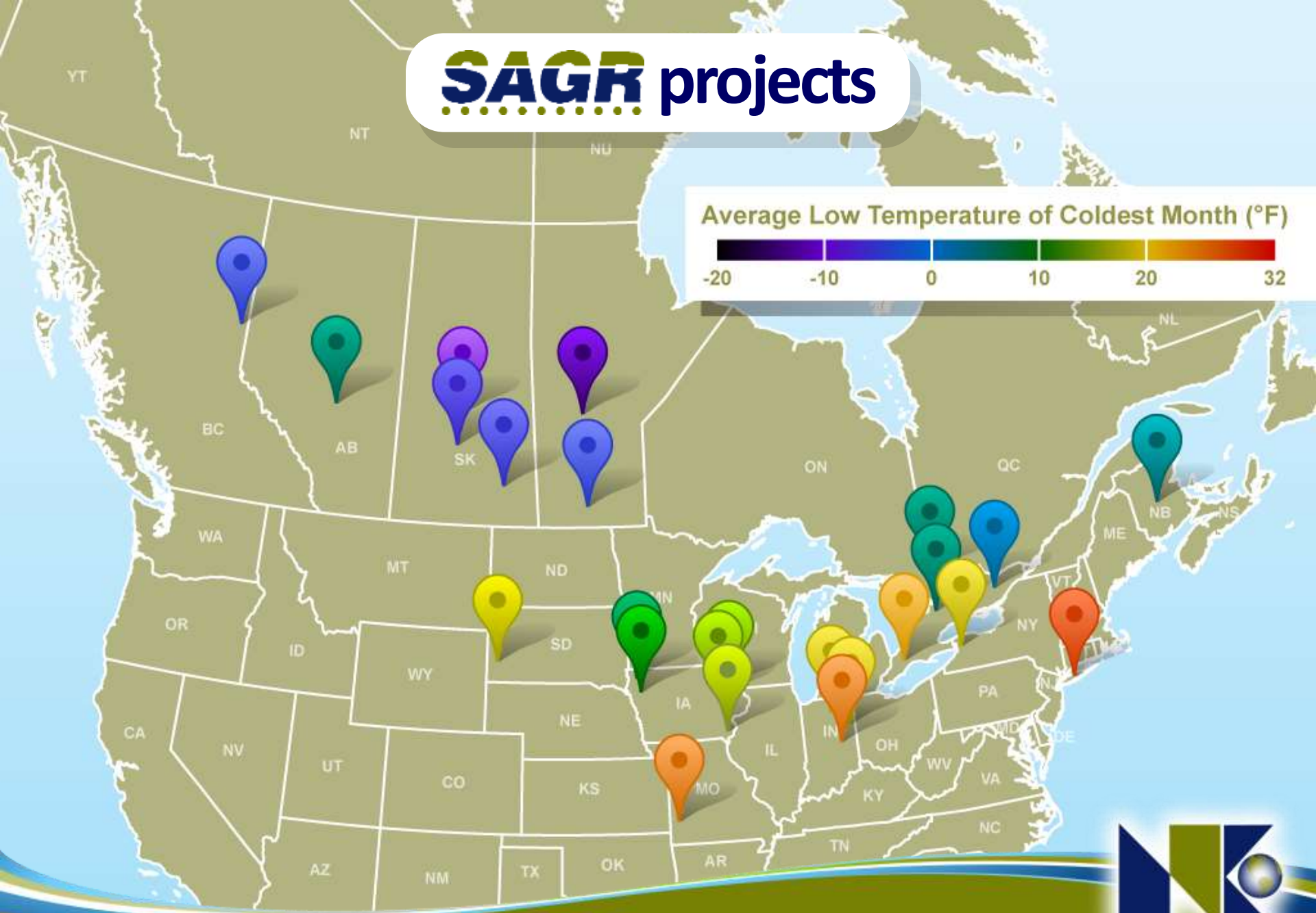
 SAGR projects in operation

 SAGR projects under construction



SAGR projects

Average Low Temperature of Coldest Month (°F)



öPTAER™ Treatment Processes



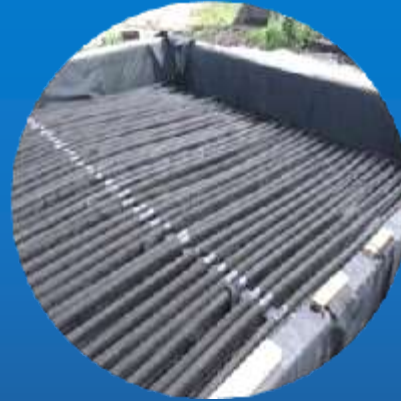
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öTPhos

Tertiary Filtration

TP Removal



what is an **ANSAGR**

Anoxic Submerged Attached Growth Reactor

- Total Nitrogen removal system (de-nitrification)
- Cloth-based media
- Designed for cold water TN treatment.

Effluent quality:

TN: <10 mg/L



ANSAGR performance data



Blumenort MB Total Nitrogen Demo November 2014 – March 2015

Parameters	SAGR Influent Avg (mg/L)	ANSAGR Influent Avg (mg/L)	ANSAGR Effluent Avg (mg/L)	Removal
TIN	37.6	39.8	6.2	83.5%
Nitrates & Nitrites	4.6	39.5	6.0	84.7%
TKN	42.6	4.7	5.6	86.9%
TAN	33.0	0.2	0.2	99.3%
Avg water temp (°C)	0.5	0.9	1.7	

Operating at 130% of design flow and load



optAER™ Treatment Processes



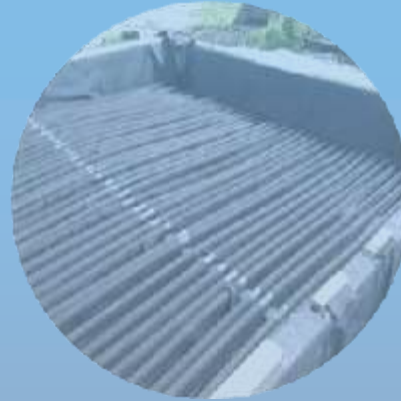
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Phosphorus Removal

TOTAL PHOSPHORUS REMOVAL

- **Rapid mix tank** for chemical dispersion and contact.
- **Slow mix tanks** for coagulation and flocculation.
- Small footprint, high performance tertiary cloth disk filters **or** settling in the lagoon.





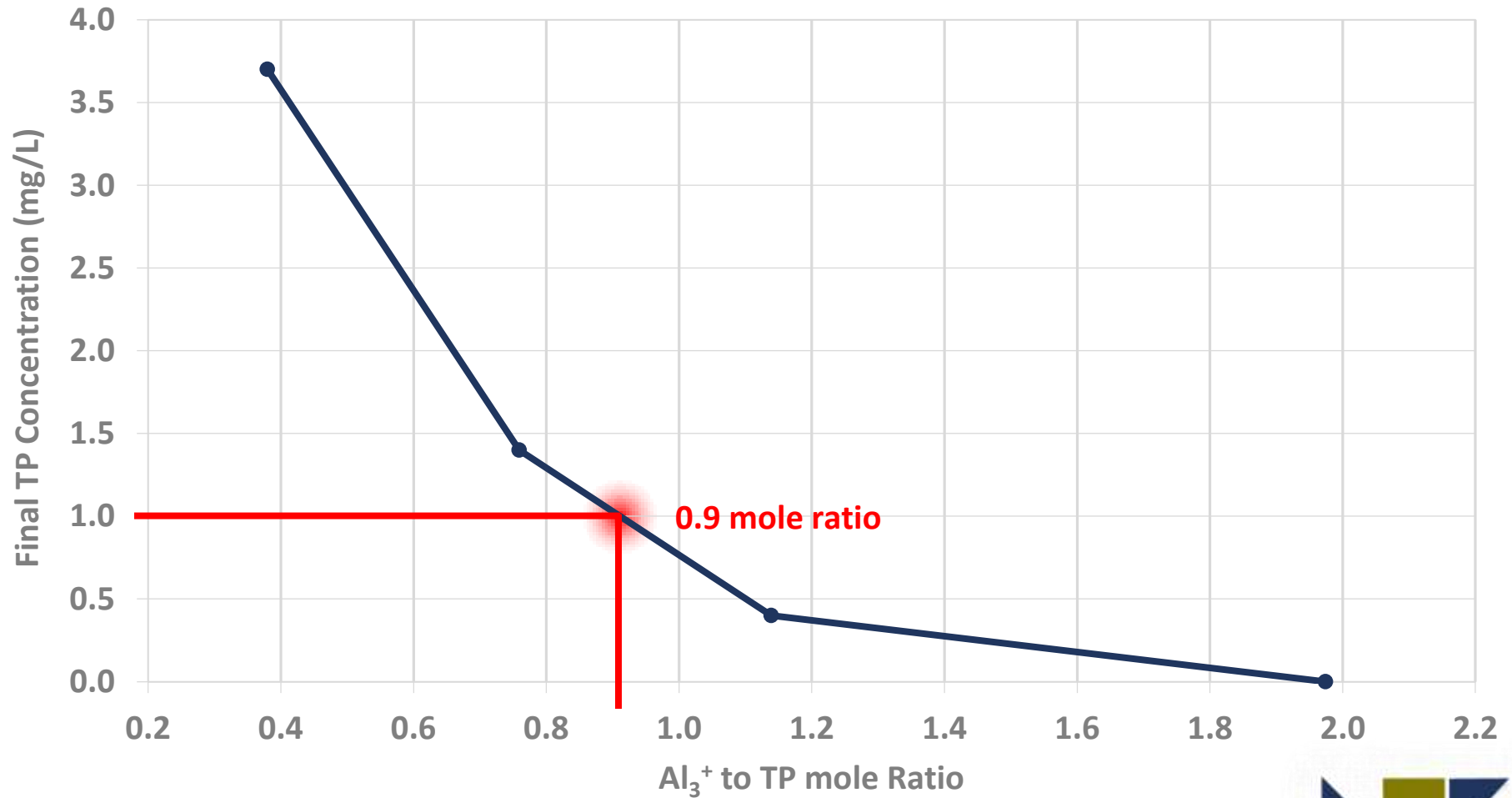
Tertiary Disk Filter

- **Smart Design:** user-friendly system on a small footprint
- **Flexible sizing:** for both small and large flow applications
- **High Performance:** can remove suspended solids to less than 5 mg/L, with low backwash



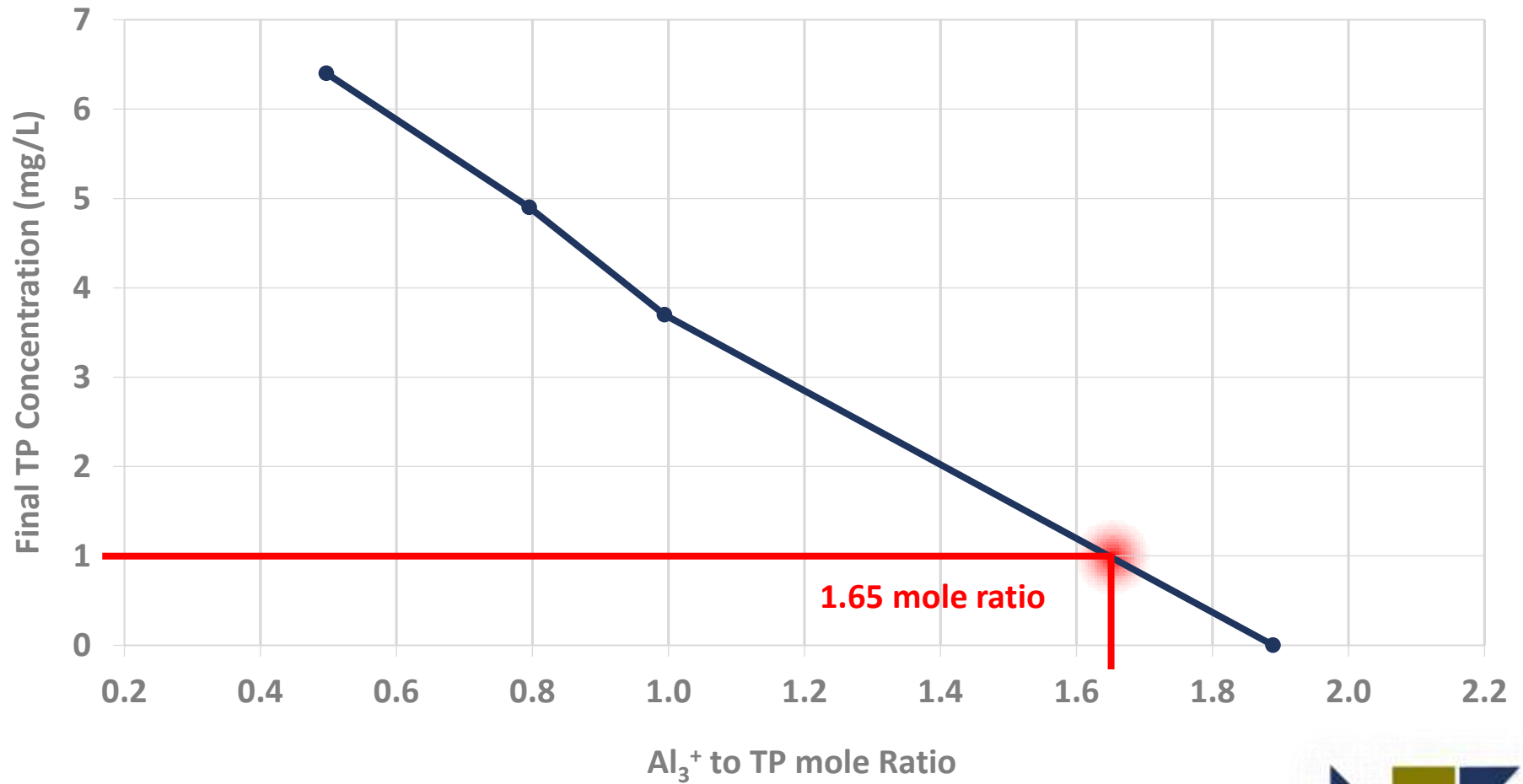
TPhos alum jar testing at 18°C

TP Removal vs. Al_3^+ /TP mole ratio



TPhos alum jar testing at 0.5°C

TP Removal vs. Al_3^+ /TP mole ratio



optAER™ Treatment Processes



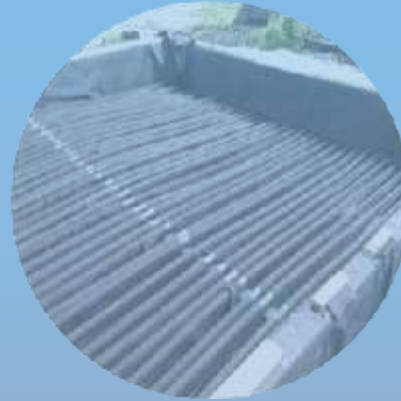
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Mentone, Indiana



Project Type:

Municipal
Wastewater

Design Flow:

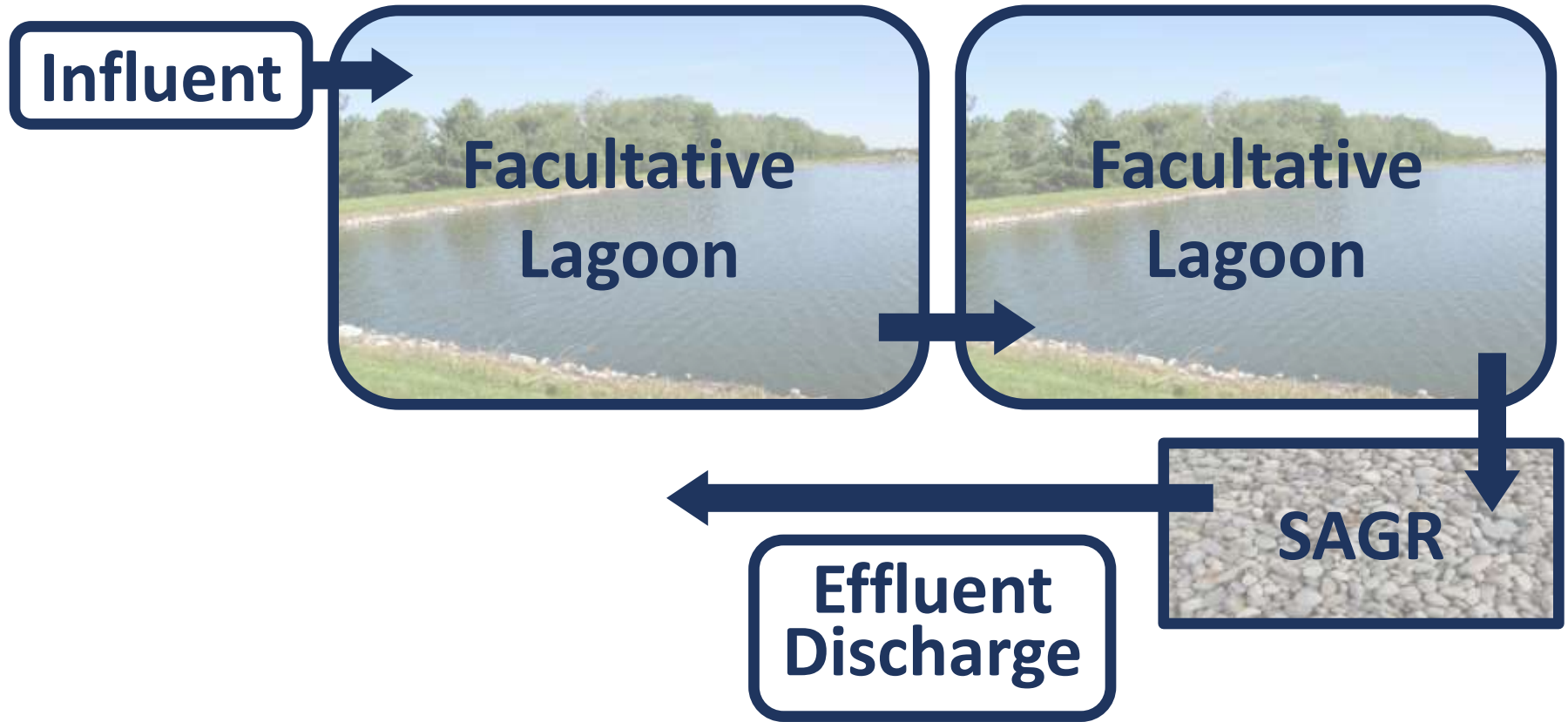
454 m³/day
(0.12 MGD)

Effluent Objective:

- Summer TAN: <9.6 mg/L
- Winter TAN: <10.4 mg/L
- BOD: <25 mg/L
- TSS: <70 mg/L



Mentone, Indiana

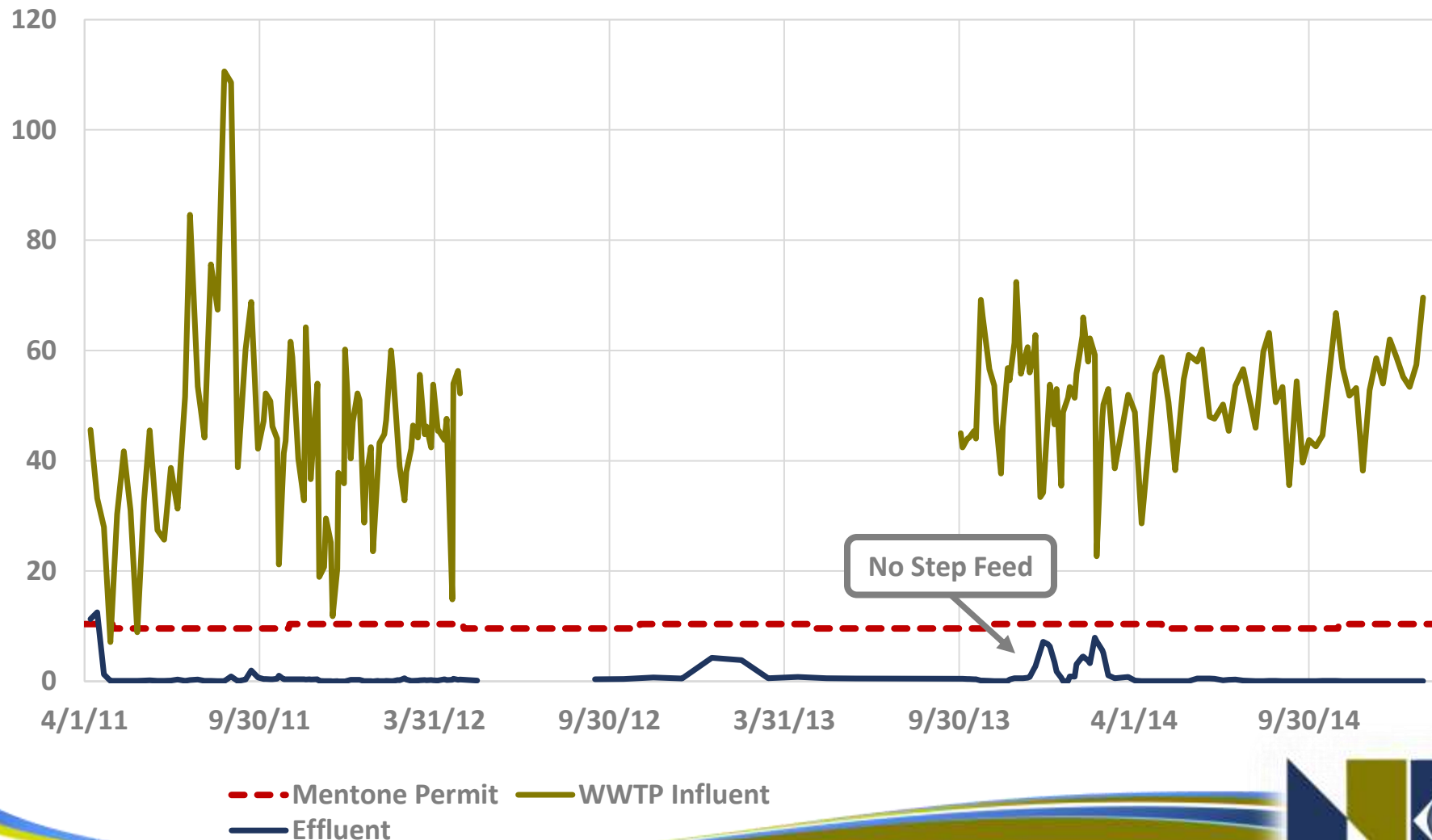


Mentone, Indiana



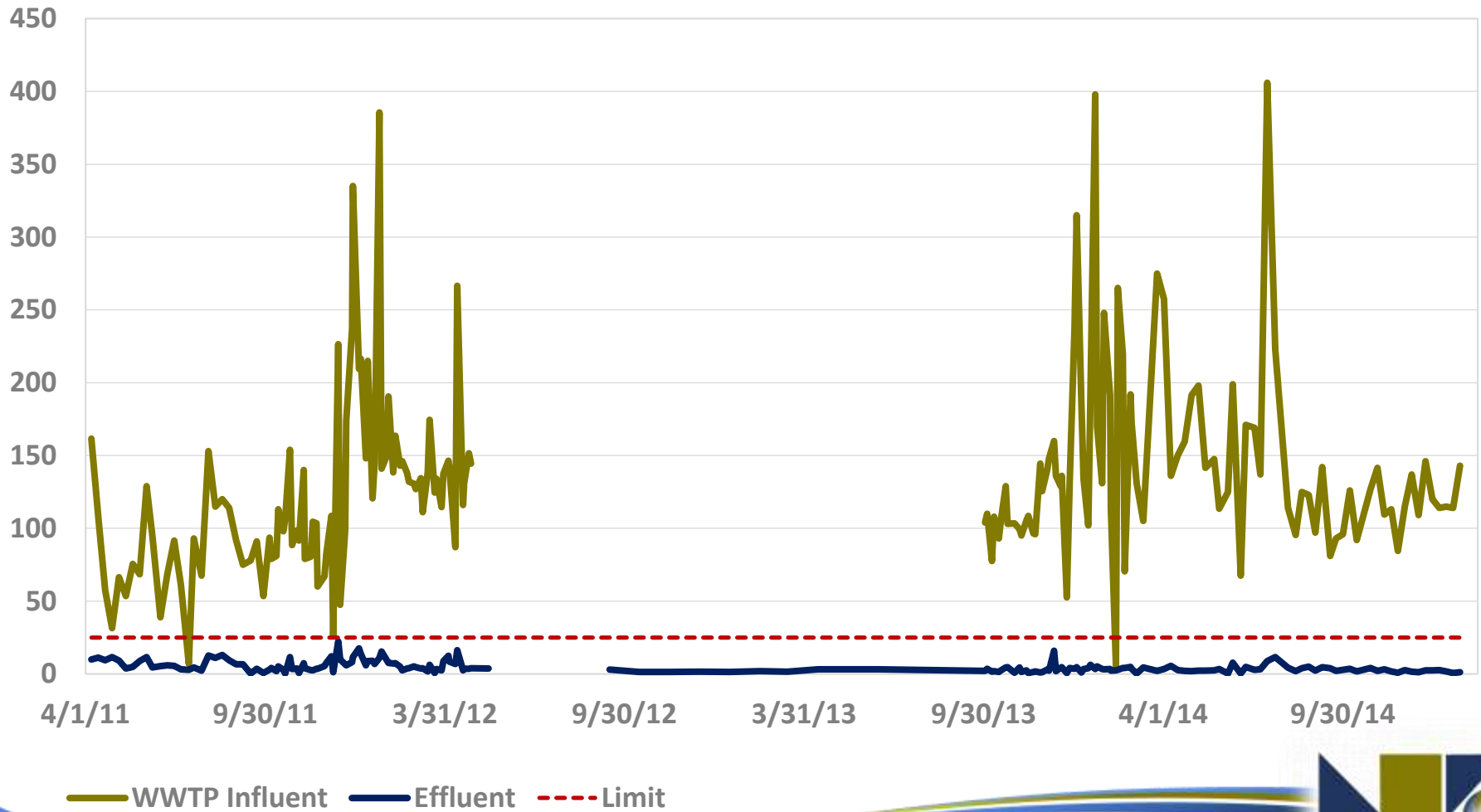
Mentone, Indiana

SAGR TAN (mg/L)



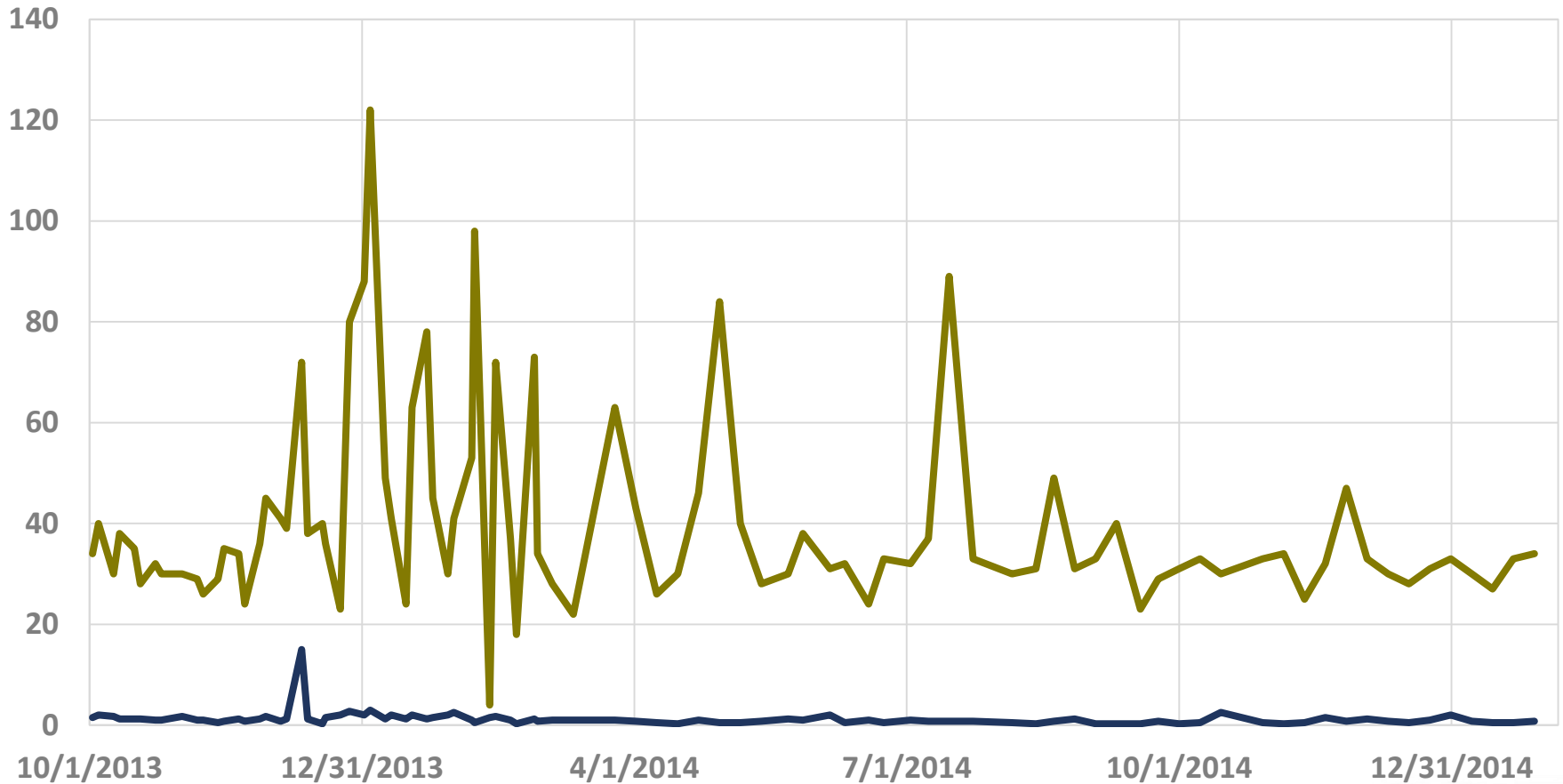
Mentone, Indiana

SAGR cBOD₅ (mg/L)



Mentone, Indiana

SAGR TSS (mg/L)



— WWTP Influent — Effluent





Kennard, Indiana

Project Type:

Municipal
Wastewater

Design Flow:

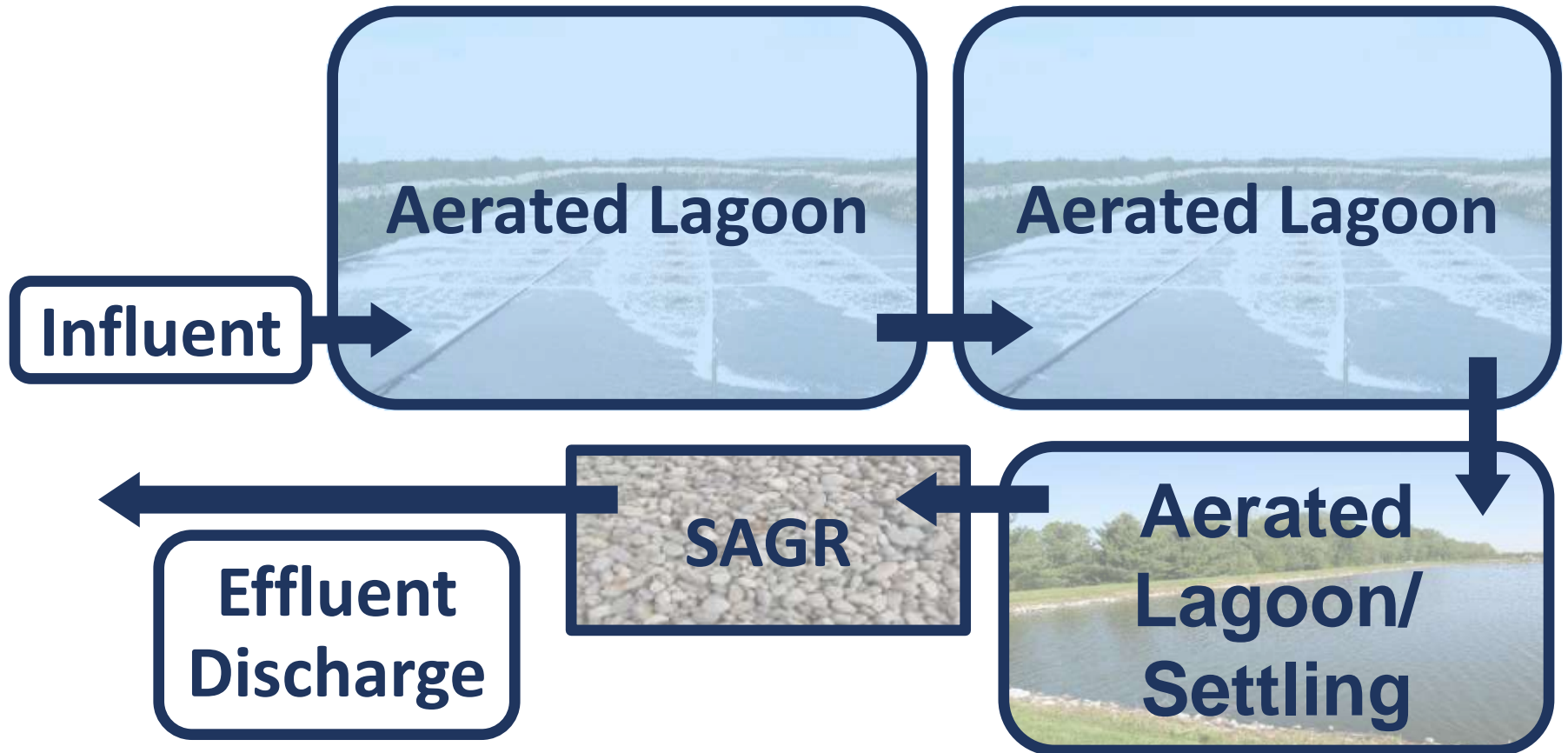
378 m³/day
(0.100 MGD)

Effluent Objective:

- Summer TAN: <1.5 mg/L
- Winter TAN: <3.0 mg/L
- BOD: <10 mg/L
- TSS: <12 mg/L



Kennard, Indiana

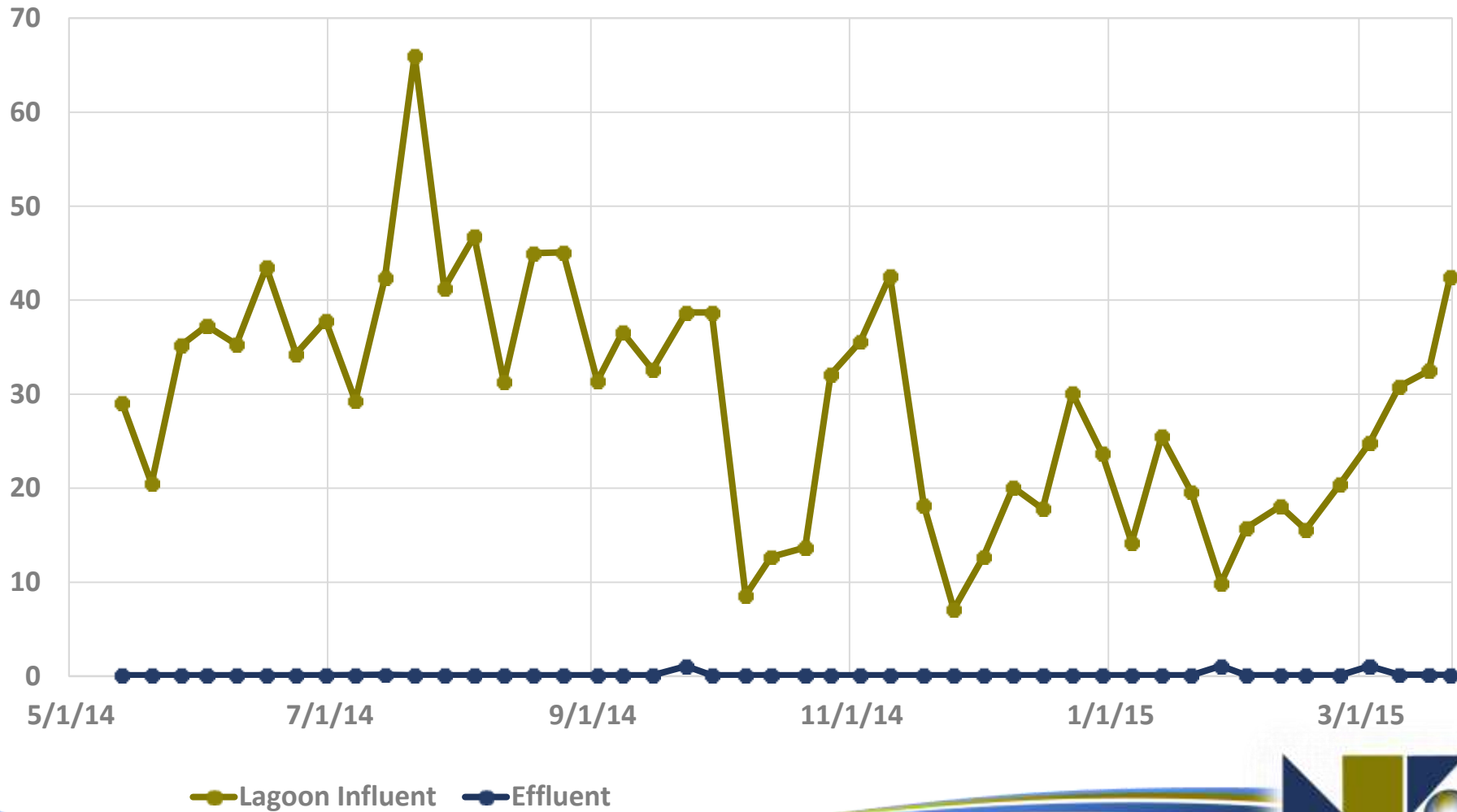


Kennard, Indiana



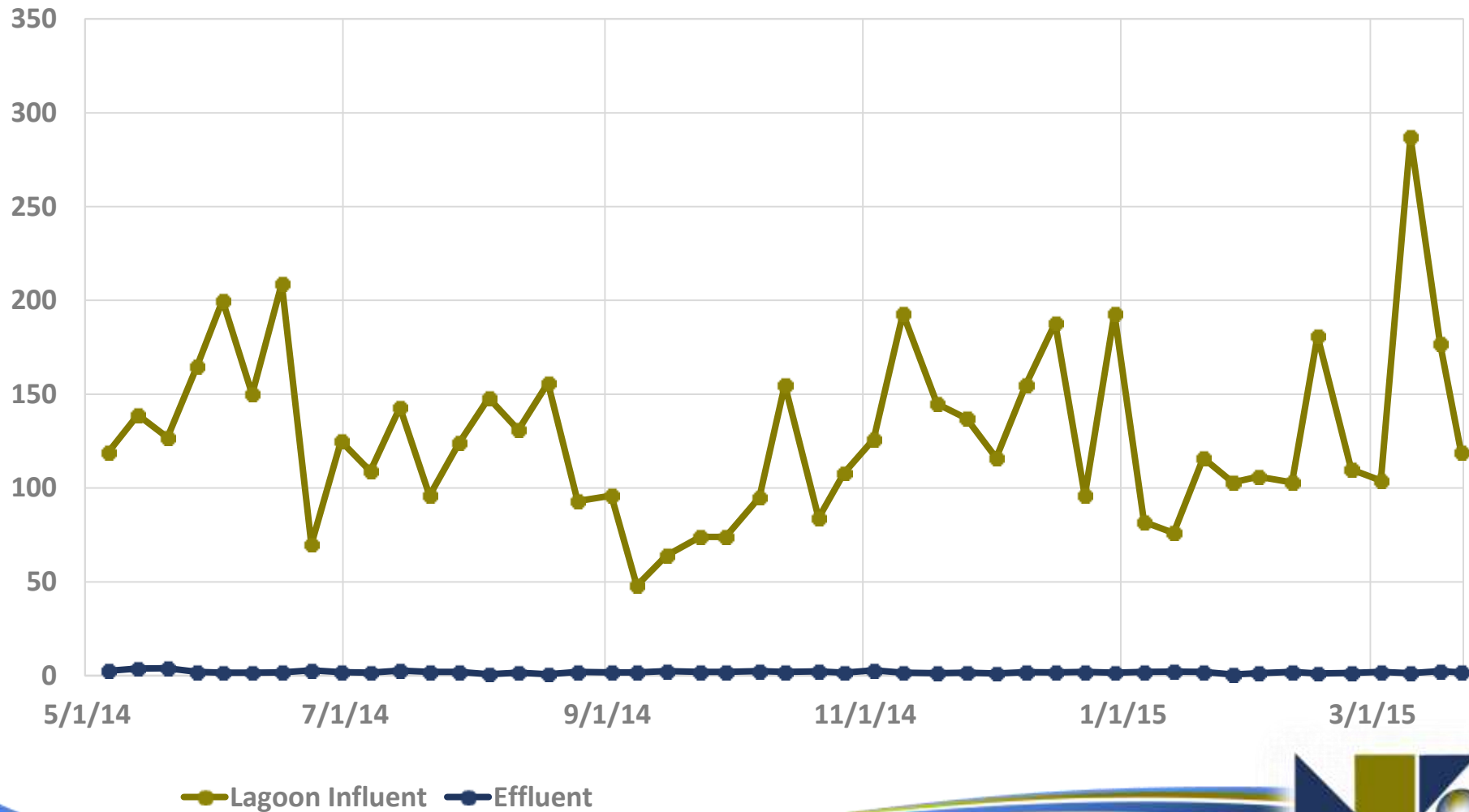
Kennard, Indiana

SAGR TAN (mg/L)



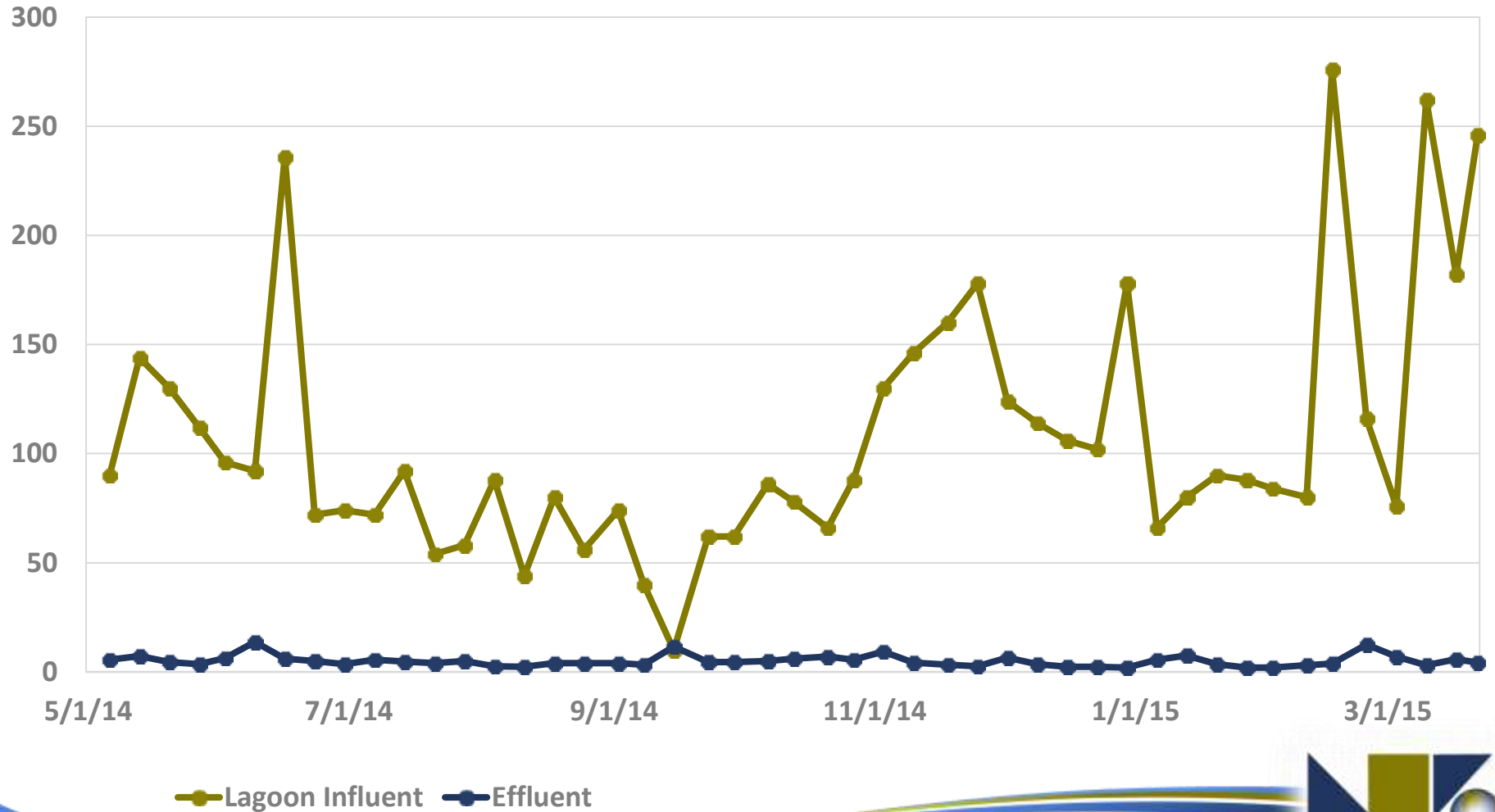
Kennard, Indiana

SAGR BOD (mg/L)



Kennard, Indiana

SAGR TSS (mg/L)



Berne, Indiana

Project Type:

Municipal
Wastewater

Design Flow:

7,257 m³/day
(1.920 MGD)

Effluent

Objective:

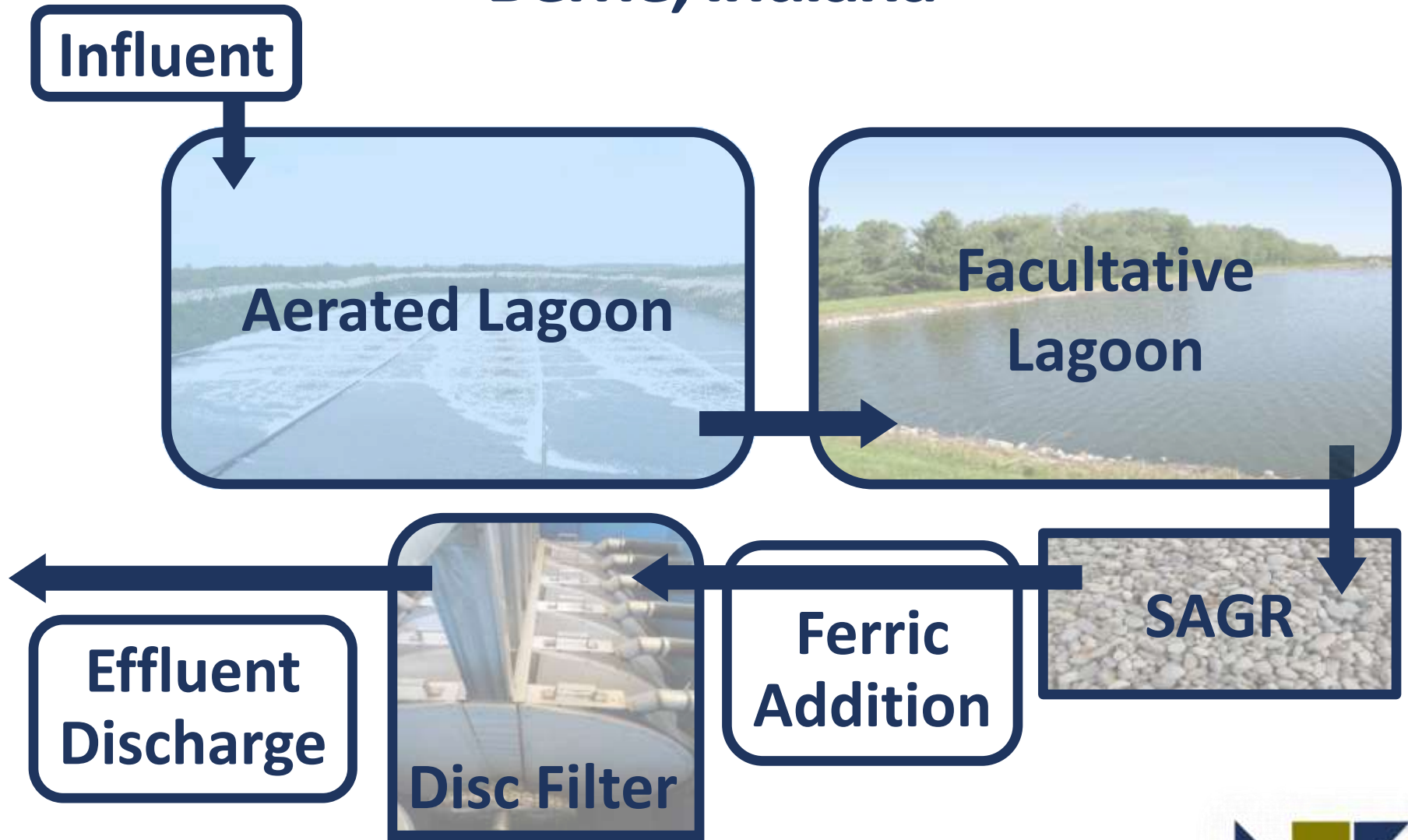
- TAN: <3 mg/L
- BOD: <10 mg/L
- TSS: <30 mg/L
- TP: <1.0 mg/L



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Berne, Indiana





Sundridge, Ontario

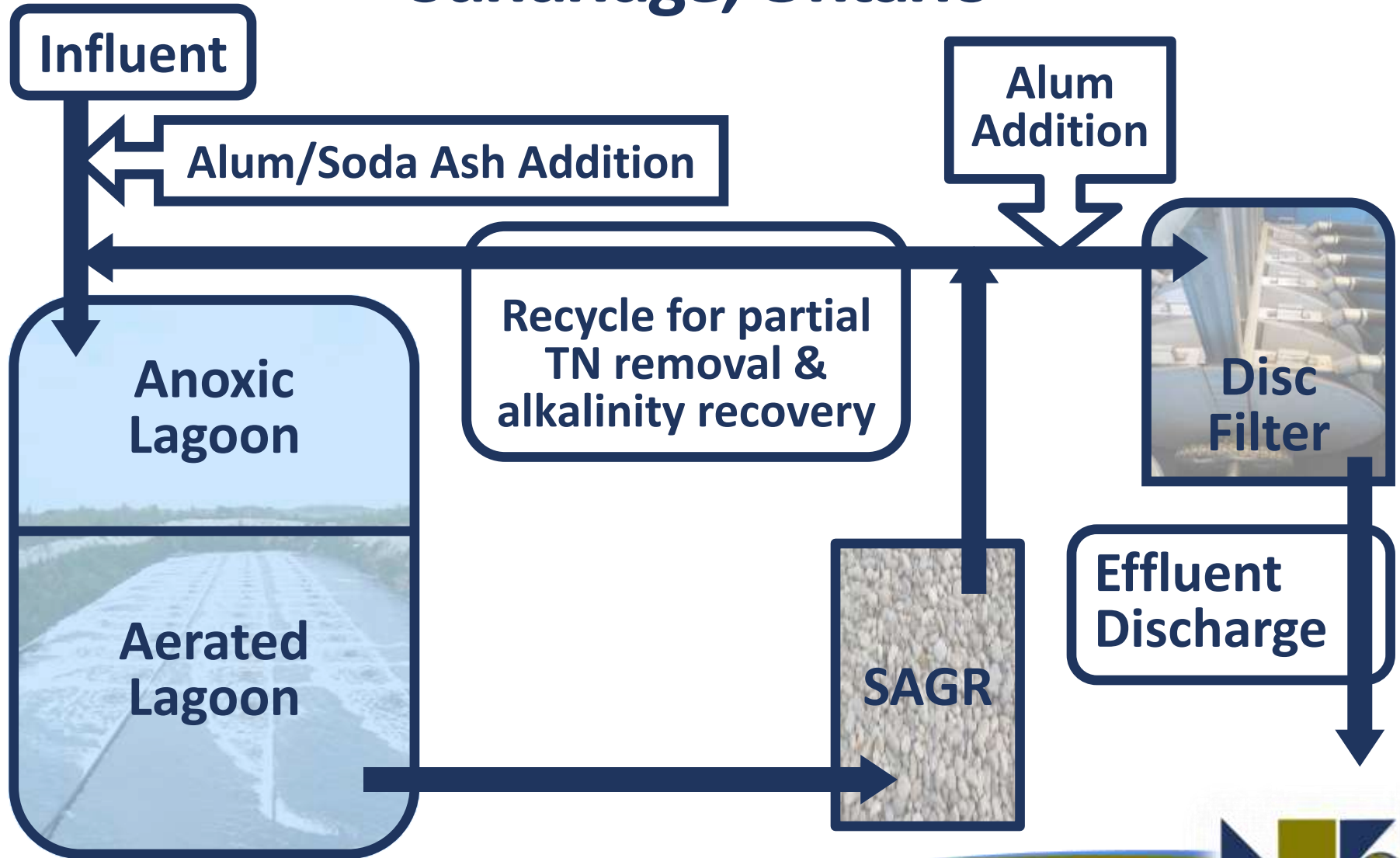
Project Type:
Municipal
Wastewater

Design Flow:
1,192 m³/day
(0.315 MGD)

**Effluent
Objective:**
• TP: <0.27 mg/L

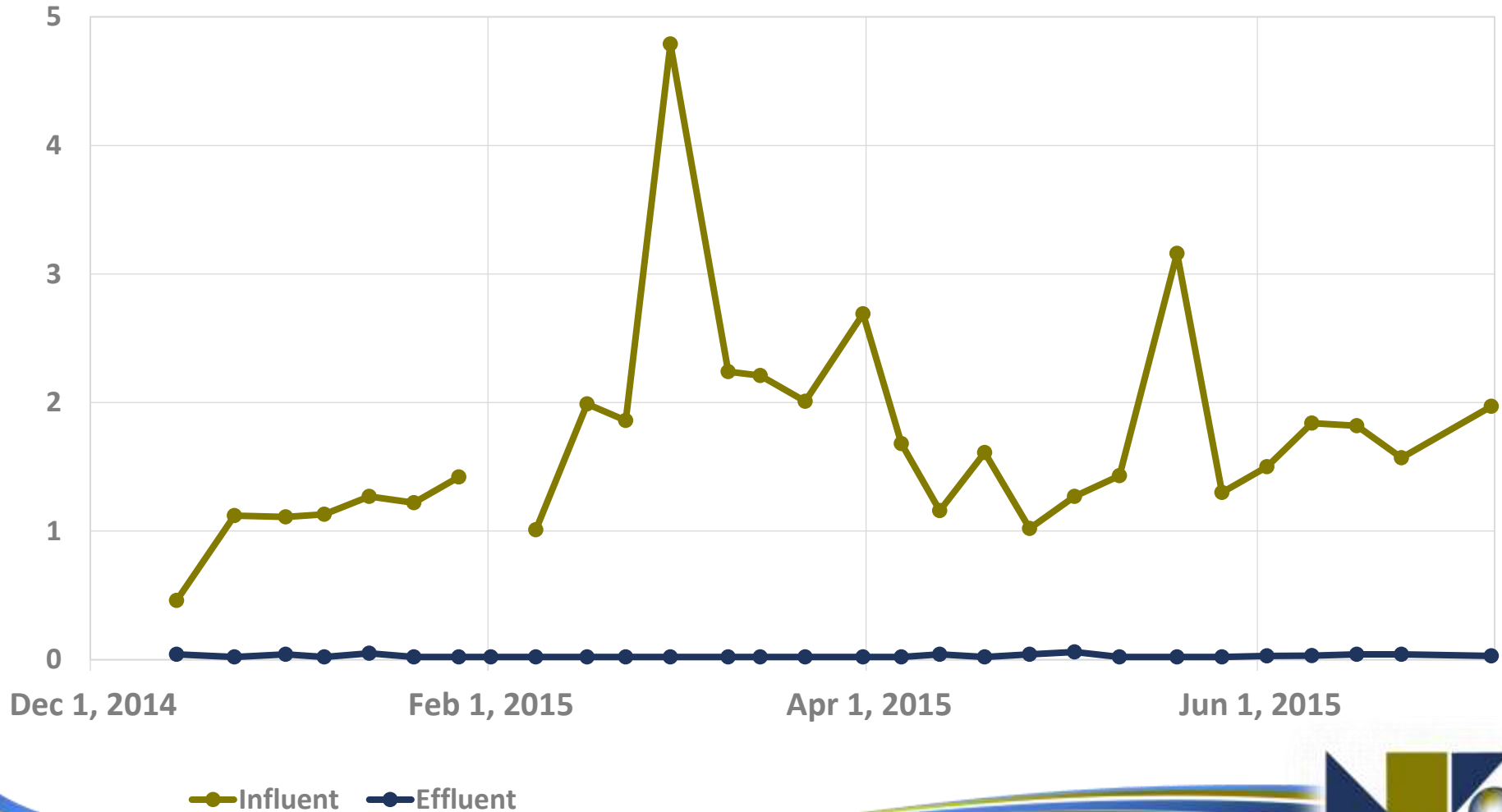


Sundridge, Ontario



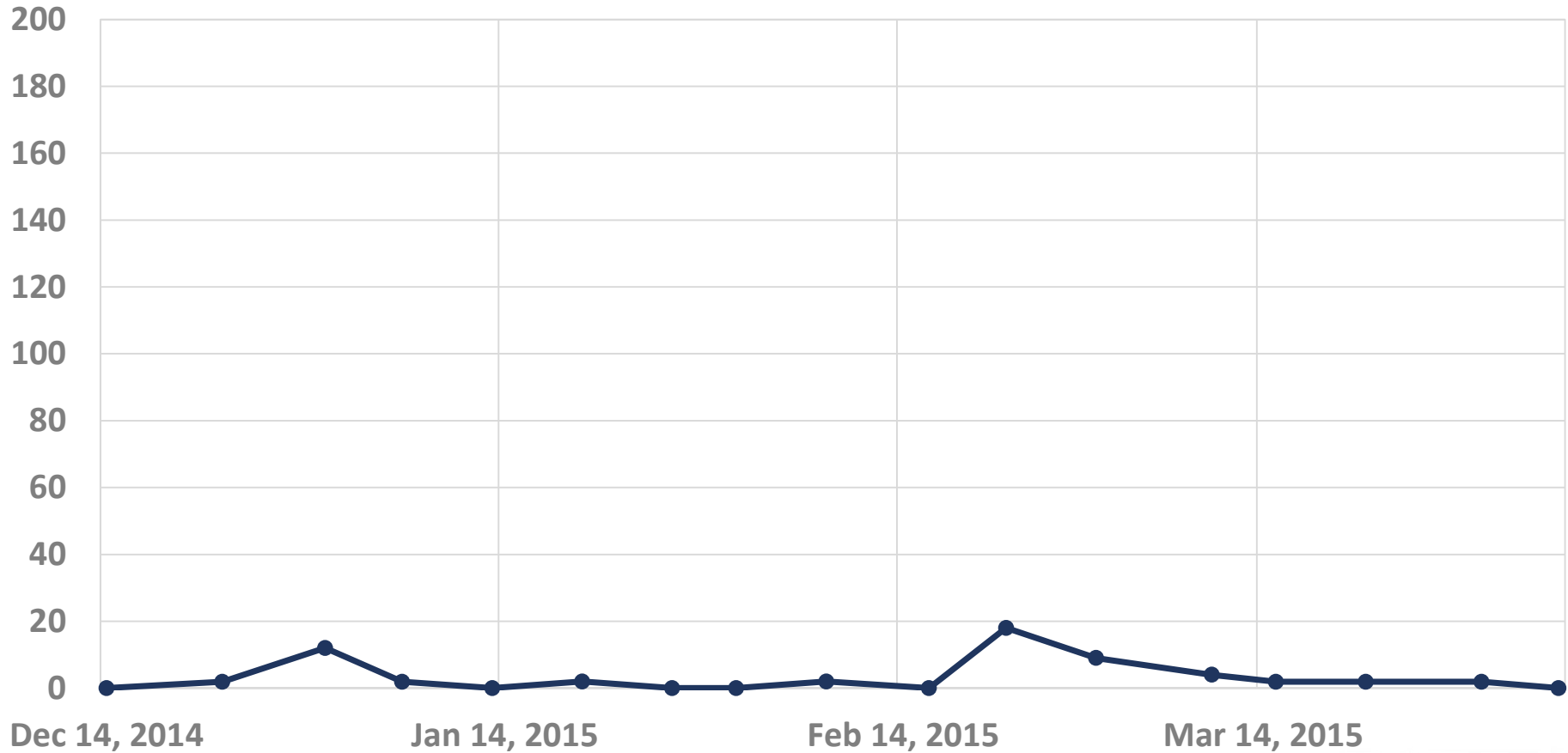
Sundridge, Ontario

opTPhos[®] Total Phosphorus (mg/L)



Sundridge, Ontario

Effluent E.Coli (CFU/100mL)



Glencoe, Ontario

Project Type:

Municipal
Wastewater

Design Flow:

1,742 m³/day
(0.46 MGD)

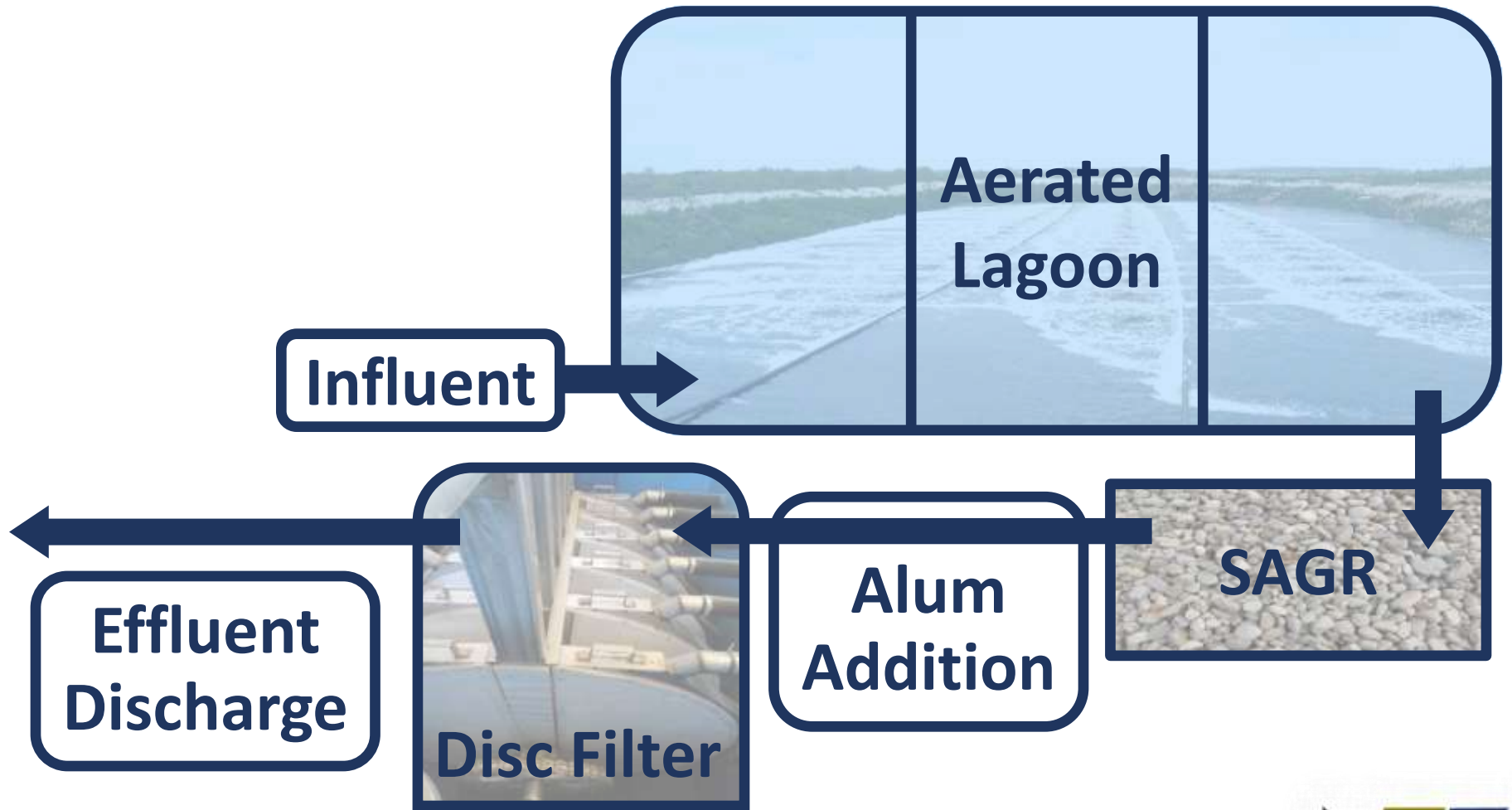
Effluent

Objective:

- TAN: <3.0 mg/L
- BOD: <13.7 mg/L
- TSS: <13.7 mg/L



Glencoe, Ontario

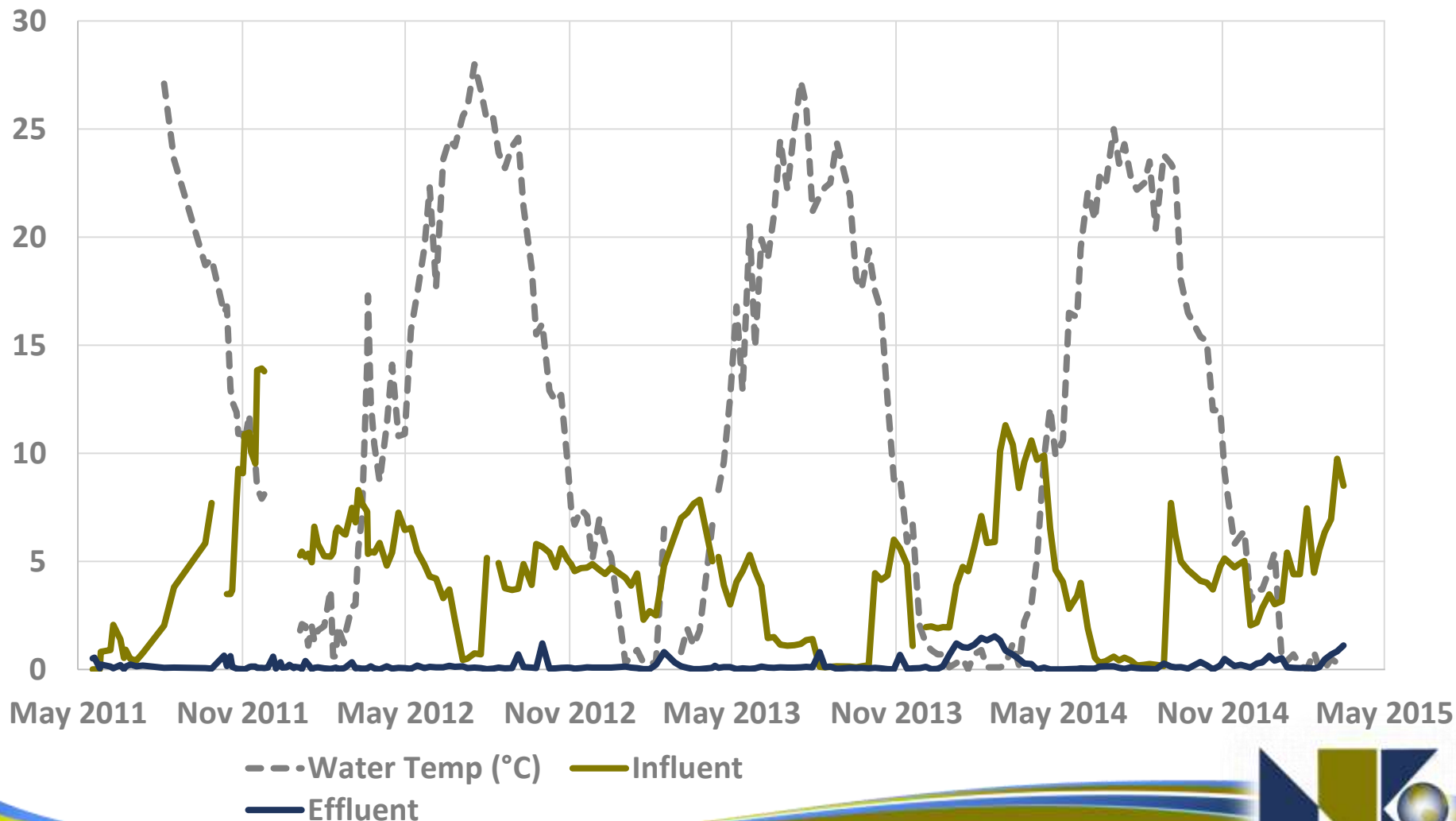


Glencoe, Ontario



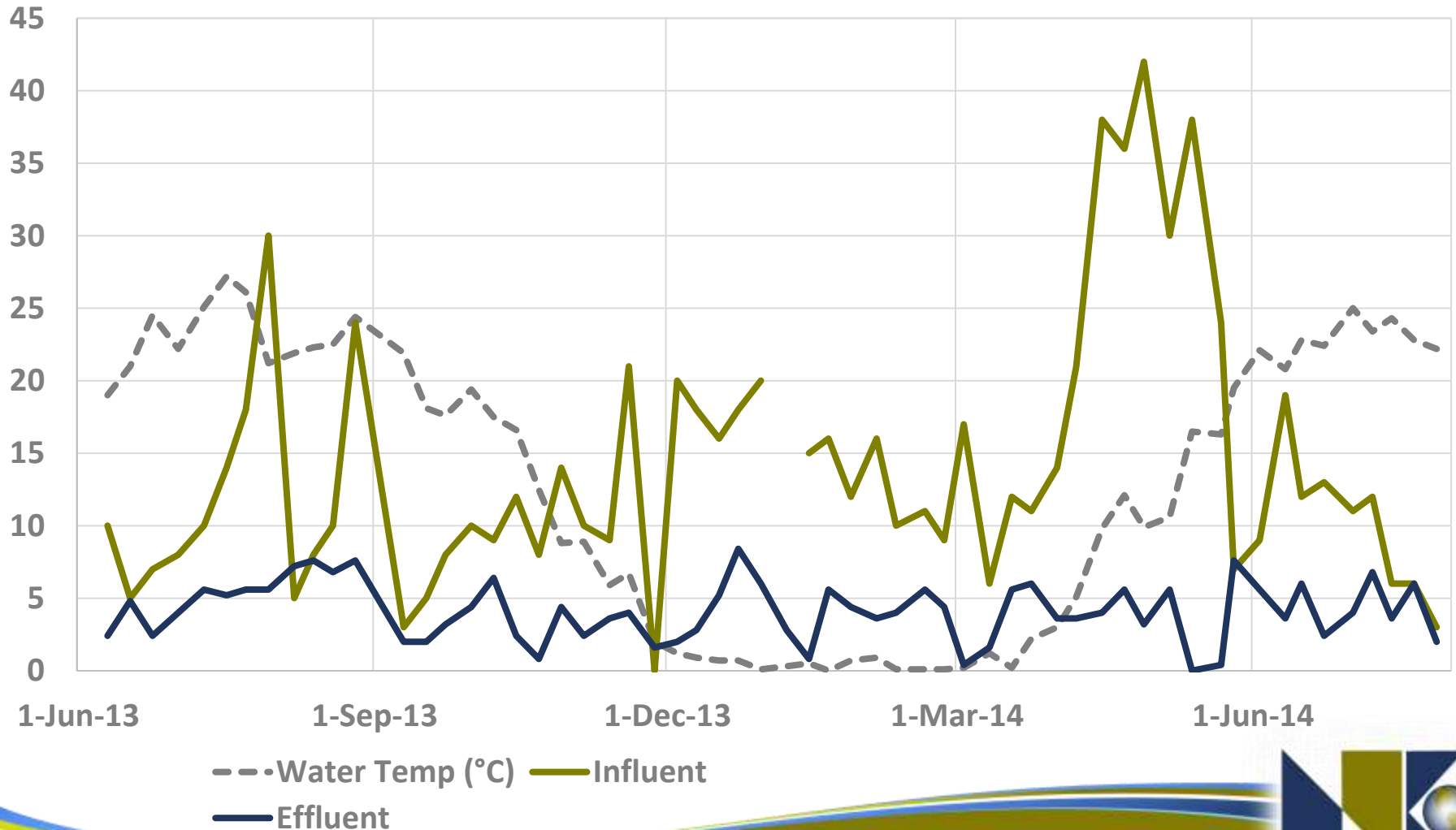
Glencoe, Ontario

SAGR TAN (mg/L)



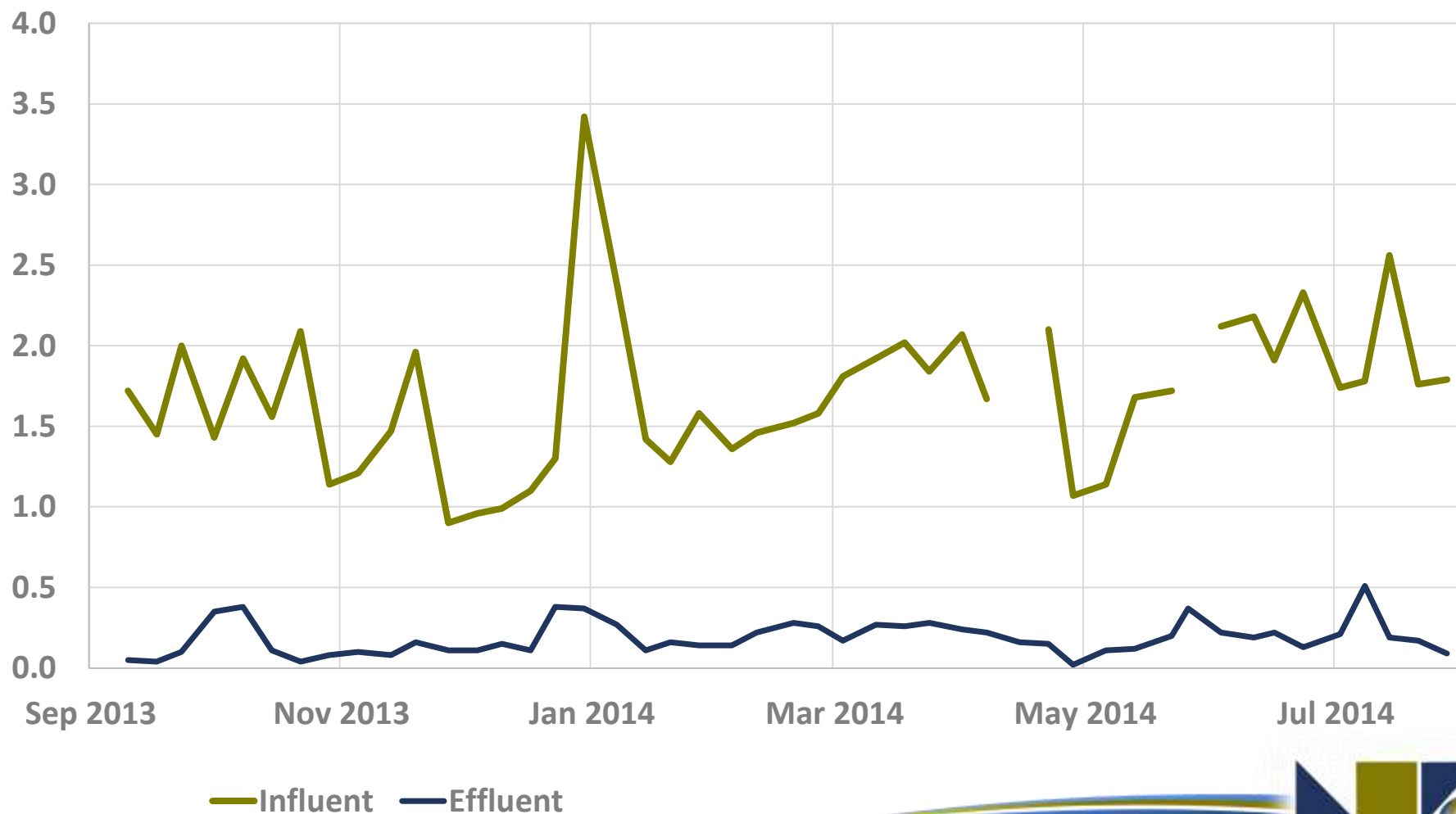
Glencoe, Ontario

SAGR TSS (mg/L)



Glencoe, Ontario

Total Phosphorus (mg/L)





SAGR process provides nitrification to $<1\text{mg/L}$ ammonia at 100% design flow

Consistent BOD/TSS $<5/10\text{ mg/L}$ (lower with tertiary filtration)

Systems can handle significant variation in incoming water quality without upset

Specifically designed for cold water applications

Your lagoons are likely paid for so use them





Questions?

www.nelsonenvironmental.com

