

Biological Nutrient Removal Challenges at Small WWTPs – Ellsworth, WI

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Outline

- ❖ Existing Conditions
- ❖ Project Goals
- ❖ WWTP Upgrades
- ❖ Performance and Optimization
- ❖ Conclusions



Existing Conditions

- ❖ WWTP overview
- ❖ Biological treatment process
- ❖ Other treatment processes
- ❖ Design capacity
- ❖ Effluent quality
- ❖ Reasons for upgrades



WWTP Overview

Existing Conditions





Biological Treatment Process

Existing Conditions

- ❖ RBCs (4)
- ❖ Trickling filter
- ❖ Secondary Clarifiers (2)
- ❖ Waste sludge pumps (3)



Other Treatment Processes

Existing Conditions

- ❖ Mechanical screens (2)
- ❖ Influent pumps (5)
- ❖ Effluent re-aeration
- ❖ Ferric chloride feed system
- ❖ Aerobic digestion



Design Capacity

Existing Conditions

- ❖ Design flow: 0.340 MGD
- ❖ Peak day flow: 0.905 MGD
- ❖ Design BOD₅ load: 834 lb/d
- ❖ Design TSS load: 834 lb/d
- ❖ Capacities based on 2007 re-rating



Effluent Quality

Existing Conditions

- ❖ Average annual data from 2007 – 09
 - ▶ 5 mg/L cBOD₅
 - ▶ 12 mg/L TSS
 - ▶ 15 mg/L NH₃
 - ▶ 0.6 mg/L TP
 - ▶ 387 mg/L chlorides



Reasons for Upgrades

Existing Conditions

- ❖ Existing design was incapable of meeting new permit limits
- ❖ Needed to replace equipment and processes reaching the end of their design life
- ❖ Projected to exceed design flows and loads in near future



Project Goals

- ❖ Meet new permit limits
- ❖ Upgrade existing processes
- ❖ Increase design capacity



Meet New Permit Limits

Project Goals

- ❖ Discharge to Isabelle Creek
 - ▶ Disappearing stream (up to 0.223 MGD loss)
 - ▶ Classifications vary from Lower Aquatic Life to Cold Water Community
 - ▶ Also receives flow from Ellsworth Co-Op Creamery
 - ◆ 0.200 MGD process water
 - ◆ 0.100 MGD non-contact cooling water



Meet New Permit Limits

Project Goals

- ❖ Discharge Option 1 – New Outfall 410th St
 - ▶ Surface water limits:
 - ◆ 1 mg/L TP
 - ◆ Seasonal disinfection to 200 c.f.u.
 - ▶ Potential to create sinkhole downstream
 - ◆ Public disapproval
 - ▶ Future reclassification as Cold Water
 - ◆ Would require tertiary filtration



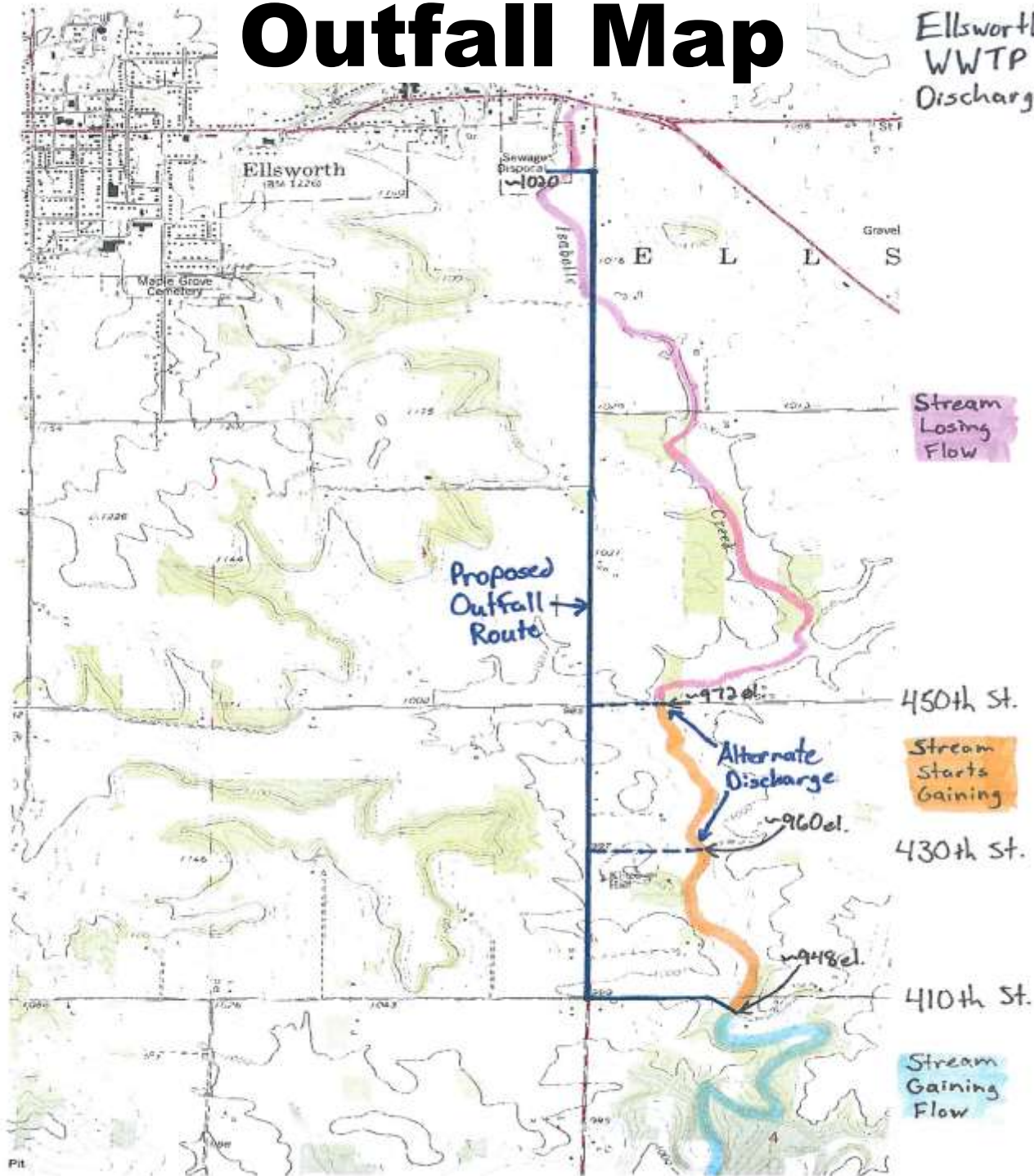
Meet New Permit Limits

Project Goals

- ❖ Discharge Option 2 – Existing Outfall
 - ▶ Surface water limits:
 - ◆ 1 mg/L TP
 - ▶ Creek disappears downstream of outfall
 - ▶ Groundwater limits:
 - ◆ 10 mg/L TN
 - ◆ 325 mg/L chlorides
 - ◆ Year-round disinfection to 400 c.f.u.

Outfall Map

Ellsworth
WWTP
Discharge





Meet New Permit Limits

Project Goals

- ❖ Discharge Option 2 selected
 - ▶ Treat for TN and work on chlorides
 - ▶ No effluent lift station and force main
 - ▶ No tertiary filtration
 - ▶ Lower in total present worth
 - ▶ No potential for sinkhole creation
- ❖ Result: need biological TN and P removal



Meet New Permit Limits

Project Goals

- ❖ Effluent Limits (biological)
 - ▶ 20 mg/L BOD₅ and TSS (monthly avg.)
 - ▶ 10 mg/L TN (monthly avg.)
 - ▶ Seasonal NH₃ limits
 - ◆ Daily max. as low as 7.8 mg/L
 - ◆ Monthly avg. as low as 3.6 mg/L
 - ▶ 1 mg/L TP (monthly avg.)



Meet New Permit Limits

Project Goals

- ❖ Effluent Limits (other)
 - ▶ 4 mg/L DO (daily min.)
 - ▶ 400 c.f.u./100 mL (monthly geo. mean)
 - ▶ 325 mg/L chlorides (weekly avg.)



Meet New Permit Limits

Project Goals

- ❖ Biological processes evaluated:
 - ▶ Activated sludge system
 - ◆ Oxidation ditch
 - ◆ Anaerobic selector
 - ▶ Trickling filter upgrade
 - ◆ Add plastic media
 - ◆ Additional RBCs
 - ▶ RBC expansion
 - ◆ Additional RBCs
 - ▶ IFAS system
 - ◆ Convert sludge tanks
 - ◆ Add media
 - ◆ Add RAS pumping



Meet New Permit Limits

Project Goals

- ❖ Selected activated sludge system
 - ▶ Lowest total present worth
 - ▶ Highly flexible system
 - ◆ Adjust biology (ML concentration)
 - ◆ Vary aeration rate
 - ◆ Add or remove cells from service
 - ▶ Capable of BioP
 - ▶ Capable of total nitrogen removal



Upgrade Existing Processes

Project Goals

- ❖ Processes replaced:
 - ▶ Mechanical screening
 - ▶ Influent pumping
 - ▶ Final clarifiers
 - ▶ Chemical feed
 - ▶ Solids handling



Upgrade Existing Processes

Project Goals

- ❖ New processes:
 - ▶ Biological treatment
 - ◆ RBCs to oxidation ditch
 - ▶ Disinfection
 - ◆ New UV system
 - ▶ Re-aeration
 - ◆ Weir to diffused air



Increase Design Capacity

Project Goals

- ❖ Peak Hour Flow: 2.160 MGD
- ❖ Peak Month BOD₅ Load: 1,019 lb/d
- ❖ Peak Month TSS Load: 1,253 lb/d
- ❖ Peak Month TKN Load: 140 lb/d
- ❖ Peak Month TP Load: 31 lb/d
- ❖ Design Year: 2030



WWTP Upgrades

- ❖ WWTP overview
- ❖ Biological treatment upgrades
- ❖ Biological nutrient removal (BNR) design
- ❖ Other upgrades
- ❖ Bidding and construction



Biological Treatment Upgrades

WWTP Upgrades

- ❖ Type: extended aeration AS with biological nitrogen and phosphorus removal
 - ▶ Three cell anaerobic selector
 - ▶ Two channel oxidation ditch with simultaneous nitrification/denitrification (SND)
 - ▶ Two final clarifiers
 - ▶ RAS pumping system
 - ▶ Internal mixed liquor recycle



Biological Process Parameters

WWTP Upgrades

- ❖ Anaerobic selector volume: 35,000 gal
- ❖ Oxidation ditch volume: 280,000 gal
- ❖ Maximum MLSS: 5,000 mg/L
- ❖ Peak month volumetric BOD₅ loading: 24.2 lb/d
- ❖ Peak month F:M: 0.103
- ❖ Design average SRT: 15 days
- ❖ RAS rate: 50 – 200% design average flow

Biological Treatment Schematic

WWTP Upgrades





Biological Treatment System WWTP Upgrades





Anaerobic Selector Basins

WWTP Upgrades





Oxidation Ditch WWTP Upgrades





Oxidation Ditch WWTP Upgrades





BNR Design

WWTP Upgrades

- ❖ Key biological processes
 - ▶ BOD removal
 - ▶ Nitrification
 - ▶ Denitrification (ML and RAS)
 - ▶ BioP
 - ▶ Settling



BNR Design

WWTP Upgrades

- ❖ Simultaneous Nitrification/Denitrification
 - ▶ $\text{NH}_3 \rightarrow \text{NO}_2 \rightarrow \text{N}_2 \uparrow$
 - ▶ Nitrospirea – Ammonia Oxidizer
 - ▶ Nitrobacter – Nitrite Oxidizer
- ❖ Nitrospirea
 - ▶ Out competes Nitrosomonas in Aerated Anoxic Reactors
 - ▶ Can Go Dormant



BNR Design

WWTP Upgrades

- ❖ Anaerobic selector basins
 - ▶ RAS denitrification
 - ▶ Readily biodegradable chemical oxygen demand (rbCOD) uptake
 - ▶ Soluble phosphorus release
 - ▶ Fermentation (?)



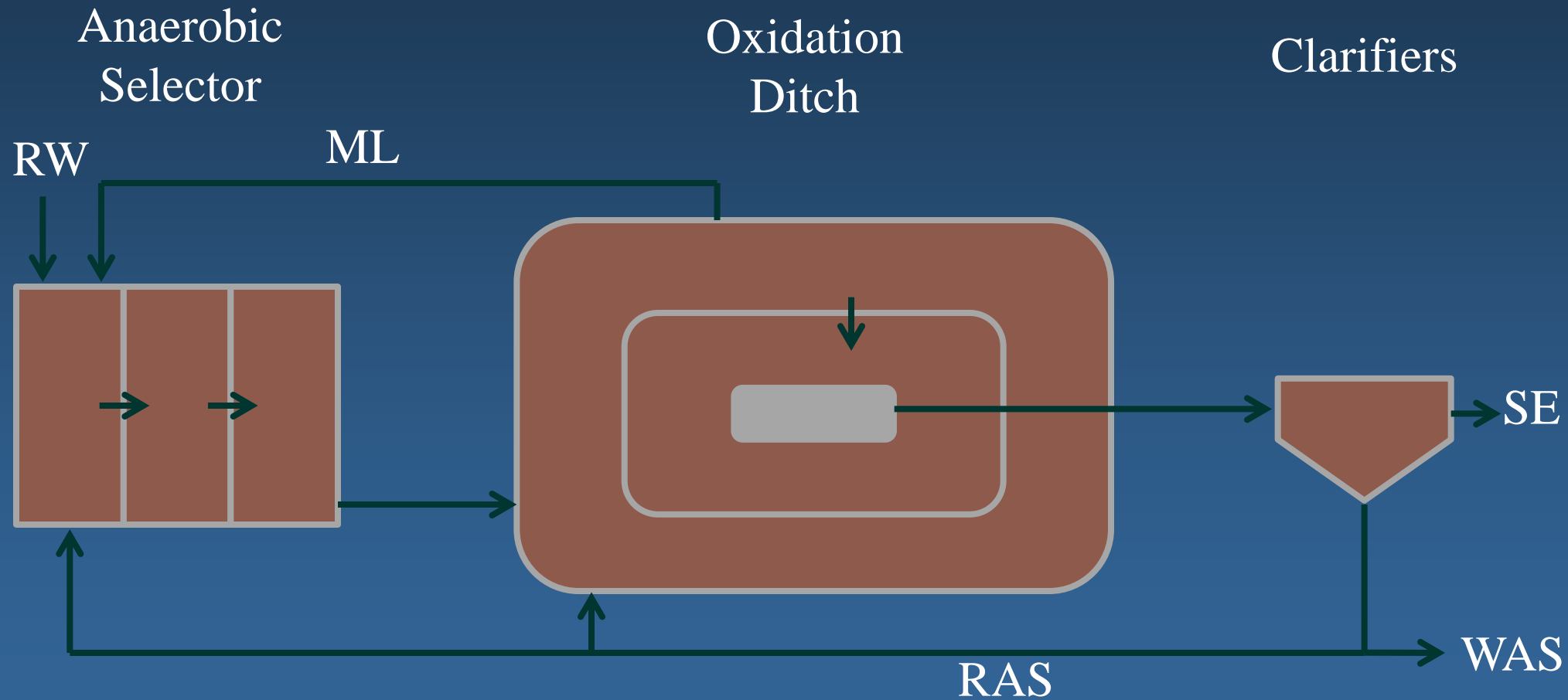
BNR Design

WWTP Upgrades

- ❖ Oxidation ditch (outer channel)
 - ▶ BOD removal
 - ▶ Simultaneous nitrification/denitrification
 - ▶ RAS denitrification
- ❖ Oxidation ditch (inner channel)
 - ▶ BOD removal
 - ▶ Nitrification
 - ▶ Soluble phosphorus uptake

Biological Treatment Schematic

WWTP Upgrades





Design Flexibility

WWTP Upgrades

- ❖ Multiple process basins
- ❖ Multiple RAS addition points
- ❖ Multiple basin functions
 - ▶ RAS denitrification
 - ▶ Detention time
- ❖ Flow and load fluctuations



Other Upgrades

WWTP Upgrades

- ❖ New mechanical fine screen
- ❖ Increased RW pumping capacity
- ❖ Replaced clarifier mechanisms
- ❖ New UV disinfection
- ❖ New diffused air re-aeration
- ❖ New chemical feed system
- ❖ Solids handling system modifications



Bidding and Construction

WWTP Upgrades

- ❖ Bid Price: \$3.34 million
- ❖ Funding: CWF loan and 30% grant
- ❖ General Contractor: Rice Lake Construction Group
- ❖ Mobilization: April 2011
- ❖ Substantial Completion: May 2012



Performance and Optimization

- ❖ Initial performance
- ❖ Operational and process optimization
- ❖ Current performance



Initial Performance

Performance and Optimization

- ❖ Influent (July 2012 – April 2013):
 - ▶ Flow: 0.269 MGD
 - ▶ BOD: 401 lb/day
 - ▶ TSS: 399 lb/day



Initial Performance

Performance and Optimization

- ❖ MLSS: 2,500–4,000 mg/L
- ❖ DO: 2.2 mg/L
- ❖ F:M: 0.067
- ❖ ORP: -150 – -250 mV
- ❖ SRT: 17 days
- ❖ RAS rate: 50%
- ❖ Loading: 10.7 lb/d/kcf
- ❖ Alum rate: 10 gpd



Initial Performance

Performance and Optimization

- ❖ Effluent quality (July 2012 – April 2013):
 - ▶ BOD₅: 21.6 mg/L
 - ▶ TSS: 7.6 mg/L
 - ▶ NH₃: 3.5 mg/L
 - ▶ TN: 12.4 mg/L (some months up to 20 mg/L)
 - ▶ TP: 0.84 mg/L



System Optimization

Performance and Optimization

- ❖ Operational Changes (April – Nov 2013)
 - ▶ Established consistent nitrification (decreased ORP to -100 mV)
 - ▶ Added some WAS to centrate and aerated to promote nitrification
 - ▶ Attempted to increase denitrification by raising RAS rate
- ❖ Reduced TN to consistently 9 – 12 mg/L



Nitrate Recycle

Performance and Optimization

- ❖ Nitrate recycle port installed
 - ▶ Opening cut in ditch wall between channels
 - ▶ Installed November 2013
 - ▶ Starting December 2013, $\text{NO}_3 + \text{NO}_2$ improved
 - ▶ Winter of 2013-14 cold, NH_3 increased
 - ▶ Nitrification rebounded in May and system began meeting TN limit



Nitrate Recycle

Performance and Optimization



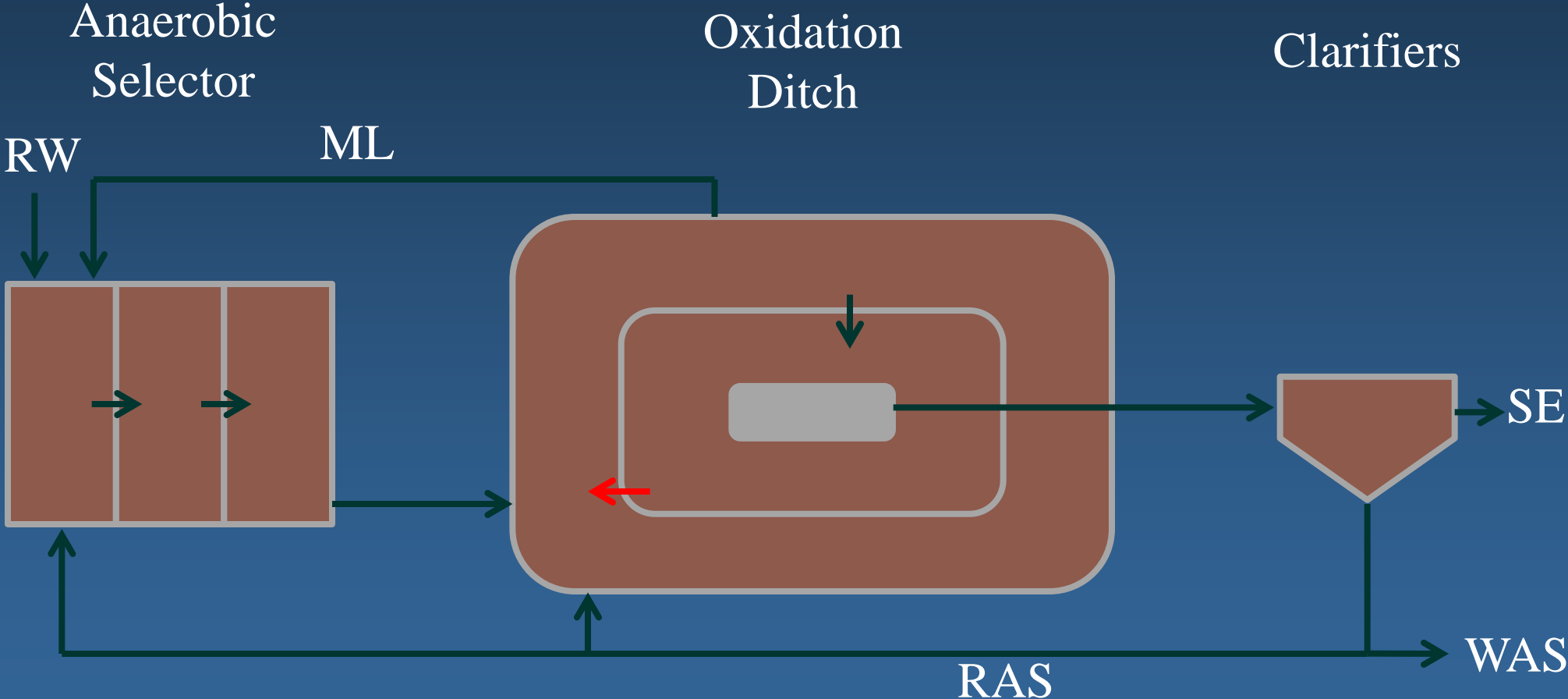


Nitrate Recycle

Performance and Optimization



Nitrate Recycle WWTP Upgrades





Current Performance

Performance and Optimization

- ❖ Influent (May 2014 – July 2015):
 - ▶ Flow: 0.347 MGD
 - ▶ BOD: 381 lb/day
 - ▶ TSS: 464 lb/day



Current Performance

Performance and Optimization

- ❖ MLSS: 2,500–5,500 mg/L
- ❖ DO: 3.0 mg/L
- ❖ F:M: 0.052
- ❖ ORP: -100 mV
- ❖ SRT: 18 days
- ❖ RAS rate: 50%
- ❖ Loading: 10.1 lb/d/kcf
- ❖ Alum rate: 10 gpd



Current Performance

Performance and Optimization

- ❖ Effluent quality (May 2014 – July 2015):
 - ▶ BOD₅: 7.3 mg/L
 - ▶ TSS: 3.9 mg/L
 - ▶ NH₃: 0.4 mg/L
 - ▶ TN: 4.5 mg/L
 - ▶ TP: 0.43 mg/L



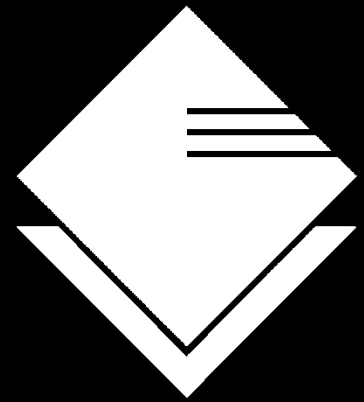
Current Performance Performance and Optimization





Conclusions

- ❖ Biological process start-up is not automatic
- ❖ Flexibility in design benefits future operation
- ❖ Effective TN and BioP is possible at small WWTPs



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