



CH2MHILL®

2010 CONFERENCE TECHNICAL PROGRAM

Estimating and Controlling Hydrogen Sulfide in Municipal Interceptors from a High Strength, High Temperature Industrial Wastewater

Presenters

Bill Oldenburg – GBMSD

John Siczka – CH2M HILL



Agenda

- Background Bill Oldenburg

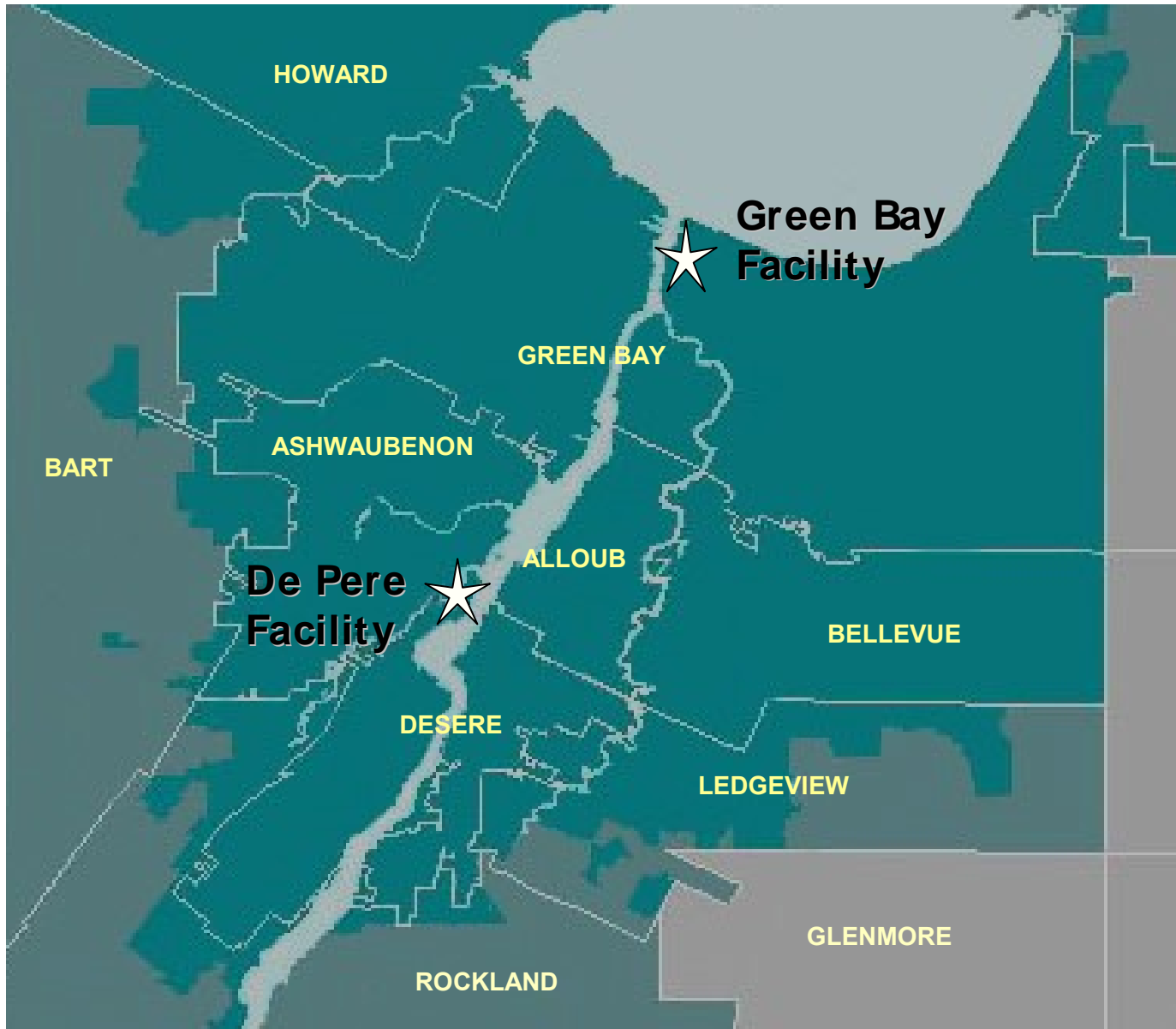
- 2009 Sulfide Study John Siczka
 - *Sulfide Generation*
 - *Modeling*
 - *Interim H₂S Limits*
 - *Interim Chemical Treatment*
 - *Permanent Solution*



- Two treatment facilities: Green Bay & De Pere
- GB Facility: 26 mgd (22.5 municipal + 4.5 mill)
- De Pere Facility: 8.4 mgd
- Annexed area = 277 square miles
- Service area = 131 square miles
- Gravity sewers: 77.2 miles
- Force mains: 24.6 miles
- 12 lift stations / 1 pumping station
- 17 municipal and one contract service customer

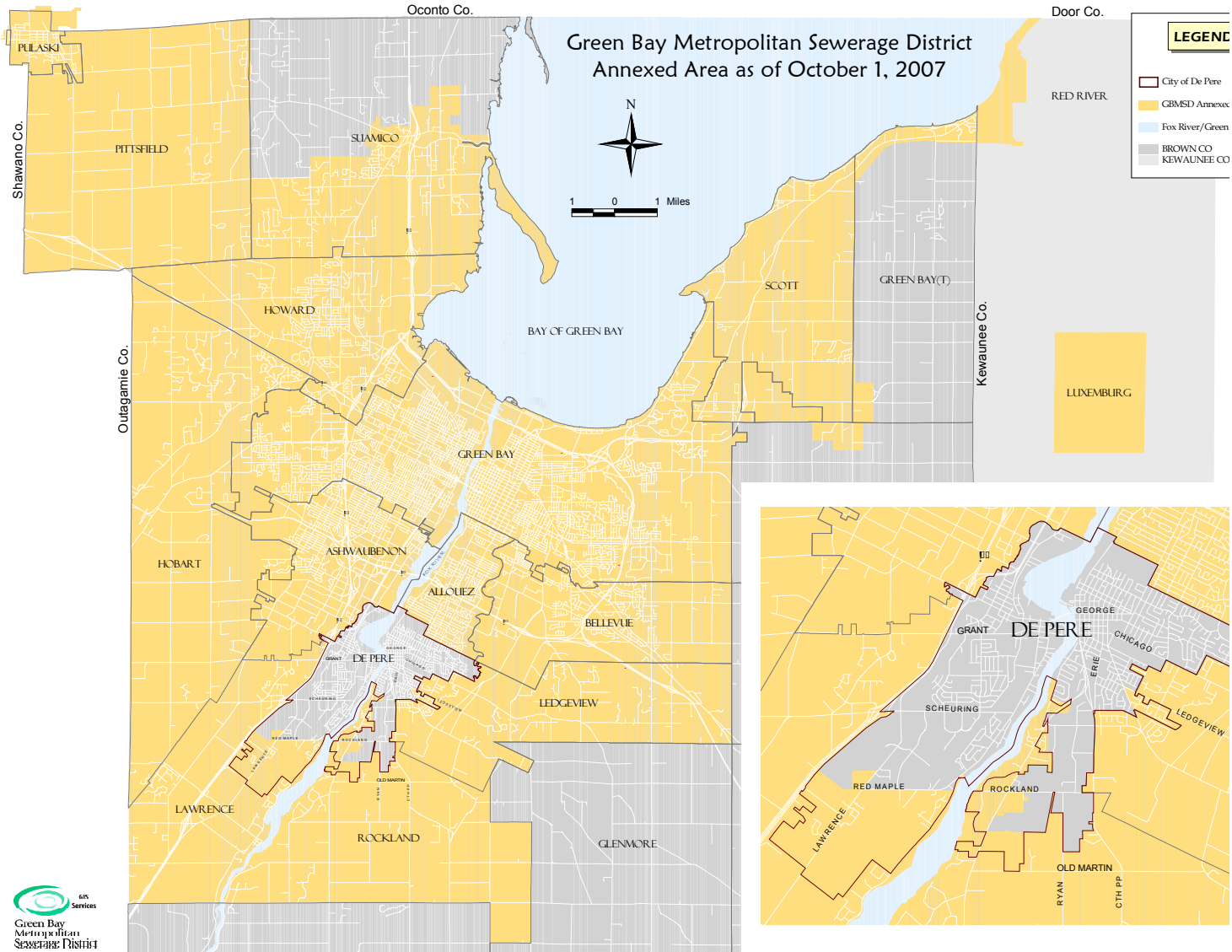


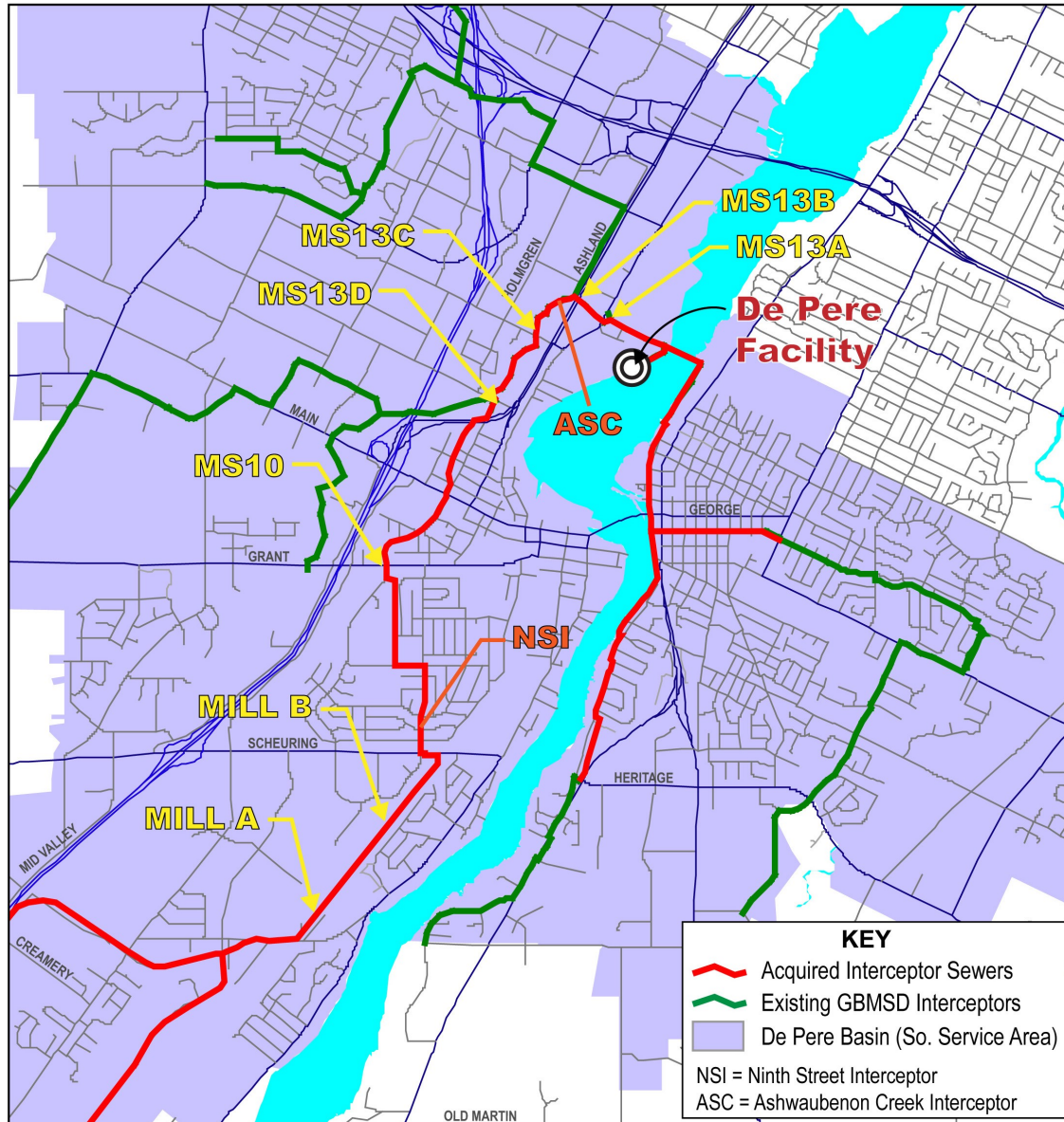
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Prior to 1/1/2008

- Sewer Service Areas
- Four historical H₂S studies
- Connected interceptors with separate ownership
- Two separate sewer use ordinances
- Request for annexation and acquisition
- Due diligence work
- Ninth Street Interceptor /Ashwaubenon Creek Interceptor (NSI/ASC)



Impacts of Hydrogen Sulfide Release

- Corrosion of sewers and treatment plant facilities
- Health and safety
 - *Workers*
 - *Public – migration through dry traps, etc.*
- Nuisance odors
 - *Collection system*
 - *Wastewater treatment plants*



Mill Wastewater Characteristics Discharging to NSI/ASC

| Mill | Average Flow (gpd) | Average BOD (mg/L) | Average Temperature (°F) |
|--------|--------------------|--------------------|--------------------------|
| Mill A | 244,300 | 1,959 | 89.8 |
| Mill B | 767,000 | 2,259 | 104.4 |

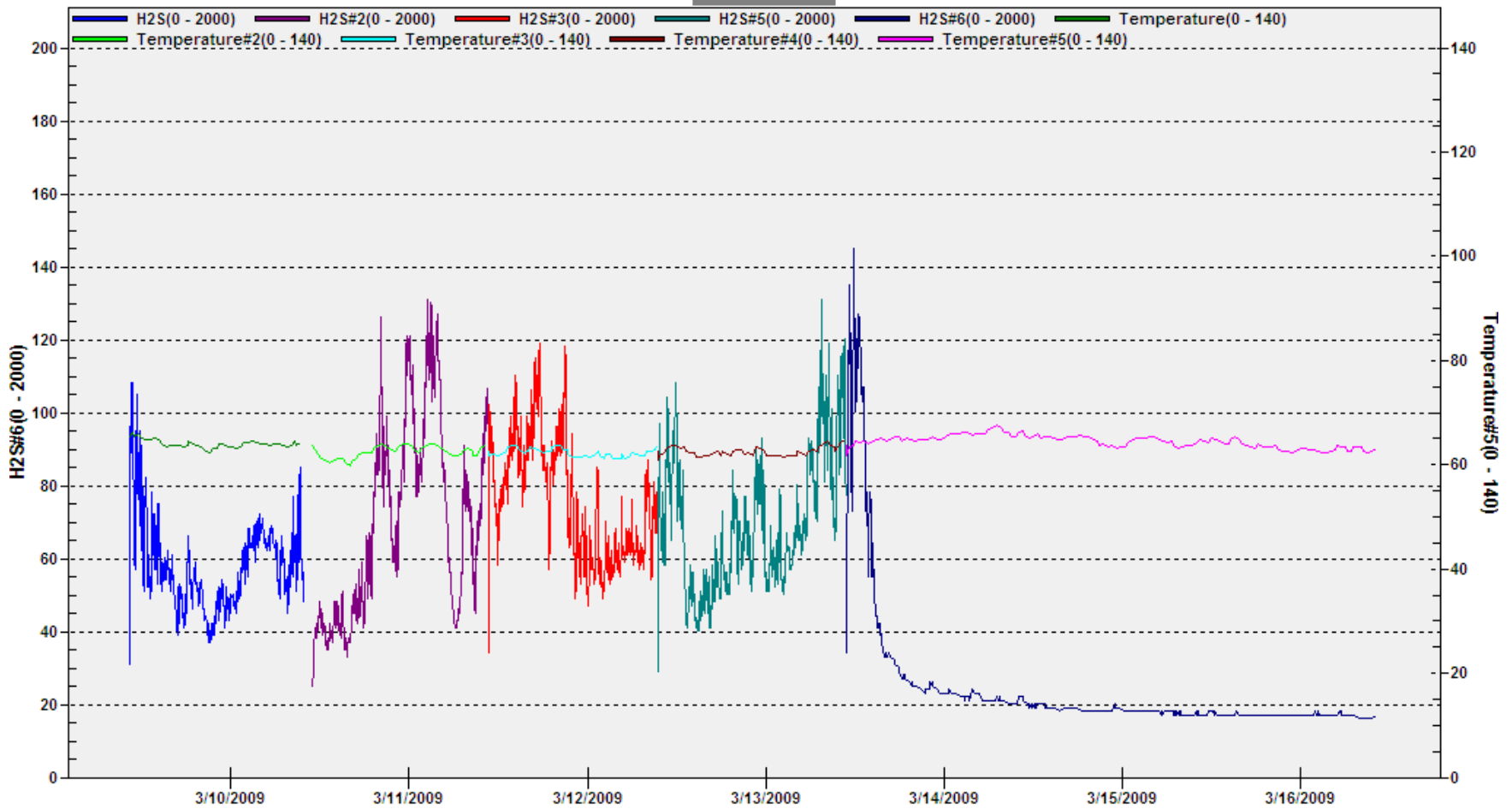


NSI/ASC – MH ASC-013: Vapor Phase H₂S

ASC-013 3-9-09 TO 3-16-09

Modified Session: Session 0

[H2S#4(0 - 1000)]



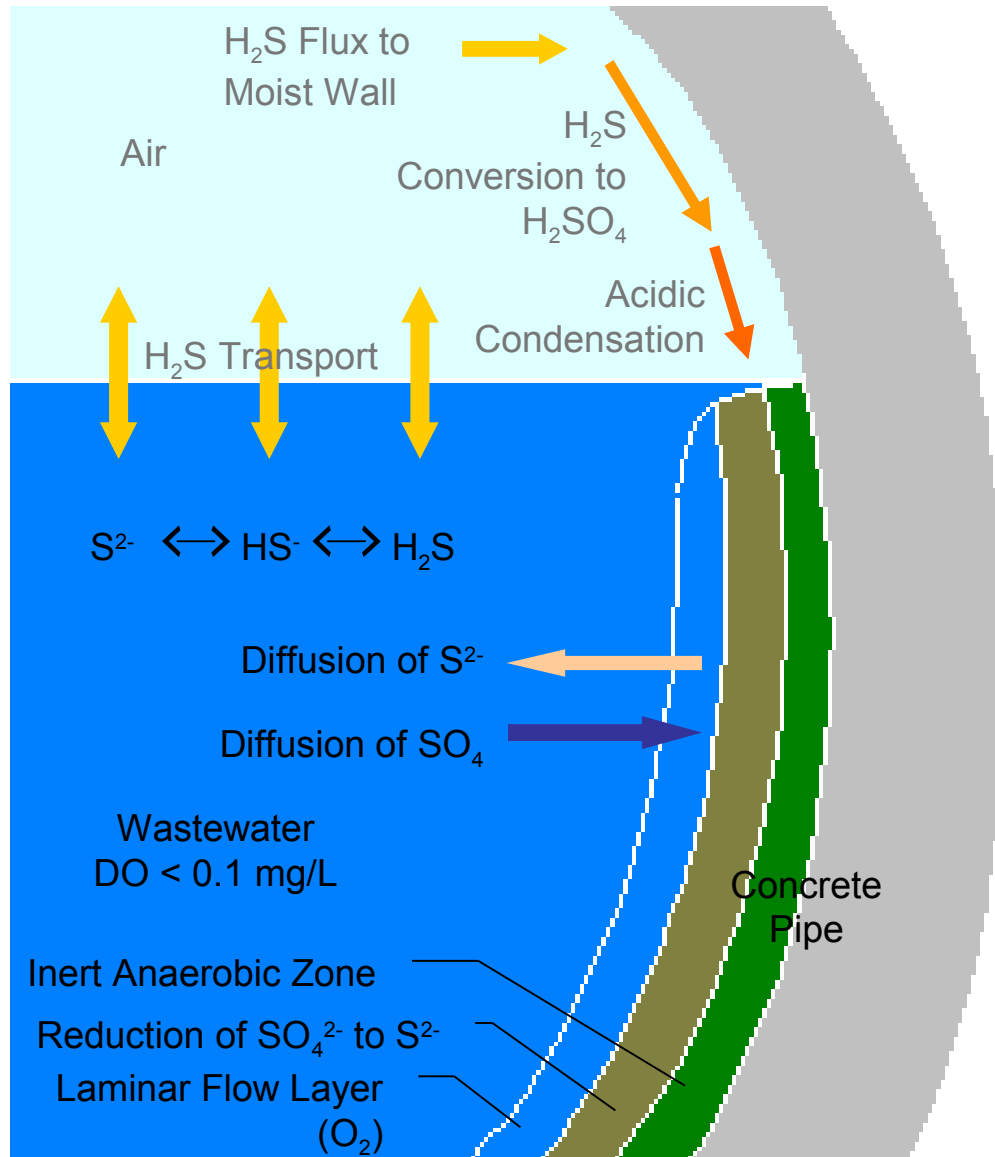




Generation of Sulfides

- Sulfate (SO_4^{2-}) + Anaerobic Bacteria → Sulfides
- Sources of sulfates
 - *Potable water*
 - *Ground water infiltration into sewers*
 - *Sulfates from industrial, commercial and domestic source*
- Sulfide generation almost always not limited by amount of sulfates in wastewater

Sulfide Generation in Sewer Pipes





Generation of Sulfides

- Sewer slime mechanisms
 - *Sulfates converted to sulfides in aerobic zone*
 - *Oxygen in aerobic zone oxidizes these sulfides*
 - *When oxygen insufficient ($<0.1 - 1$ mg/L), sulfides diffuse into wastewater*
 - *Several factors influence depth of aerobic zone and oxygen concentration*



Parameters that Effect Sulfide Generation

- Higher velocity = less sulfide generation
 - *Oxygen consuming solids don't settle*
 - *Slime layer/anaerobic zone is thinner*
 - *More oxygen transfer from wastewater to aerobic zone*
 - *More sewer slope = higher velocity*
 - *However, higher sewer slope increases turbulence and stripping of sulfides to sewer vapor headspace*



Parameters that Effect Sulfide Generation

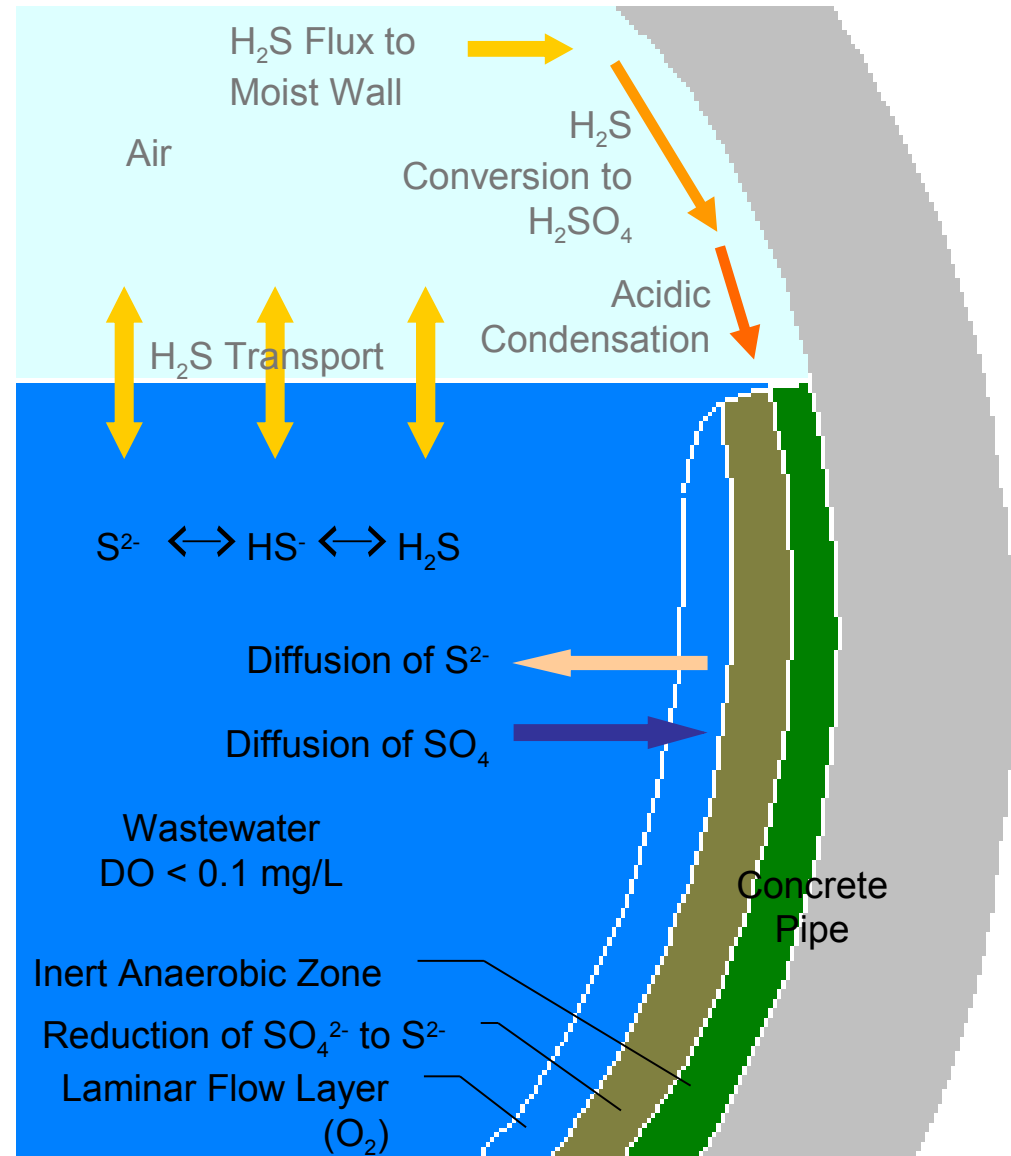
- Higher BOD = more sulfide generation
 - *Higher oxygen demand, reduces wastewater dissolved oxygen and the ability of aerobic bacteria to oxidize sulfides produce in the anaerobic slime layer zone*
 - *More BOD provides more food for anaerobic bacteria*



Parameters that Effect Sulfide Generation

- Higher temperature = more sulfide generation
 - *Increases kinetics and speed of reactions*
- Higher detention time / low flows = more sulfide generation
 - *More time for reactions to occur (e.g. conversion of sulfates to sulfides)*

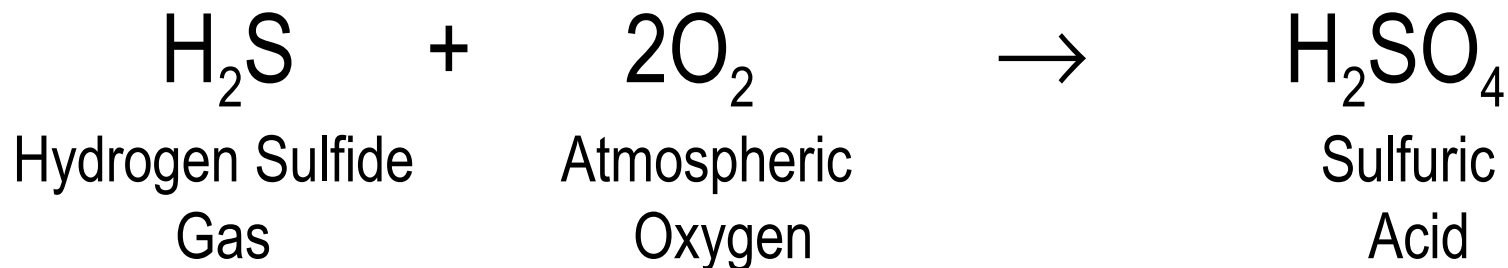
- Release of H_2S depends on:
 - *Turbulence – drops, high velocity, slope changes*
 - *Ventilation rate*
 - *pH – more H_2S present at lower pH*



Corrosion

- Corrosion rate dependent on:
 - *Alkalinity*
 - *Surface pH*
 - *Wall thickness*
 - *Concrete mix*

Thiobacillus
Bacteria





INTERCEPTOR Model

- Predicts both liquid and vapor phase hydrogen sulfide concentrations
- Previous models (Pomeroy and Parkhurst) only predicted liquid phase
- Vapor phase concentrations determine odor and corrosion impacts
- Applicable to both gravity lines and force mains



INTERCEPTOR Model – Used to Determine Methods for Reducing Odors

- Impacts on changes in wastewater BOD, flows, temperatures
- Determine chemical dosages and optimum addition points
- Use vapor phase concentrations and air flow rates to size vapor phase treatment (carbon, scrubbers, etc.)
- Determine which manholes may require sealing or other odor control

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Interceptor Model

1 Choose Compound
 HYDROGEN SULFIDE

2 Input Data
 Input Reach Data
 Input Side Sewer Data

3 View Results/Output
 Tables, Graphs, & Pictograms
 Results

4 Review Input & Calculations
 Input Sheet - Side
 Input Sheet - Main
 Main Hydraulic, Main VOC
 SS VOC, SS Hydraulic

5 Model Setup & Defaults:
 Oxygen Data, Validation Data, VOC Data

Study Details
 Project Name: Interceptor Pre-Release Beta
 Scenario Name: Model Validation
 Staff Name: DTR Consulting
 Date: 12/9/98

Status
 Ready

Data Management
 Load, Save
 C:\DTR Consulting\Interceptor Model\test.

Printer Setup, User Level, Help, Close Model

3 main reaches (indicated by a blue arrow pointing to a globe icon)

0 side sewers (indicated by a green arrow pointing to the globe icon)

Ready

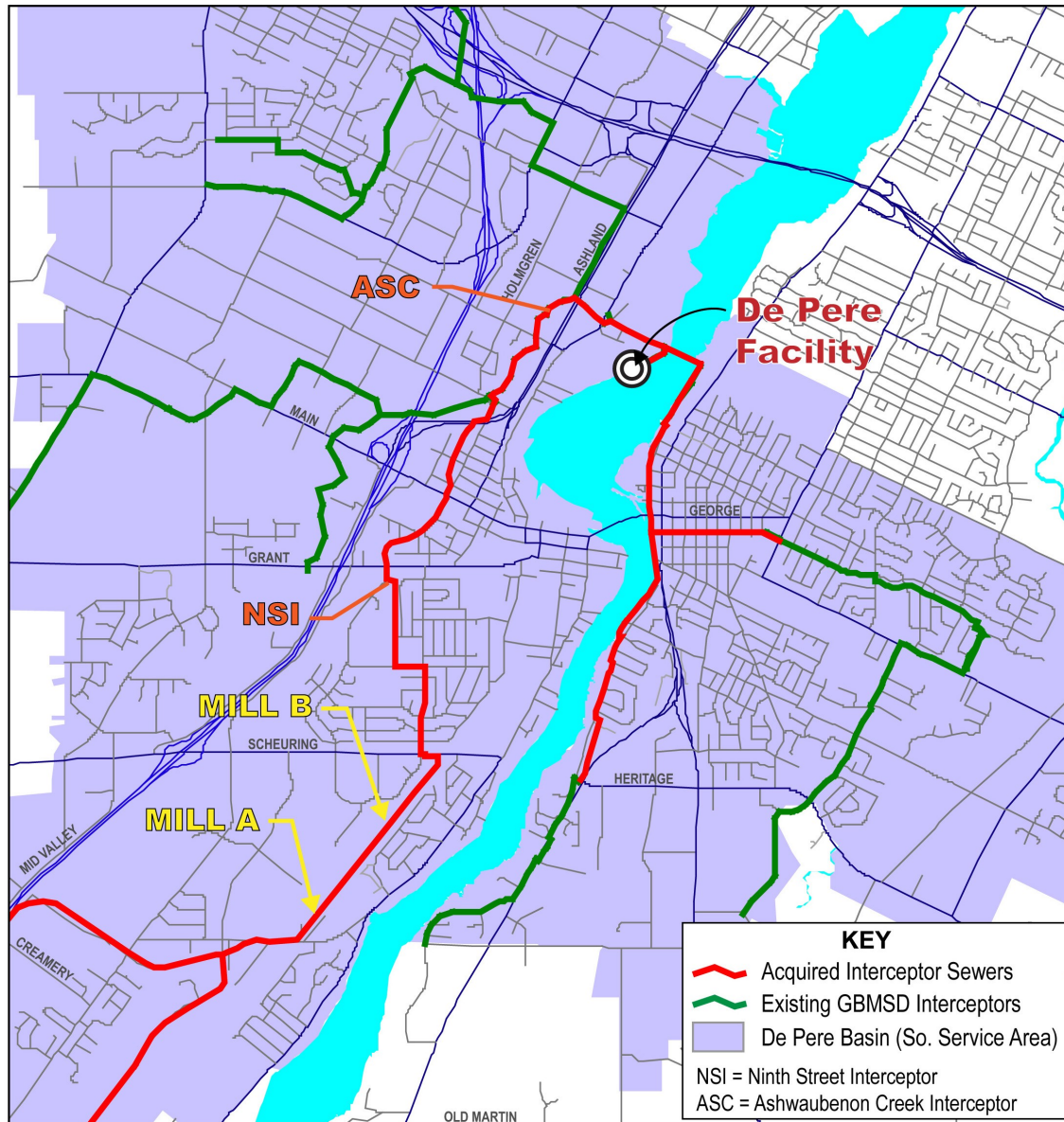
INTERCEPTOR Model Runs

- Calibrated with extensive vapor phase data
- Numerous scenarios run
 - *Different loading conditions*
 - *Different mill discharge temperatures*
 - *Only one mill operating*
 - *No mills operating*
- Models and data assisted in confirming mills were the source of high vapor phase H₂S

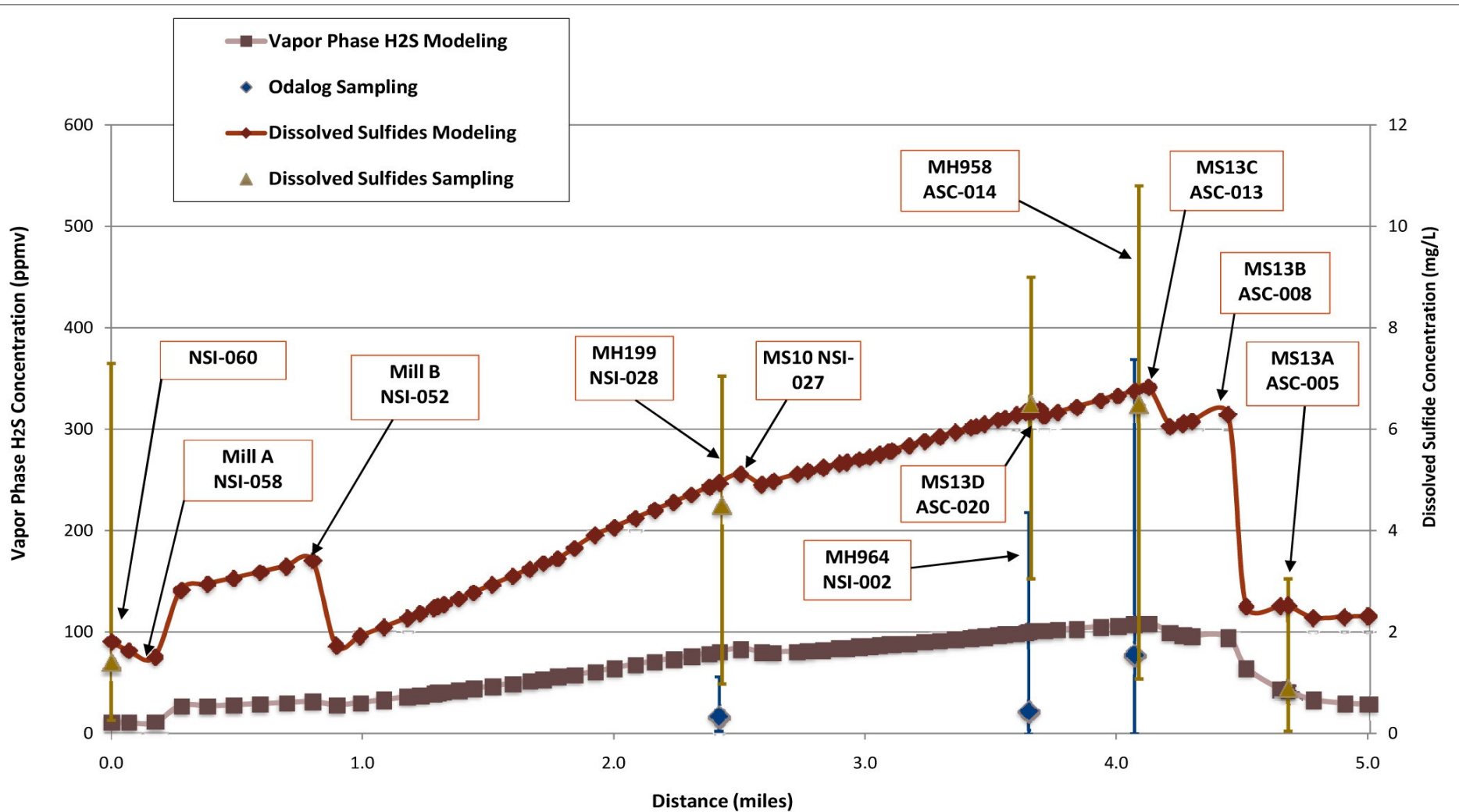


NSI/ASC INTERCEPTOR Model Selected Inputs

| Location | Flow (gpd) | BOD (mg/L) | Temperature (°F) | Dissolved Oxygen (mg/L) | Dissolved Sulfide (mg/L) |
|-------------------|------------|------------|------------------|-------------------------|--------------------------|
| Upstream of Mills | 175,600 | 200 | 57 | 2 | 1.8 |
| Mill A | 244,300 | 1,959 | 96 | 0.5 | 1.8 |
| Mill B | 767,000 | 2,259 | 109 | 0.5 | 0.5 |
| MS10 | 130,000 | 188 | 55 | 2 | 2 |
| MS13D | 70,000 | 1,364 | 60 | 0.5 | 3 |
| MS13C | 200,000 | 261 | 59 | 1 | 0 |
| MS13B | 2,450,000 | 211 | 57 | 1 | 0 |
| MS13A | 450,000 | 290 | 64 | 1 | 0 |



NSI/ASC Average Loading Condition: Modeling Predicted Sulfide Concentrations and Sampling Data





Interim Vapor Phase H₂S Limits

- Immediate addition of treatment chemicals
- GBMSD long term standards
 - *24 hour running average: 2 ppmv*
 - *Instantaneous Peak: 10 ppmv*
- Interim limits: protect public health and safety
 - *Dry traps*
 - *Worker safety*

Interim Vapor Phase H₂S Limits

- OSHA, ACGIH, and NIOSH limits consulted
- GBMSD interim standards
 - *24 hour running average: 20 ppmv*
 - *Instantaneous peak: 40 ppmv*
- Existing NIOSH standards and other proposed standards for worker exposure are lower
 - *Dilution by air prior to receptor*
 - *20 – 40 ppmv not usual (hazard to public)*
 - *40 ppmv below the IDLH concentration of 100 ppm and the OSHA 50 ppm short term PEL*



Interim Chemical Treatment

- Mills responsible for selecting and dosing chemicals with GBMSD and CH2M HILL guidance
- INTERCEPTOR model used to determine initial, conservative dosages
 - *Actual dosages slightly higher due to highly variable mill discharge*
- OdaLog[®] data reviewed on a weekly basis
 - *Assess effectiveness*
 - *Adjust chemical dosing*



Interim Chemical Treatment

- Mill criteria: effective treatment at acceptable cost
- Mill A
 - *Not operating for an extended period of time*
 - *BIOXIDE® dosed when operating*
- Mill B
 - *Ferric chloride*
 - *Peroxide/calcium nitrate/catalyst blend*
 - *Ozone/oxygen*
 - *BIOXIDE®*

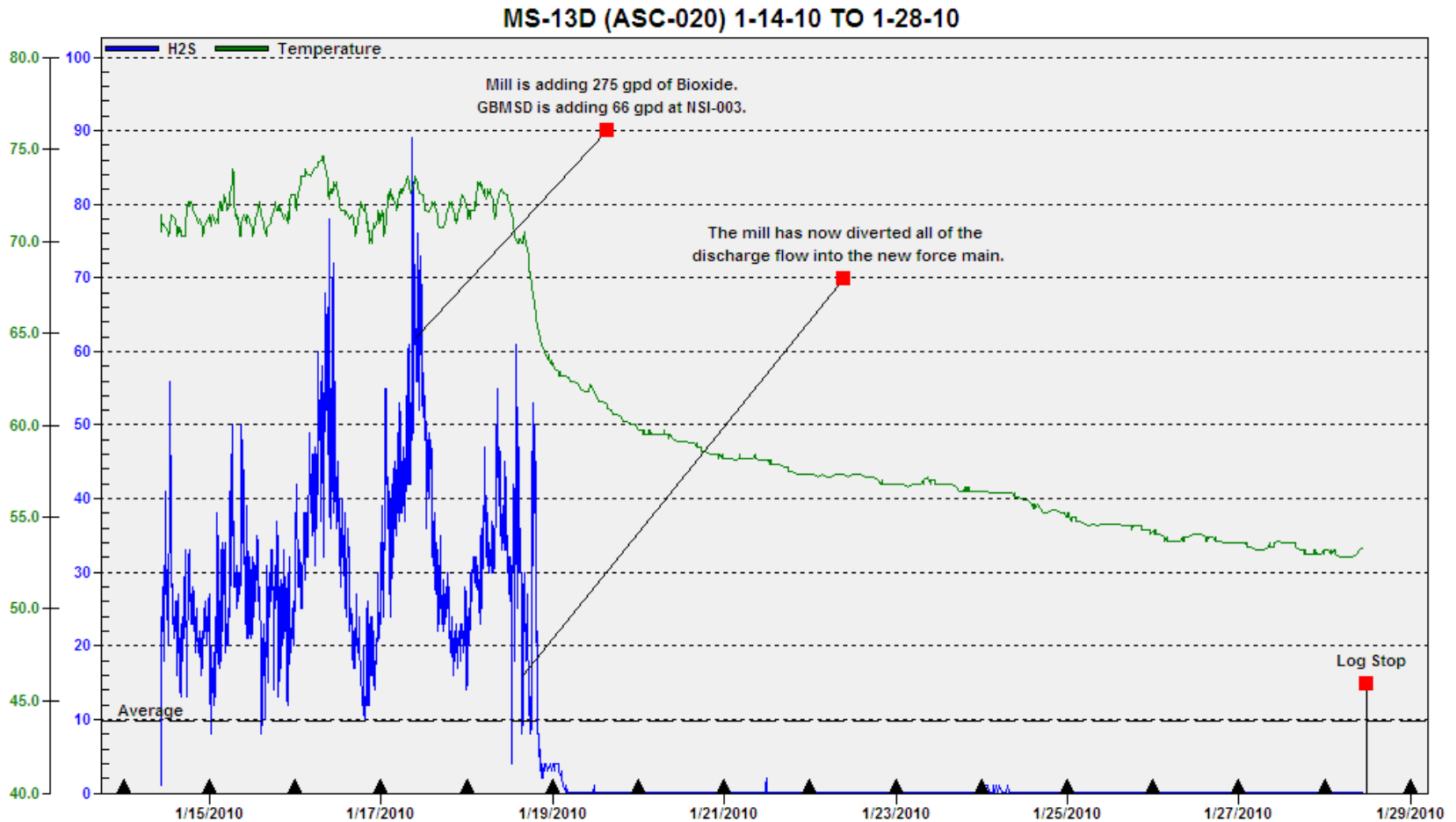


Permanent Solution

- Dedicated mill waste force mains
 - *Mill B to De Pere Facility (12" dia, 3.7 miles)*
 - *De Pere Facility to Green Bay Facility (10" dia, 6.9 miles)*
- Force main construction completed January, 2010
- Mill A
 - *Alter manufacturing process*
 - *Chemical dosing*



NSI/ASC – MH ASC-020: Vapor Phase H₂S Before and After Completion of Force Main



Period Displayed: 1/13/2010 - 1/29/2010 (Oda File: ASC-020 1-14-10 TO 1-28-10.oda -- Serial Number: Odialog Type L2 03900430 Instrument Range 0-1000PPM)

— Average 10 ▲ Day Transition Min 0 Max 89 (Use Screen Data Only)



Force Main Sulfide Control – Toxicity

- INTERCEPTOR Model used
 - *Sulfide generation*
 - *Chemical dosing requirements (3 mg/L target)*
- Jar testing
 - *Chemical performance*
 - *Chemical dosing requirements*
- New chemical dosing stations
 - *De Pere Facility*
 - *Intermediate Chemical Feed Building*
 - *Ferric chloride or BIOXIDE®*

Mill Waste Force Main Operation

| Mill Waste Force Main Location | INTERCEPTOR Predicted Dissolved Sulfides (mg/L) | Actual Dissolved Sulfides (mg/L) |
|-----------------------------------|--|--|
| De Pere Facility | 110 | 1 - 2 |
| Green Bay Facility | 117 | 5 – 10 |

- Discharge pressures in De Pere - Green Bay force main much higher than design pressure



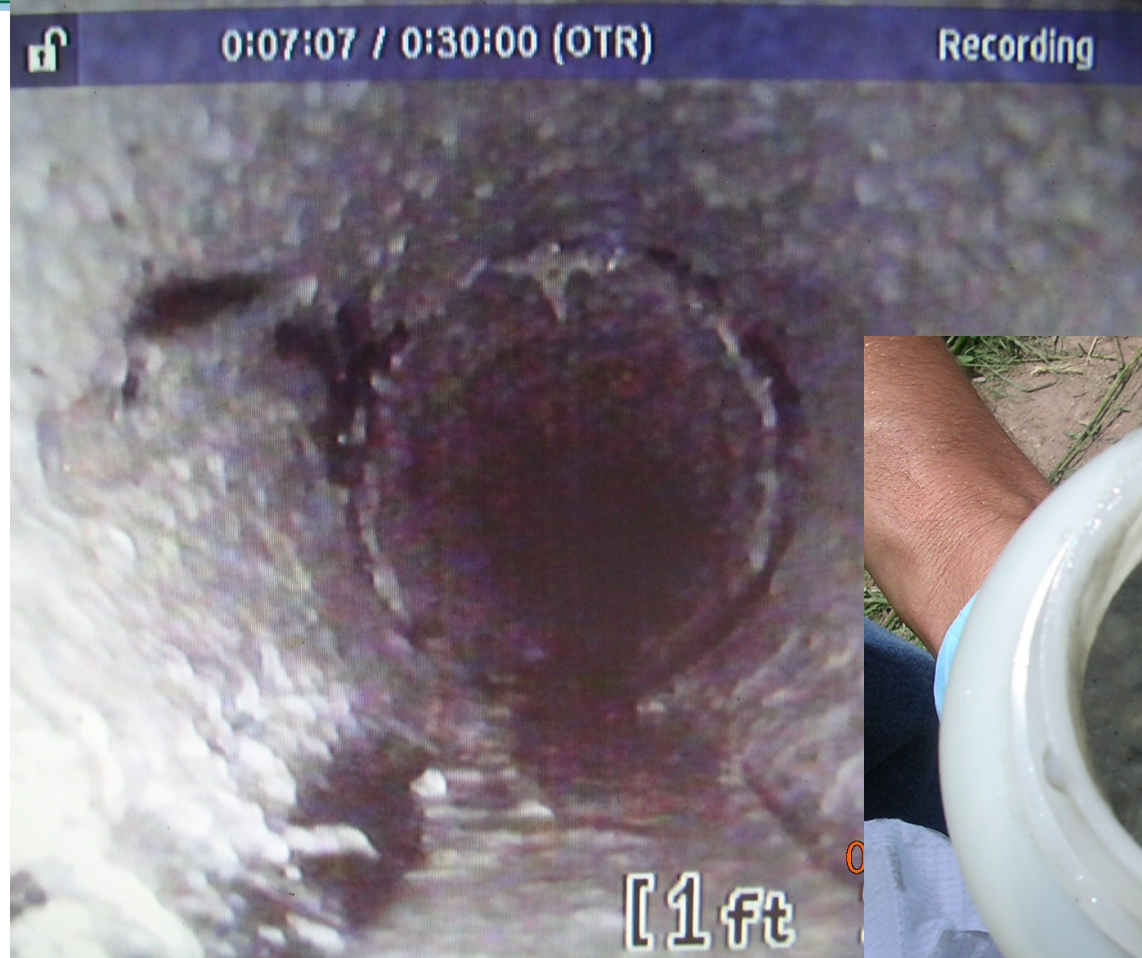
Mill Waste Force Main Operation

- Visual inspection of De Pere – Green Bay force main
 - *0.5 inch slime layer in force main*
 - *Proteinaceous slime unique to paper mill wastewater*
- Exists in both force mains but more prevalent in De Pere – Green Bay force main
 - *Appears to not be temperature related*
- Discharge pressures have stabilized



0:07:07 / 0:30:00 (OTR)

Recording



Mill Waste Force Main Operation

- Proteinaceous slime may reduce sulfide generation by:
 - *Inhibiting the activity of the sulfate reducing bacteria biofilm*
 - *Physically covering the biofilm*
 - *Retarding transfer of food to the bacteria*
 - *Retarding transfer of sulfide to the wastewater*
 - *Creating environment not conducive to sulfate reducing bacteria*
- Dosing ferric chloride at the Green Bay Facility



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Questions?