Kenosha Wastewater Treatment Plant

Energy Optimized Resource Recovery Project

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Kenosha Water Utility

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WWTP Service Area Overview

• Population: 110,000
• Service Area: 85.7 mi²

Collection System
  • Gravity Sewer System: 332 mi.
  • Lift Stations: 13

• Effluent Discharge: Lake Michigan
• Annual Average Daily Flow: 21.9 mgd
• Permitted Average Annual Daily Flow: 28.6 mgd
WWTP Loadings

Current Loadings (Based on 2015 Data):

• **BOD:**
  • Avg. Day 32,910 lbs/day; Effluent = 2,475 lbs
  • 92% Removal

• **TSS:**
  • Avg. Day 32,863 lbs/day; Effluent = 1,415 lbs
  • 96% Removal

• **Ammonia:**
  • Avg. Day 4,881 lbs/day; Effluent = 530 lbs
  • 89% Removal

• **Phosphorus:**
  • Avg. Day 533 lbs/day; Effluent = 85 lbs
  • 84% Removal
Sludge Characteristics

Primary Sludge:
- Average Flow – 68,619 gpd
- Solids Concentration – 3.3%
- Solids Production – 19,018 lbs/day
- Volatile Solids Production – 14,267 lbs/day
- Volatility – 77%

Waste Activated Sludge (WAS):
- Average Flow – 151,350 gpd
- Solids Concentration – 1.05%
- Solids Production – 13,006 lbs/day
- Volatile Solids Production – 9,377 lbs/day
- Volatility – 72%

Digested Sludge:
- Solids Concentration – 2.7%
- Volatile Solids – 54%
- Sludge to Landfill (2015) – 2,495 dry tons
Motivation Behind Project

• Aging WWTP infrastructure
• An effort to combat ever rising utility costs:
  • Natural Gas
  • Electricity
• Reduce or eliminate landfill disposal fees
Project Objectives

- Increase the generation of methane gas from anaerobic digestion of sludge;
- Generate electricity from the methane gas to produce greater than 500 kW of continuous power to be interconnected to the existing plant power network;
- Use the electricity generated to **offset peak energy pricing** during high demand periods;
- Use the electric and thermal energies generated to dry the biosolids so as to achieve 90% dry solids;
- Reduce the volume and cost of biosolids land filled;
- Produce high quality biosolids that meet the criteria for Class A biosolids allowing for beneficial reuse;
- Recover and utilize waste heat as the main thermal energy supply for the facility;
- Maintain existing effluent quality of the plant;
- Not increase ambient noise level, odor or particulates beyond the waste water treatment plant;
- Obtain a performance warranty for the system; and
- Install a system that can provide a payback period of 8 years or less.
Design Approach

• Design/build approach was utilized
• Wisconsin allows for design/build on resource recovery projects

• In the RFP the design/build was tasked with the following:
  • Preparation of the design
  • Assisting the Kenosha Water Utility (KWU) in obtaining all necessary permits
  • Procuring, constructing and installing all components
  • Integrating the new system with the existing plant supervisory control and data acquisition (SCADA) network
  • Startup and commissioning
  • Preparation of operations and maintenance manuals
  • Warrantying the system
KWU and Centrisys Corporation

• Relationship began in 2009 with the installation of a dewatering centrifuge
  • Intent was to replace our three plate and frame presses for sludge dewatering.
  • This project met or exceeded all design criteria
  • In addition, the reduced operational and labor costs provided a payback of one year!

• Based on the success of this project as well as the fact Centrisys is headquartered in Kenosha, WI we began a partnership to function as a research and development site for their technology.

• In 2011 Centrisys installed their first ever thickening centrifuge
  • Intent was to replace our dissolved air floatation thickening (DAFT) system for our waste activated sludge.
Primary Sludge Thickening
THK 200 by Centrisys Corporation

• *Previously*: The gravity thickened primary sludge was pumped directly from the primary clarifiers into one of the four primary digesters.
  • On average the primary sludge was 3.3% solids being pumped into the anaerobic digesters.

• *After Project*: To accomplish our goals of reducing the number of functional digesters and improving the overall heat balance of the plant KWU needed to further thicken the primary sludge stream
  • A thickening centrifuge was installed to further thicken the primary sludge to 7% solids.
  • No polymer or chemical addition is necessary to achieve desired sludge thickness.
Primary Thickening Centrifuge Installation
WAS Thickening Centrifuge

THK 200 by Centrisys Corporation

• Prior to our partnership: A DAFT system was utilized to thicken the WAS flow stream
  • The DAFT system thickened the WAS from 1% to 3.5%-4.0% solids before being pumped into one of the four primary digesters.

• A WAS thickening centrifuge was previously pilot tested and installed in 2011
  • Due to downstream limitations the WAS flow stream was thickened to roughly 5% solids with the thickening centrifuge
  • This project allowed us to further thicken the WAS flow stream to 7% solids
  • Once again, no polymer or chemical addition is necessary to achieve desired sludge thickness
  • The thickened WAS flow is discharged into a thermo-chemical hydrolysis process for further processing.
WAS Thickening Centrifuge Installation
Components of Hydrolysis Process:

• “Thermo” – TWAS is heated to 65-70°C (150-160°F)
• “Chemical” – Two liters of caustic soda (50% concentration) is injected per 1 m³ of TWAS
• Detention Time – After the addition of caustic soda and heat, the thickened WAS stream circulates through the reactor for 2 to 2.5 hours.
Thermo-Chemical Hydrolysis
Thermo-Chemical Hydrolysis

pH:
• Upon addition of caustic soda pH = 11
• Following hydrolysis process pH = 6.8 to 7.0
• Hydrolysis process breaks down the cell walls and releases internal organic acids which brings the pH of the flow stream back to neutral.
• “Hydrolysis” causes the pH adjustment and therefore no additional chemical addition is necessary.
Reduced Viscosity Provides for:
- Lower mixing energy requirements
- Higher digester loading rates
Thermo-Chemical Hydrolysis

Additional biogas production

Before Project:
• 2012: 166,200 ft³/day
• 2013: 173,800 ft³/day
• 2014: 170,600 ft³/day

After Project:
• Week of 2/29: 181,100 ft³/day (4-9% Increase)
• Week of 3/7: 187,300 ft³/day (8-13% Increase)
• Week of 3/14: 190,500 ft³/day (10-15% Increase)
Thermo-Chemical Hydrolysis

Additional biogas production

Before Project:
• 2012: 12.2 ft³/kg VS feed
• 2013: 13.4 ft³/kg VS feed
• 2014: 13.2 ft³/kg VS feed

After Project:
• Since 1/21/16: 17.6 ft³/kg VS feed
Thermo-Chemical Hydrolysis

Thermal Efficiency

• The blending of hydrolyzed TWAS and unheated thickened primary sludge results in a final temperature of roughly 40°C (100°F) which is ideal for the anaerobic digestion process

• All thermal energy required for the hydrolysis process is transferred into the digesters.

Atmospheric Pressure

• The entire hydrolysis process is completed at atmospheric pressure

Additional Volatile Solids Reduction

Increased Dewaterability of Digested Sludge
Thermo-Chemical Hydrolysis

Reactor:

• Two stage reactor with an outer and inner chamber
  • Outer Chamber – Recirculates the heated thickened WAS and caustic soda mixture
  • Inner Chamber – Acts as a buffer tank from which the transfer pump draws out of

• Volume - 516 ft\(^3\) (3,860 gal)

• Diameter:
  • Outer chamber – 8.2 ft
  • Inner chamber – 6.1 ft

• Height - 15.85 ft
PONDUS Reactor Installation
Thermo-Chemical Hydrolysis

Heat Exchanger:

• Corrugated tube in tube heat exchanger which creates turbulent flow resulting in:
  • Greater heat transfer capabilities
  • Reduced fouling of surface area

• Removable ends for easy inspection and maintenance
  • Thumb screws allow ends to be easily removed for internal inspection and cleaning.
PONDUS Heat Exchanger
High Solids Anaerobic Digestion

• **Before Project:**
  - Six functional anaerobic digesters
    - 4 primary & 2 secondary
  - Total capacity 633,550 ft$^3$
  - Unmixed
  - Batch feeding operation based on 8-hour shifts
  - Feed: Primary 3.3% TS and WAS 5.0% TS

• **After Project:**
  - Three functional anaerobic digesters
    - 2 primary & 1 secondary
  - Total capacity 319,650 ft$^3$
  - Fully mixed with mechanical hydraulic mixing
  - Continuous feeding operation
  - Feed: Primary and WAS 7% TS
High Solids Anaerobic Digestion

- **Hydraulic Retention Time (Average Day Flow):**
  - **Prior to Project:**
    - Primary Digesters 30 days
  - **Current:**
    - Primary Digesters 17 days
  - **Ultimate Operation:**
    - Primary Digester 22 days
    - Secondary Digester 15 days
Mechanical Hydraulic Mixing
Rotamix by Vaughan Company

System consists of:
• Chopper pump
• Internal piping
• Six nozzles (per digester)

Benefits:
• More even heating of contents
• Improved volatile solids reduction
• Increased gas production
Mechanical Hydraulic Mixing
Biosolids Dewatering

CS 21-4HC Centrifuge by Centrisys Corporation

• A dewatering centrifuge was installed at the WWTP in 2009.
• Replaced three plate and frame presses.
• The dewatering centrifuge has historically been fed digested sludge with a 2.7% TS concentration and consistently achieved 26-29% TS on the cake material.
• Due to the addition sludge thickening and PONDUS, the goal is to feed digested sludge with a 4.4% TS concentration and produce 30-32% TS solids.
Biosolids Dewatering
Drying of Biosolids
Compact belt dryer by Sulzle-Klein

• Prior to this project the dewatered biosolids were manually loaded into a truck and disposed of at a local landfill.

• After the installation of the new System, the dewatered material leaving the dewatering centrifuge is dried using the recovered heat from the co-generation units as the thermal supply.

• The compact belt dryer achieves all the requirements of Class-A material (temperature, duration, and moisture content) and KWU is currently in the process of getting our final biosolids product re-classified with the Wisconsin Department of Natural Resources.

• The dried product is discharged into a conveyor system and automatically deposited into the bed of a dump truck.
## Drying of Biosolids

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Value</th>
<th>Units</th>
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</thead>
<tbody>
<tr>
<td>Maximum Throughput (at 30% DS)</td>
<td>2,315</td>
<td>lb/hr</td>
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<tr>
<td>Heating Water Supply Temperature</td>
<td>194</td>
<td>°F</td>
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<tr>
<td>Heating Water Flow</td>
<td>115</td>
<td>gpm</td>
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<tr>
<td>Heating Water Return Temperature</td>
<td>160-170</td>
<td>°F</td>
</tr>
<tr>
<td>Maximum Air Flow</td>
<td>6,050</td>
<td>ft³/min</td>
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</table>
Drying of Biosolids
Biogas Conditioning
Gas conditioning and siloxane removal by Unison Solutions

• Prior to this project the raw biogas produced from the anaerobic digestion process was used as a fuel for our raw water pump engines, hot water boilers or flared to the atmosphere.

• Knowing a more efficient utilization of our biogas would be critical to an effective energy optimization project, a package system capable of removing moisture, particulates and siloxane was incorporated to condition and compress the biogas prior to use as a fuel source in the combined heat and power (CHP) generators.
Biogas Conditioning
Electric & Thermal Energy Generation
CHP Generators by Kraft Power

• Prior to this project the electricity needed to run the equipment at the WWTP was purchased exclusively from the local utility.
• In addition, any heat needed for our operations were provided by our boilers using either natural gas or biogas as their fuel source.
• To better utilize the biogas produced during the digestion process we installed two combined heat and power (CHP) generators.
• These generators utilize the methane produced in the anaerobic digestion process as a fuel source to generate electricity as well as thermal energy.
Electric & Thermal Energy Generation

• The CHP units are each capable of producing:
  • 330 kW of electrical energy
  • 422 kW of thermal energy.

• The electricity produced will power the new system as well as supply the excess electricity to the main plant power network for beneficial use elsewhere throughout the plant.

• The thermal energy will be utilized by the PONDUS system, the compact belt dryer and the central WWTP heating loop.
Odor Control
KWT 1000/1300 by Sulzle-Klein

• Due to the wastewater plant being located adjacent to a residential neighborhood odor control was also incorporated into the design.

• A robust odor control system which utilizes water, sulfuric acid and caustic soda was installed to treat the exhaust air from the belt dryer as well as the aspiration air from the primary sludge mix tank, blended sludge mix tank, PONDUS reactor, primary sludge thickening centrifuge, WAS thickening centrifuge, dewatering centrifuge and dryer feed pump.

• Water is utilized to cool the exhaust and remove particulates from the air.

• The sulfuric acid is used to reduce or eliminate the ammonia odors from the biosolids process.

• Caustic soda is used to reduce or eliminate the odors from sulfur compounds such as mercaptans in the exhaust stream.
Odor Control
Other Items Incorporated Into Project
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## Estimated Added Value

<table>
<thead>
<tr>
<th>Criteria</th>
<th>Daily</th>
<th>Annual</th>
<th>Unit Cost</th>
<th>Unit</th>
<th>Annual Savings</th>
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<tbody>
<tr>
<td>On-Peak Electricity (kWh)</td>
<td>4,536</td>
<td>1,655,640</td>
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<td>per kWh</td>
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<td>Off-Peak Electricity (kWh)</td>
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<td>Electric Demand (kW)</td>
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<td>Electrical Total</td>
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<td>Cake Sludge (wet tons)</td>
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<td>9,249</td>
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<td>per ton</td>
<td>$351,554</td>
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<td>Disposal Total</td>
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<td>TOTAL Savings</td>
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</table>
Grant from Local Utility

• Due to the nature of the project KWU was awarded over $500,000 in grants for implementing the new biosolids process from Focus on Energy.
• The installation of the thermo-chemical hydrolysis system, co-generation units, and LED lighting all qualified for the largest grant this organization can award for a single project.
Conclusion

Through innovative thinking KWU was able to:

• Become more energy efficient
• Less reliant on purchased electrical and thermal energy
• Reduce operating costs
Questions?

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